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1 **A robust nitrifying community in a bioreactor at 50°C opens up the path for**
2 **thermophilic nitrogen removal**

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4 Emilie N. P. Courtens¹, Eva Spieck², Ramiro Vilchez-Vargas¹, Samuel Bodé³, Pascal
5 Boeckx³, Stefan Schouten⁴, Ruy Jauregui⁵, Dietmar H. Pieper⁵, Siegfried E. Vlaeminck^{1,6*}
6 and Nico Boon¹✉*

7

8 ¹Laboratory of Microbial Ecology and Technology (LabMET), Ghent University, Coupure Links 653, 9000
9 Gent, Belgium

10 ²Biocenter Klein Flottbek, University of Hamburg, Microbiology & Biotechnology, Ohnhorststrasse 18, D-
11 22609 Hamburg, Germany

12 ³Isotope Bioscience Laboratory, Ghent University, Coupure Links 653, 9000 Gent, Belgium

13 ⁴Royal Netherlands Institute for Sea Research (NIOZ), Landsdiep 4, 1797 SZ, 't Horntje, Texel, Netherlands

14 ⁵Microbial Interactions and Processes Research Group, Helmholtz Centre for Infection Research, Braunschweig,
15 Germany

16 ⁶Research Group of Sustainable Energy, Air and Water Technology, University of Antwerp, Groenenborgerlaan
17 171, 2020 Antwerpen, Belgium

18

19 * These authors contributed equally and are both senior authors for this work

20 The authors declare no conflict of interest

21 ✉ Corresponding author: Nico Boon

22 Tel.: +32-9-2645976

23 Fax: +32-9-2646248

24 E-mail: Nico.Boon@UGent.be

25

26 **Running title:** A nitrifying community in a bioreactor at 50°C

27 **Subject Category:** Microbial engineering

28 **Keywords:** Archaea, compost, nitrification, *Nitrospira*, thermophile

29 **Abstract**

30

31 The increasing production of nitrogen-containing fertilizers is crucial to meet the global food
32 demand, yet, high losses of reactive nitrogen associated with the food
33 production/consumption chain progressively deteriorate the natural environment. Currently,
34 mesophilic nitrogen-removing microbes eliminate nitrogen from wastewaters. Although
35 thermophilic nitrifiers have been separately enriched from natural environments, no
36 bioreactors are described that enchain these processes for the treatment of nitrogen in hot
37 wastewaters. Samples from composting facilities were used as inoculum for the batch-wise
38 enrichment of thermophilic nitrifiers (350 days). Subsequently, the enrichments were
39 transferred to a bioreactor to obtain a stable, high-rate nitrifying process (560 days). The
40 community contained up to 17% ammoni-oxidizing archaea (AOA) closely related to
41 “*Candidatus Nitrososphaera gargensis*”, and 25% nitrite-oxidizing bacteria (NOB) related to
42 *Nitrospira calida*. Incorporation of ¹³C-derived bicarbonate into the respective characteristic
43 membrane lipids during nitrification supported their activity as autotrophs. Specific activities
44 up to 198±10 and 894±81 mg N g⁻¹ VSS day⁻¹ for AOA and NOB were measured, where
45 NOB were 33% more sensitive to free ammonia. The NOB were extremely sensitive to free
46 nitrous acid, while the AOA could only be inhibited by high nitrite concentrations,
47 independent of the free nitrous acid concentration. The observed difference in
48 product/substrate inhibition could facilitate the development of NOB inhibition strategies to
49 achieve more cost-effective processes such as deammonification. This study describes the
50 enrichment of autotrophic thermophilic nitrifiers from a nutrient-rich environment and the
51 successful operation of a thermophilic nitrifying bioreactor for the first time, facilitating
52 opportunities for thermophilic nitrogen removal biotechnology.

53 **Introduction**

54 The increased combustion of fossil fuels and extensive production of nitrogen-containing
55 fertilizers and industrial products lead to accumulation of reactive nitrogen in many natural
56 ecosystems, causing a worldwide environmental problem (Galloway *et al.* 2014). Just as
57 biodiversity loss and climate change, the aforementioned anthropogenic distortion of the
58 nitrogen cycle has by far exceeded the safety boundaries of our planet (Steffen *et al.* 2015).
59 Nitrification, the two-step microbe-mediated aerobic oxidation of ammonia to nitrate, plays a
60 key role in the transformation of reactive nitrogen necessary to restore the imbalanced
61 nitrogen cycle. Ammonia-oxidizing bacteria (AOB) and archaea (AOA) catalyze the first step,
62 i.e., the oxidation of ammonia (NH₃) to nitrite (NO₂⁻), while the successive oxidation to
63 nitrate (NO₃⁻), is carried out by nitrite-oxidizing bacteria (NOB).

64 Most AOB grow optimally at temperatures between 25 and 30°C (Ward *et al.* 2011), with a
65 maximum reported growing temperature of 55°C (Lebedeva *et al.* 2005). The recent
66 discovery of “*Candidatus Nitrosocaldus yellowstonii*”, an archaeon that grows up to 74°C
67 however broadened the phylogenetic spectrum of ammonia oxidizers active at high
68 temperatures (de la Torre *et al.* 2008). Two other moderately thermophilic (46°C) AOA
69 “*Candidatus Nitrososphaera gargensis*” (Hatzenpichler *et al.* 2008) and “*Candidatus*
70 *Nitrosotenuis uzonensis*” (Lebedeva *et al.* 2013) have been enriched from Russian hot
71 springs. Thermophilic ammonia oxidation is fuelling hydrothermal and geothermal life. Many
72 archaeal ammonia monooxygenase subunit A (*amoA*) genes have been detected in high-
73 temperature habitats such as deep-sea hydrothermal vents (Baker *et al.* 2012, Wang *et al.*
74 2009), subsurface thermal springs (Spear *et al.* 2007, Weidler *et al.* 2008) and terrestrial hot
75 springs (Dodsworth *et al.* 2011, Reigstad *et al.* 2008). In addition to these oligotrophic
76 ecosystems, the *amoA* gene was also measured in nutrient-rich high-temperature engineered
77 environments such as petroleum reservoirs (Li *et al.* 2011) and composting facilities (Zeng *et*

78 *al.* 2011). Although many archaeal *amoA* genes were detected in thermophilic environments,
79 only three enrichments were described so far (“*Candidatus Nitrosocaldus. yellowstonii*”,
80 “*Candidatus Nitrososphaera gargensis*” and “*Candidatus Nitrosotenus uzonensis*”).

81 Regarding thermophilic nitrite oxidation, it appears that *Nitrospira* spp. are the most dominant
82 NO_2^- oxidizers up to 60°C. *Nitrospira calida* was isolated from a microbial mat of a terrestrial
83 geothermal spring and maximally oxidizes NO_2^- at 46-52°C (Lebedeva *et al.* 2011). Thus far,
84 other detected/enriched NOB from geothermal springs are all closely related with *Nitrospira*
85 *calida* (Edwards *et al.* 2013, Marks *et al.* 2012).

86 Thermophilic microorganisms played a crucial role during the evolution of life on our planet
87 (Nisbet and Sleep 2001). Despite of the partnership between AOA and *Nitrospira* spp. that
88 potentially pioneered in ancestral nitrification (Vlaeminck *et al.* 2011), until now,
89 thermophilic nitrifiers were always separately enriched/studied in batch cultures. Enchained
90 ammonia and nitrite oxidation under thermophilic conditions has not yet been described,
91 neither in long-term batch flask enrichments nor in bioreactors. Besides for the recently
92 described *Nitrolancea hollandica* (Sorokin *et al.* 2014), all reported substrate/product
93 inhibitions levels for the described thermophilic nitrogen–converting organisms are relatively
94 low (Hatzenpichler *et al.* 2008, Lebedeva *et al.* 2011), making them rather unsuitable for
95 robust biotechnological applications. Lopez-Vazquez *et al.* (2014) recently reported nitrifying
96 activity up to 50°C in mesophilic sludge from an industrial wastewater treatment plant after
97 temperature shocking of mesophilic biomass (34°C) in short term batch activity assays.
98 However, the observations by Courtens *et al.* (2014a) pointed out that prolonged exposure (48
99 hours) of mesophilic biomass to a temperature shock can lead to a complete loss of nitrifying
100 activity. To our knowledge, there is no description of nitrification at 50°C or above for an
101 extended period of time. Long-term thermophilic aerobic bioreactor studies focused mainly
102 on the oxidation of organics. The major nitrogen removal mechanisms in those systems were

103 assumed to be ammonia stripping ($65 \pm 14\%$) and nitrogen assimilation into biomass (14 ± 4)
104 (Abeynayaka and Visvanathan 2011a, Abeynayaka and Visvanathan 2011b, Kurian *et al.*
105 2005, Yi *et al.* 2003). As neither nitrite nor nitrate was ever measured in these bioreactors at
106 45-60°C, there is no evidence that nitrification took place in these thermophilic systems. Until
107 now, only a few bioreactor studies focused on the long-term establishment of enchainned
108 thermophilic ammonia and nitrite oxidation, yet, reaching no more than 42°C (Courtens *et al.*
109 2014a, Shore *et al.* 2012).

110 This study describes the enrichment of autotrophic thermophilic nitrifiers from compost and
111 the successful operation of a thermophilic nitrifying bioreactor with high biotechnological
112 potential. We demonstrate that autotrophic AOA and NOB serve as key players in the
113 microbial community of the thermophilic nitrifying bioreactor. We also provide a
114 phylogenetic, physiological and morphological characterization of this unique nitrifying
115 consortium.

116

117 **Materials and methods**

118 ***Inoculum and batch enrichments***

119 Different aerobic compost facilities were sampled during the thermophilic stage (50-70°C):
120 digested organic waste (a), green waste (b), cow manure (c) and a mix of rabbit manure/green
121 waste (d). A 'compost extract' was prepared by shaking 20 g of compost in 200 mL water
122 with glass beads (12 h). The extract was used as inoculum (25 vol%) for enrichment
123 incubations (50°C) in a buffered medium (pH 7) with final concentrations of 0.929 g KH_2PO_4
124 L^{-1} , 1.622 g $\text{K}_2\text{HPO}_4 \text{ L}^{-1}$ and 0.5 g $\text{NaHCO}_3 \text{ L}^{-1}$ with $(\text{NH}_4)_2\text{SO}_4$ or NaNO_2 as the only
125 substrate (20 mg N L^{-1}). All incubations were provided with two different packing materials,
126 Kaldness K1 and polyurethane foam, to allow for both floccular as well as biofilm growth.

127 ***Reactor set-up and operation***

128 The compost enrichments showing both NH_3 and NO_2^- oxidation (b, d) were transferred to a
129 bioreactor. The reactor vessel (2 L, diameter 12 cm) was jacketed, allowing temperature
130 control at 50°C with a circulating thermostatic water bath. The reactor was operated in a
131 sequencing batch feeding/withdrawal mode. The 3-h cycle consisted of a 150-min aerobic
132 reaction period, a 10-min feeding period at the beginning of the cycle, a 15-min settling
133 period, a 5-min decanting period and a 10-min idle period. The bioreactor was fed with a
134 synthetic medium consisting of $(\text{NH}_4)_2\text{SO}_4$ (10-140 mg N L^{-1}), NaNO_2 (0-50 mg N L^{-1}), 9 g
135 $\text{NaHCO}_3 \text{ g}^{-1}$ N, KH_2PO_4 (10 mg P L^{-1}), NaCl (1.2 g L^{-1}) and 0.1 mL L^{-1} trace element
136 solution (Kuai and Verstraete 1998) dissolved in tap water. A flow rate of $3.4 \pm 0.2 \text{ L d}^{-1}$
137 resulted in a hydraulic retention time of 14 ± 0.7 h. Any transient $\text{NH}_4^+/\text{NO}_2^-$ build-up was
138 immediately corrected by adjusting the nitrogen loading, preventing accumulation of free
139 ammonia (FA) or free nitrous acid (FNA). The reactor pH was controlled between pH 6.8 and
140 7.2 by a dosage of 0.1 M NaOH/HCl. The dissolved oxygen was controlled at $3.6 \pm 0.2 \text{ mg L}^{-1}$

141 ¹ with air pumps providing aeration through a diffuser stone at a superficial air flow rate of
142 $1.33 \text{ m}^3 \text{ m}^{-2} \text{ h}^{-1}$.

143 ***Physiological characterization***

144 Physiological characterization along with inhibition tests were performed in ex-situ batch
145 activity measurements in 96-well plates with a working volume of 250 μL . Plates were
146 incubated in a MB100-4A Thermoshaker (Hangzhou Allsheng Instruments, Hangzhou,
147 China) at 50°C and 600 rpm, containing a buffer solution with a final concentration of 500 mg
148 P L^{-1} ($\text{KH}_2\text{PO}_4/\text{K}_2\text{HPO}_4$), 500 mg $\text{NaHCO}_3 \text{ L}^{-1}$, 0.1 mL L^{-1} trace element solution (Kuai and
149 Verstraete 1998) and $(\text{NH}_4)_2\text{SO}_4$ or NaNO_2 .

150 Operational parameters in the batch tests varied according to the investigated parameter. pH,
151 temperature and substrate concentrations were measured in all tests. From these, FA/FNA
152 concentrations were calculated based on their chemical equilibrium (Anthonisen *et al.* 1976).
153 The effects of the different parameters can only be separated from each other by a
154 combination of different tests as presented in **Table S1** for ammonia oxidation. A similar
155 strategy was applied for separation of nitrite and FNA effects on nitrite oxidation (**Table S2**).
156 All treatments were performed in sextuple, and liquid samples (2 μL) were taken over time
157 for NH_4^+ and NO_2^- analysis. Protein measurements enabled the calculation of specific rates
158 that were converted to volatile suspended solids (VSS) based on the average protein content
159 of the thermophilic sludge (32.7% protein VSS^{-1}).

160 ***High-throughput DNA sequencing, phylogenetic analysis and qPCR***

161 Biomass samples of the reactor were collected over time, and total DNA was extracted as
162 described previously (Courtens *et al.* 2014b). Prokaryotic biodiversity was analyzed using
163 pair-end high-throughput sequencing (MiSeq Illumina platform) of the regions V5-V6 of the
164 16S rRNA gene, using the primers 807F and 1050R previously described (Bohorquez *et al.*

165 2012). Libraries for barcoding sequencing were constructed as previously described
166 (Camarinha-Silva *et al.* 2014). The sequences were analyzed, obtaining 189358 total reads of
167 240 nucleotides in length. After a quality filter, 153611 total operational taxonomic units
168 (OTUs) were obtained and clustered into 155 unique taxa (Camarinha-Silva *et al.* 2014).
169 Forward and reverse reads were aligned manually, allowing zero mismatch (**Dataset S1**).
170 Sequencing depth was rarefied to the minimum, obtaining 18191 OTUs per sample. The 163
171 unique taxa were taxonomically annotated manually (**Dataset S1**). The vegan and phyloseq
172 packages in R were used to plot the rarefaction curves and normalize to the minimum
173 sequencing depth respectively. Phylogenetic analyses were performed with MEGA5 (Tamura
174 *et al.* 2011) using the neighbor-joining method with Jukes-Cantor correction and pairwise
175 deletion of gaps/missing data. In total 1000 bootstrap replications were performed to test for
176 branch robustness. The heat map was generated using gplots and RColorBrewer packages.
177 The SYBR Green assay (Power SyBr Green, Applied Biosystems) was used to quantify the
178 16S rRNA of *Nitrospira* spp. (Dionisi *et al.* 2002) and the functional archaeal amoA gene
179 (Tourna *et al.* 2008).

180 ***Electron microscopy***

181 For electron microscopy, biofilm material from three different sampling points in the
182 bioreactor was fixated and embedded in SPURR as described by Spieck and Lipski (2011).
183 The ultrathin sections were observed using a transmission electron microscope (model JEM
184 100C or LEO-906E, Zeiss, Jena, Germany).

185 ***Stable isotope probing: membrane lipids***

186 Reactor biomass was incubated (50°C, 100 rpm) in 120 mL gas-tight serum flasks containing
187 20 mL phosphate buffer (pH 7) with final concentrations of 750 mg P L⁻¹ (KH₂PO₄/
188 K₂HPO₄), 1 g NaH¹³CO₃ L⁻¹ and NH₄⁺ or NO₂⁻ as the sole nitrogen source. Liquid samples (2

189 μL) were taken over time for NH_4^+ and NO_2^- analysis. pH was adjusted through the addition
190 of HCl or $\text{NaH}^{13}\text{CO}_3$. Biomass from three parallel incubations with NH_4^+ (harvested at day 0,
191 49 and 85) served for alkyl iodides analysis, while biomass from five parallel incubations
192 with NO_2^- (harvested at day 0, 3, 7, 14 and 21) served for PLFA analysis. The sampling points
193 were determined based on the relative abundance of the AOA/NOB, the oxidation rates and
194 the sensitivity of the respective biomarker analysis.

195 *Alkyl iodides analysis*

196 Biomass was subjected to acid hydrolysis by refluxing for 3 h with 5% HCl in MeOH. The
197 resulting extract was separated using Al_2O_3 chromatography. Hexane:DCM (9:1) and
198 DCM:methanol (1:1) as eluents, yielding an apolar and polar fraction. An aliquot of the polar
199 fraction was analyzed for tetraether lipids using HPLC/MS (Schouten *et al.* 2007). The
200 remaining polar fractions were subjected to chemical treatment to release the biphytanyl
201 chains from the tetraether lipids (Lengger *et al.* 2014). The stable carbon isotopic composition
202 of the released biphytanes was analyzed in replicate using an Agilent 6800 GC coupled to a
203 Thermo Fisher Delta V isotope ratio monitoring mass spectrometer (Thermo Fisher Scientific,
204 Waltham, MA, USA) (Lengger *et al.* 2014).

205 *Phospholipid fatty acid analysis*

206 Extraction and derivatization of PLFAs for compound specific ^{13}C analysis was adapted from
207 Huygens *et al.* (2011). Identification of 11-methyl C16:0 was based on the retention time and
208 comparison with published mass spectra (Lipski *et al.* 2001) using the mass fragments m/z
209 185 and m/z 213 resulting from cleavage of the molecule at both sides of the methyl-branch,
210 as these are diagnostic fragments of 11-methyl-branched FAME. Isotopic enrichment was
211 assessed using the m/z 74/(74 + 76) ratio of the methyl acetate ion fragment.

212 *Chemical analyses*

213 NH_4^+ (Nessler method) and volatile suspended solids (VSS) were measured according to
214 standard methods. NO_2^- and NO_3^- were determined on a 930 Compact Ion Chromatograph
215 (Metrohm, Herisau, Switzerland) equipped with a conductivity detector. Dissolved oxygen
216 (DO) and pH levels were measured with an Oxymax COS22D probe (Endress Hauser,
217 Reinach, Switzerland) and a Dulcotest pH-electrode PHEP 112 SE (Prominent, Heidelberg,
218 Germany), respectively. In the batch activity tests, NH_4^+ and NO_2^- concentrations were
219 determined spectrophotometrically with the Berthelot and Montgomery reaction.
220 Measurements were obtained using a Tecan infinite plate reader (Tecan, Männedorf,
221 Switzerland), and biomass was quantified through protein concentrations. To determine the
222 protein concentration, the method developed by Lowry was used with bovine serum albumin
223 (BSA) as the standard.

224 **Results**

225 *Thermophilic batch enrichments*

226 Samples from four composting facilities served as inocula for the batch-wise enrichment of
227 thermophilic (50°C) nitrifying communities. The different origin of the organic fractions and
228 different compost process parameters (temperature, pH) resulted in different nitrogen
229 compound distributions in the four compost solutions. The green waste (a) and rabbit
230 manure/green waste mixture (b) exclusively contained oxidized forms of nitrogen ($\text{NO}_2^-/\text{NO}_3^-$
231), while the digested organic waste (c) and cow manure (d) only contained NH_4^+ (**Table S3**).
232 This distinction was reflected in the observed thermophilic nitrifying activity. First NH_3 and
233 NO_2^- oxidation was observed after approximately 100 days of incubation. Samples (a) and (b)
234 showed both NH_4^+ and NO_2^- oxidation, while samples (c) and (d) only showed NO_2^-
235 oxidation. After one year of incubation and several dilution steps, two highly active nitrite
236 oxidizing and two enchainned ammonia and nitrite oxidizing enrichment communities were
237 obtained (**Fig. S1**).

238 *Bioreactor performance*

239 The enrichments showing complete nitrification were pooled and served as inoculum for the
240 bioreactor at 50°C. Initial volumetric nitrification rates were low ($4.7 \pm 2.6 \text{ mg N L}^{-1} \text{ d}^{-1}$).
241 However, after two months of operation, a clear exponential increase in nitrifying activity was
242 observed in the reactor reaching volumetric NH_3 and NO_2^- oxidation rates of 126 ± 7 and
243 $189 \pm 17 \text{ mg N L}^{-1} \text{ d}^{-1}$, respectively (**Fig. 1**). After this first stage, due to a technical failure, the
244 community was challenged by a temperature drop to 30°C and a subsequent shock at pH 11
245 (days 235-238), leading to an initial loss of ammonia oxidation activity. However, the reactor
246 re-stabilized successfully, reaching nitrification rates higher than $200 \text{ mg NH}_4^+\text{-N L}^{-1} \text{ d}^{-1}$ (**Fig.**
247 **1**). Practically all the removed $\text{NH}_4^+\text{-N}$ was recovered as $\text{NO}_3^-\text{-N}$ ($93 \pm 4\%$), confirming that

248 nitrification was the main process involved. The biomass predominantly appeared as an
249 orange to brownish biofilm on the packing material and wall of the reactor vessel.

250 ***Phylogeny and morphology***

251 The thermophilic nitrifying microbial community was analyzed once in the first stage (day
252 150, data not shown) and once during the re-stabilization period of the reactor (days 245-387).
253 Illumina sequencing identified one unique sequence (OTU7) of archaea closely related to the
254 AOA “*Candidatus Nitrososphaera gargensis*” Ga9.2 (99% similarity) (**Fig. 2**), while no
255 known AOB could be detected. For nitrite oxidation, several different sequences closely
256 related to *Nitrospira* spp. were identified. OTU1, 99% similar to *Nitrospira calida* Ns10 (**Fig.**
257 **3**), was the most abundant *Nitrospira* sequence in the *Nitrospira*-community (98±2%) and the
258 only *Nitrospira*-related OTU that strongly increased in abundance over time (**Fig. S2**). Both
259 Illumina sequencing as qPCR analyses showed a considerable increase in abundance of
260 *Nitrospira*-related NOB and archaeal ammonia oxidizers over 6 months of operation (**Fig S3**).
261 The higher relative abundance of NOB (±25% vs. ±10%) in this community might have been
262 a result from the influent feeding strategy in which, besides ammonium, nitrite was provided
263 over most of the experiment to prevent limitation in NOB growth in case ammonia oxidation
264 would attenuate (**Fig. 1**). Beside the core nitrifiers (OTU1 and OTU7), the most abundant
265 OTU’s (>1%) at the end of the experiment appeared to be, among others, OTU2 and OTU3
266 (*Meiothermus*), OTU4 (*Thermomonas*), OTU5 and OTU8 (*Armatimonadetes*), OTU9
267 (*Ignavibacterium*) and OTU11 (*Proteobacterium*) (**Fig. S4**).

268 The presence of the described nitrifiers in the biofilm of the thermophilic reactor was
269 morphologically confirmed through transmission electron microscopy (TEM) (**Table S4**).
270 Cells of *Nitrospira* spp. were characterized by a spiral-shaped morphology with a
271 pleomorphic cell appearance, a wide periplasmic space and a granular cell interior (Ehrlich *et*

272 *al.* 1995)(**Table S4**). Small, very electron-dense, spherical cells with thick cell wall with
273 visible fimbriae and pili were observed, which were similar to the “*Candidatus*
274 *Nitrososphaera gargensis*” AOA characterised by Hatzenpitcher *et al.* (2008) (**Table S4**). As
275 the putative AOA cells were observed closely to the *Nitrospira* cells, this suggest the role of
276 the former cells as ammonia oxidizers. .

277 ***Carbon incorporation***

278 The autotrophic nature of the AOA and NOB during nitrification was investigated by
279 incorporation of ^{13}C -derived bicarbonate into the characteristic membrane lipids during two
280 sets of incubations, one with NH_4^+ and another with NO_2^- . Isotopic analysis of the biphytane
281 moieties of the characteristic archaeal membrane lipids, glycerol dibiphytanyl glycerol
282 tetraether lipids (GDGTs), was performed for AOA. The GDGTs were dominated by
283 crenarchaeol, in agreement with culture studies of “*Candidatus Nitrososphaera gargensis*”
284 (Pitcher *et al.* 2010). The two biphytanes released showed considerable enrichment in ^{13}C
285 compared to the start of the incubation, pointing at AOA autotrophy (**Fig. 4**). The activity of
286 NOB was determined by assessing the incorporation of ^{13}C -labeled bicarbonate into 11-
287 methyl C16:0, a specific biomarker for moderately thermophilic *Nitrospira* (Lipski *et al.*
288 2001, Spieck and Lipski 2011). The isotopic label was incorporated in the 11-methyl C16:0
289 phospholipid fatty acid biomarker after a lag-time of 3 days at the rate of $0.3\% \text{ day}^{-1}$ during
290 the 21 days of incubation. Interestingly, both for AOA and NOB, the ^{13}C enrichment (%)
291 appeared to be linear with the total amount of nitrogen oxidized (**Fig. 4**), demonstrating that
292 the autotrophic carbon assimilation by AOA and NOB occurred concurrently with the NH_3
293 and NO_2^- oxidation. Furthermore, the partnership between “*Candidatus Nitrososphaera*
294 *gargensis*” and *Nitrospira calida* was confirmed, as a 26% ^{13}C enrichment was measured for
295 the *Nitrospira* biomarker at the end of the incubation fed with NH_4^+ .

296

297 ***Physiological characterization***

298 The thermophilic biomass showed specific nitrifying rates up to 198 ± 10 and 894 ± 81 mg N g⁻¹
299 VSS day⁻¹, for NH₃ and NO₂⁻ oxidation, respectively. Taken into account an average relative
300 abundance of 10% AOA and 25% NOB and the simplified assumption that total protein was
301 equally distributed among all organisms in the culture, these rates result in a specific AOA
302 and NOB rate of 18 ± 1 and 33 ± 3 μg N mg⁻¹ protein h⁻¹, respectively. With respect to the
303 development of biotechnological applications and effective process control strategies, it is
304 important to distinguish the inhibitory effects of NH₄⁺ from those of free ammonia (FA) and
305 NO₂⁻ from those of free nitrous acid (FNA). The thermophilic NH₃ and NO₂⁻ oxidizers were
306 both sensitive to FA, while insusceptible to NH₄⁺. Ammonia oxidation was not inhibited up to
307 300 mg NH₄⁺-N L⁻¹ for the batch activity series with low FA, while it was inhibited for the
308 series tested at a higher FA, resulting in an IC₅₀ of 7.5 mg NH₃-N L⁻¹ (**Fig. 5A**). Interestingly,
309 no complete inhibition of ammonia oxidation was observed up to 80 mg NH₃-N L⁻¹ (**Fig. S5**).
310 A stable FA ammonia inhibition of $64 \pm 5\%$ was measured from 8.5 mg NH₃-N L⁻¹ onwards
311 (**Fig. S5**). Nitrite oxidation was slightly more sensitive for FA with an IC₅₀ of 5.0 mg NH₃-N
312 L⁻¹ (**Fig. 5B**). Regarding NO₂⁻/FNA inhibition, ammonia oxidizers were clearly inhibited by
313 NO₂⁻ and not by FNA. Both the series with high and low FNA gave the same inhibition
314 response with increasing NO₂⁻ concentrations (**Fig. 5C**). Sensitivity was, however, very low,
315 characterized with an IC₅₀ of 2117 mg NO₂⁻-N L⁻¹. In contrast, the NOB were extremely
316 sensitive to FNA and not to NO₂⁻ with an IC₅₀ of 0.0010 mg HNO₂-N L⁻¹ (**Fig. 5D**). Lowering
317 FNA while applying the same NO₂⁻ concentrations namely eliminated the inhibitory effect.
318 Nitrate inhibition of nitrite oxidation was also observed (IC₅₀ 360 mg NO₃⁻-N L⁻¹) (**Fig. S6**).
319 Thermophilic NH₃ oxidation showed a pH optimum at pH 7, maintaining >70% of its activity

320 within the tested pH range (pH 6-8) (**Fig. 6**). Although the bioreactor was controlled between
321 pH 6.8-7.2, it showed increasing NO_2^- oxidation at lower pH, given low FNA concentrations
322 (**Fig. 6**). Ammonia oxidation showed a broad temperature optimum (45-55°C), while nitrite
323 oxidation showed a clear optimal activity at the reactor temperature (50°C). Thermophilic
324 NH_3 oxidation could be inhibited by the conventional nitrification inhibitor ATU with an
325 $\text{IC}_{50/100}$ of 3.5/8.8 mM and the AOA-specific inhibitor carboxy-PTIO with an $\text{IC}_{50/100}$ of
326 63/117 μM (**Fig. S7**).

327 **Discussion**

328 In this study, the enrichment of coupled autotrophic thermophilic ammonia- and nitrite-
329 oxidizers from compost was achieved followed by the successful operation of a thermophilic
330 nitrifying bioreactor, opening up opportunities for nitrogen removal in warm wastewater.

331 The thermophilic nitrifying community in the bioreactor consisted of an AOA and NOB
332 closely related to “*Candidatus Nitrososphaera gargensis*” and *Nitrospira calida*. Interestingly,
333 the same co-existence was found in nature as both were originally isolated from the Garga hot
334 spring (Russia) (Hatzenpichler *et al.* 2008, Lebedeva *et al.* 2011). In contrast to the
335 oligotrophic nature of these geothermal springs, this study enriched nitrifiers from aerobic
336 compost, a nutrient-rich high-temperature anthropogenic environment. Although many
337 archaeal *amoA* genes (Maeda *et al.* 2011, Zeng *et al.* 2011) and even “*Candidatus*
338 *Nitrososphaera gargensis*”-like sequences (Oishi *et al.* 2012, Yamamoto *et al.* 2011) were
339 detected during composting processes, so far, no autotrophic thermophilic nitrifiers were
340 enriched from compost. Only a heterotrophic AOB growing at 50°C related to *Bacillus*
341 *halodurans* was isolated previously from animal waste composting (Shimaya and Hashimoto
342 2011). As the two compost piles that originally contained appreciable nitrate levels developed
343 thermophilic ammonia oxidation, while all compost yielded nitrite oxidation, the presence of
344 nitrate can lead to a smart selection of compost type for further studies focusing on
345 thermophilic AOA. The presence of the described core nitrifiers in the bioreactor was,
346 furthermore, linked with their activity and functionality. Incorporation of ¹³C labeled
347 bicarbonate was observed into crenarchaeol and 11-methyl C16:0, characteristic membrane
348 lipids for “*Candidatus Nitrososphaera gargensis*” (Pitcher *et al.* 2010) and *Nitrospira* (Lipski
349 *et al.* 2001), respectively. Although the carbon assimilation confirmed the autotrophic activity
350 of the studied nitrifiers, it does not exclude the presence of other, unknown autotrophic or
351 heterotrophic nitrifiers. An abundant cell type, embedded in a dense biofilm structure could

352 not be identified. Together with the observed delay/heterogeneity of the AOA presence over
353 time (**Fig. S3**), this could suggest that an uncharacterized ammonia oxidizing organism was
354 also present, as was recently observed in reactors with low dissolved oxygen concentrations
355 (Fitzgerald *et al.* 2015). The linearity of the nitrogen oxidation and the ^{13}C enrichment in the
356 stable isotope experiment (**Fig. 4**), however, suggest that “*Candidatus Nitrososphaera*
357 *gargensis*” and *Nitrospira calida* were important thermophilic nitrifiers in the biomass
358 community.

359 The physiological characterization revealed that the specific oxidation rates of both AOA
360 ($18 \pm 1 \mu\text{g N mg}^{-1} \text{ protein h}^{-1}$) and NOB ($33 \pm 3 \mu\text{g N mg}^{-1} \text{ protein h}^{-1}$) were in the same order of
361 magnitude as related nitrifiers. In particular, the specific rates for AOA range from 11 to 24
362 $\mu\text{g N mg}^{-1} \text{ protein h}^{-1}$ (Kim *et al.* 2012), while reported rates for *Nitrospira* spp. range
363 between 16 and 42 $\mu\text{g N mg}^{-1} \text{ protein h}^{-1}$ (Nowka *et al.* 2015). Interesting differences in
364 substrate/product tolerances were observed. Until now, data concerning $\text{NH}_4^+/\text{NH}_3$ inhibition
365 on (thermophilic) AOA has been limited attributing the inhibitory effect to NH_4^+ without
366 excluding FA inhibition. However, with respect to biotechnological applications and the
367 development of effective process control strategies, this distinction can be of great importance
368 and was determined in this study. The “*Candidatus Nitrososphaera gargensis*”-like AOA in
369 the thermophilic nitrifying bioreactor appeared to be insensitive to NH_4^+ , and could
370 maximally be inhibited by $63 \pm 5\%$ from $8.5 \text{ mg NH}_3\text{-N L}^{-1}$ (**Fig. 5, Fig. S5**). At a neutral pH
371 and a temperature of 50°C , this inhibition corresponds to a NH_4^+ concentration of 300 mg
372 $\text{NH}_4^+\text{-N L}^{-1}$. This concentration is 7 times higher than the inhibitory NH_4^+ concentration
373 reported for “*Candidatus Nitrososphaera gargensis*” (Hatzenpichler *et al.* 2008). The higher
374 FA tolerance could be attributed the fact that the AOA in this study originated from nutrient-
375 rich compost in contrast with oligotrophic geothermal springs. Indeed, the AOA detected in
376 cattle manure compost by Oishi *et al.* (2012) (Oishi *et al.* 2012) also showed a higher

377 tolerance towards media with a higher NH_4^+ concentration. The thermophilic NOB in the
378 bioreactor of our study were also sensitive to FA and insensitive to NH_4^+ , but the higher
379 sensitivity (IC_{50} of $5.0 \text{ mg NH}_3\text{-N L}^{-1}$) could allow a selective NOB inhibition based on FA.
380 Furthermore, the AOA were insensitive to FNA, while the NOB were extremely sensitive to
381 FNA (IC_{50} of $0.0010 \text{ mg HNO}_2\text{-N L}^{-1}$). Both the insensitivity of AOA for FNA and the high
382 sensitivity of NOB for FA and FNA suggest that a selective NOB inhibition could be easily
383 established in the described thermophilic nitrifying community, enabling the development of
384 more cost-effective nitrogen removal processes, such as nitritation/denitritation or
385 deammonification.

386 Until now, the main thermophilic nitrogen removal mechanism was assumed to be ammonia
387 stripping and nitrogen assimilation into biomass (Abeynayaka and Visvanathan 2011b).
388 Development of thermophilic biotechnology for nitrogen removal is necessary, as ammonia
389 stripping transfers the problem to the gas phase, and no sufficient nitrogen removal can be
390 reached based on assimilation. Besides eliminating cooling requirements, thermophilic
391 nitrogen removal also lowers sludge production and confers better settling properties
392 (Suvilampi and Rintala 2003). These advantages apply not only to warm wastewaters but also
393 to wastewaters on sites with excess heat available. A few lab-scale studies have explored the
394 potential of thermophilic nitrification for wastewater treatment, but achieved no more than
395 $40\text{-}42.5^\circ\text{C}$ (Courtens *et al.* 2014a, Shore *et al.* 2012). Thus far, this is the first study
396 describing a thermophilic nitrifying bioreactor at 50°C . Although challenges such as the effect
397 of carbon on the autotrophic/heterotrophic competition and the coupling of nitrification with a
398 reductive nitrogen removal process (denitrification, anammox) have to be addressed to enable
399 implementation, this study paves the way for thermophilic nitrogen removal.

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403 **Conflict of Interest**

404 The authors declare no conflict of interest.

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415

416 Supplementary Information accompanies this paper on The ISME Journal website
417 (<http://www.nature.com/ismej>)

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608

609

610 **Figure legends**

611 **Figure 1.** Nitrification performance ($\text{mg N L}^{-1} \text{d}^{-1}$) and nitrogen loss (%), i.e., the amount of
612 removed $\text{NH}_4^+\text{-N}$ not recovered as $\text{NO}_2^-\text{-N}$ or $\text{NO}_3^-\text{-N}$, in the thermophilic bioreactor (50°C)
613 inoculated with thermophilic nitrifying batch enrichments from compost samples. The white
614 and black triangles indicate the sampling for high-throughput DNA sequencing and
615 transmission electron microscopy, respectively.

616 **Figure 2.** Phylogenetic relationships between the archaeal 16S rRNA gene sequence (OTU7)
617 of the thermophilic nitrifying reactor biomass and all described AOA cultures or isolates, as
618 well as relevant environmental clone sequences. OTU7 belongs to the group 1.1b of
619 Thaumarchaeota (formerly Crenarchaeota).

620 **Figure 3.** Phylogenetic relationships between the most dominant *Nitrospira* 16S rRNA gene
621 sequences of the thermophilic nitrifying reactor biomass (OTU1) and all described *Nitrospira*
622 cultures or isolates, as well as relevant environmental clone sequences.

623 **Figure 4.** Relationship between the absolute amount of nitrogen oxidized and the ^{13}C
624 incorporation in characteristic biomarkers: the biphytane moieties of the glycerol dibiphytanyl
625 glycerol tetraether lipids (GDGTs), more specifically crenarchaeol, as a biomarker for
626 “*Candidatus Nitrososphaera gargensis*” and the 11 methyl C16:0 as a specific phospholipid
627 fatty acid biomarker of *Nitrospira* spp. Data points represent the average replicate extractions
628 ($n=3$), error bars represent the standard error.

629 **Figure 5.** Effect of ammonium/FA (free ammonia) and nitrite/FNA (free nitrous acid) levels
630 on thermophilic ammonia (A and C) and nitrite (B and D) oxidation. Each panel represents
631 two complementary batch activity experiments (filled and empty circles) with full lines
632 depicting the remaining activity, while the dotted lines display the corresponding FA/FNA

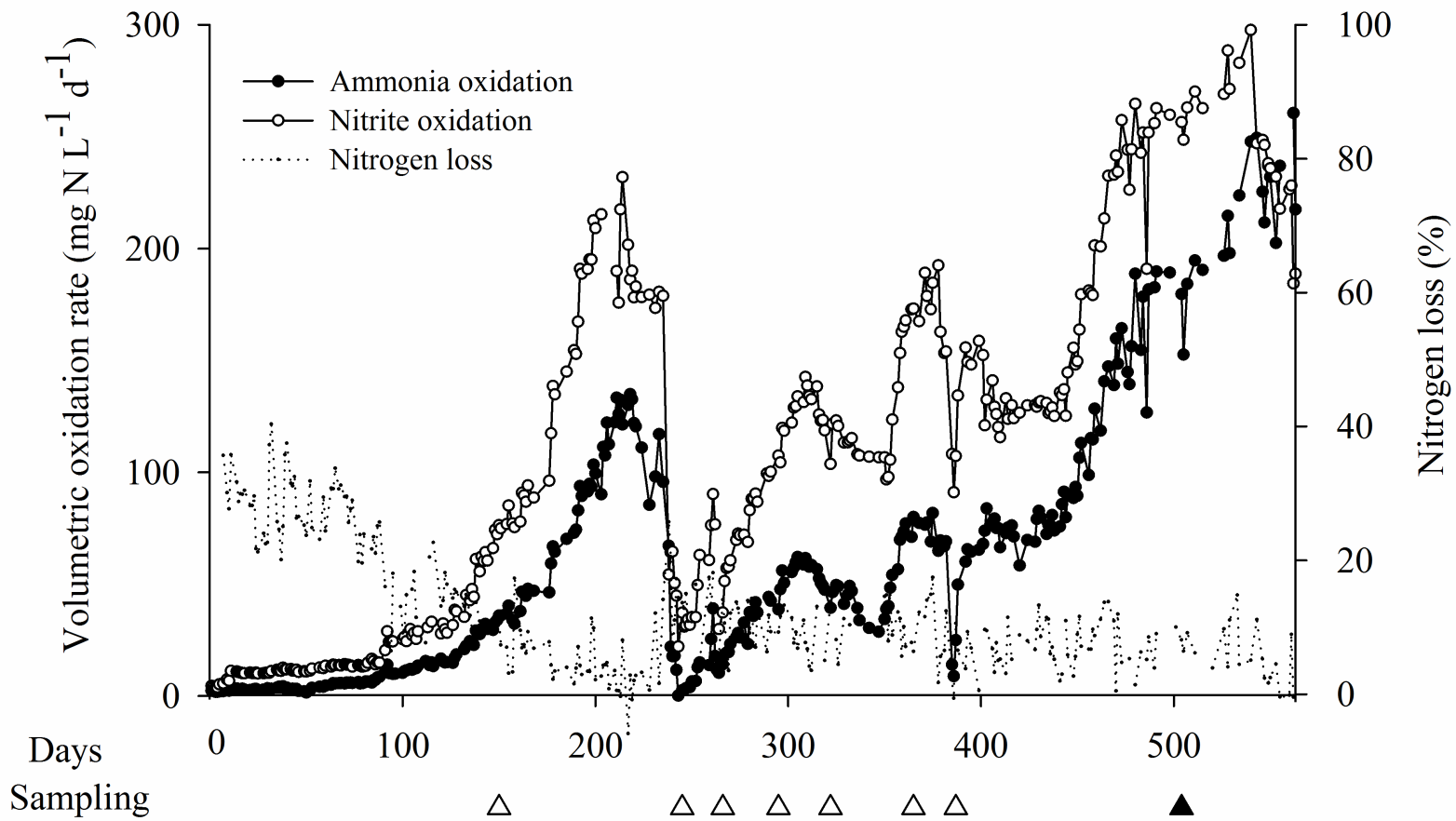
633 levels per test. Data points represent the average replicate tests (n=6), error bars represent the
634 standard error.

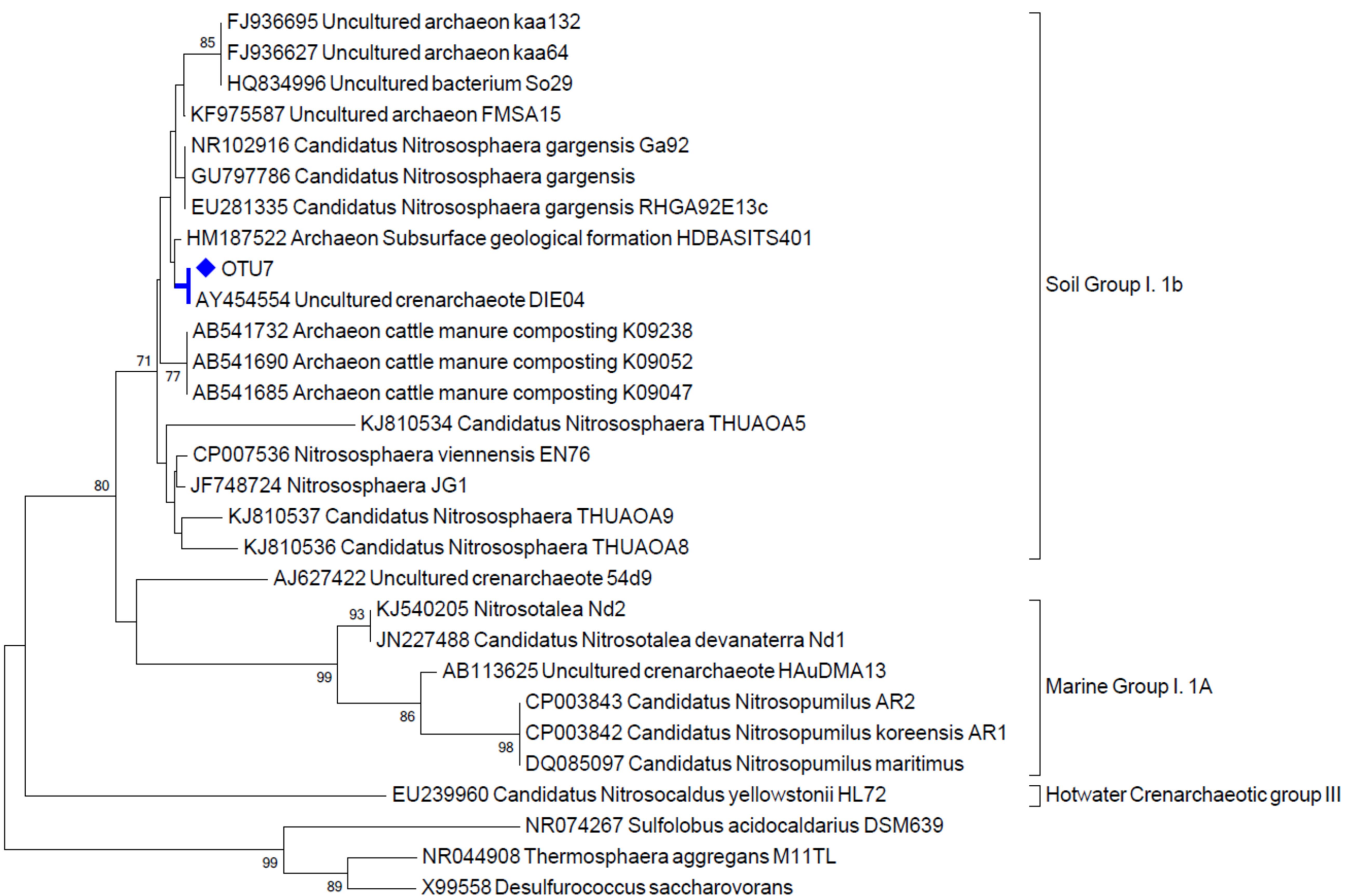
635 **Figure 6.** Effect of pH and temperature on thermophilic ammonia (A and B) and nitrite (C
636 and D) oxidation. Data points represent the average replicate tests (n=6), error bars represent
637 the standard error.

638

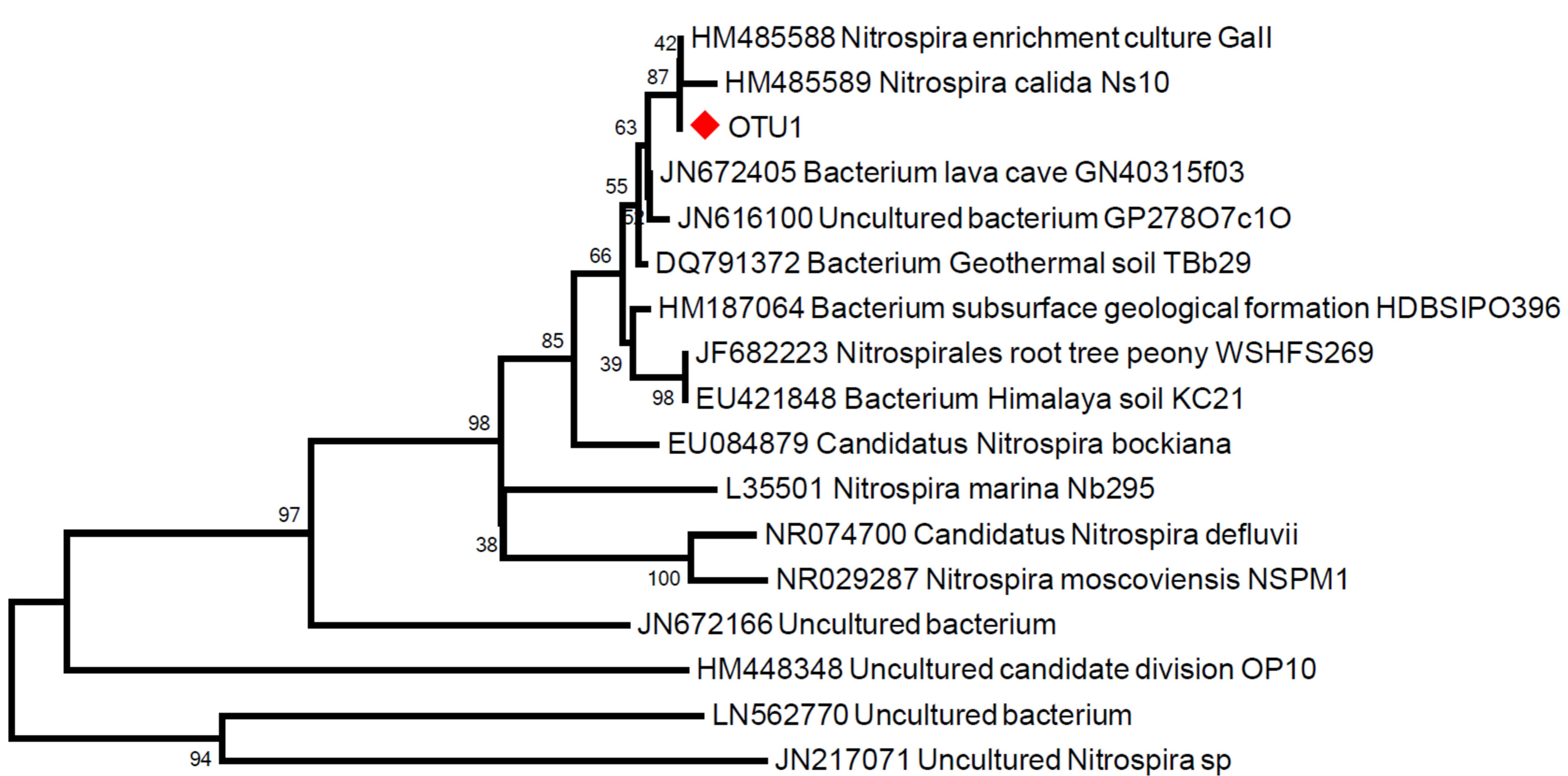
Influent (mg N L⁻¹)

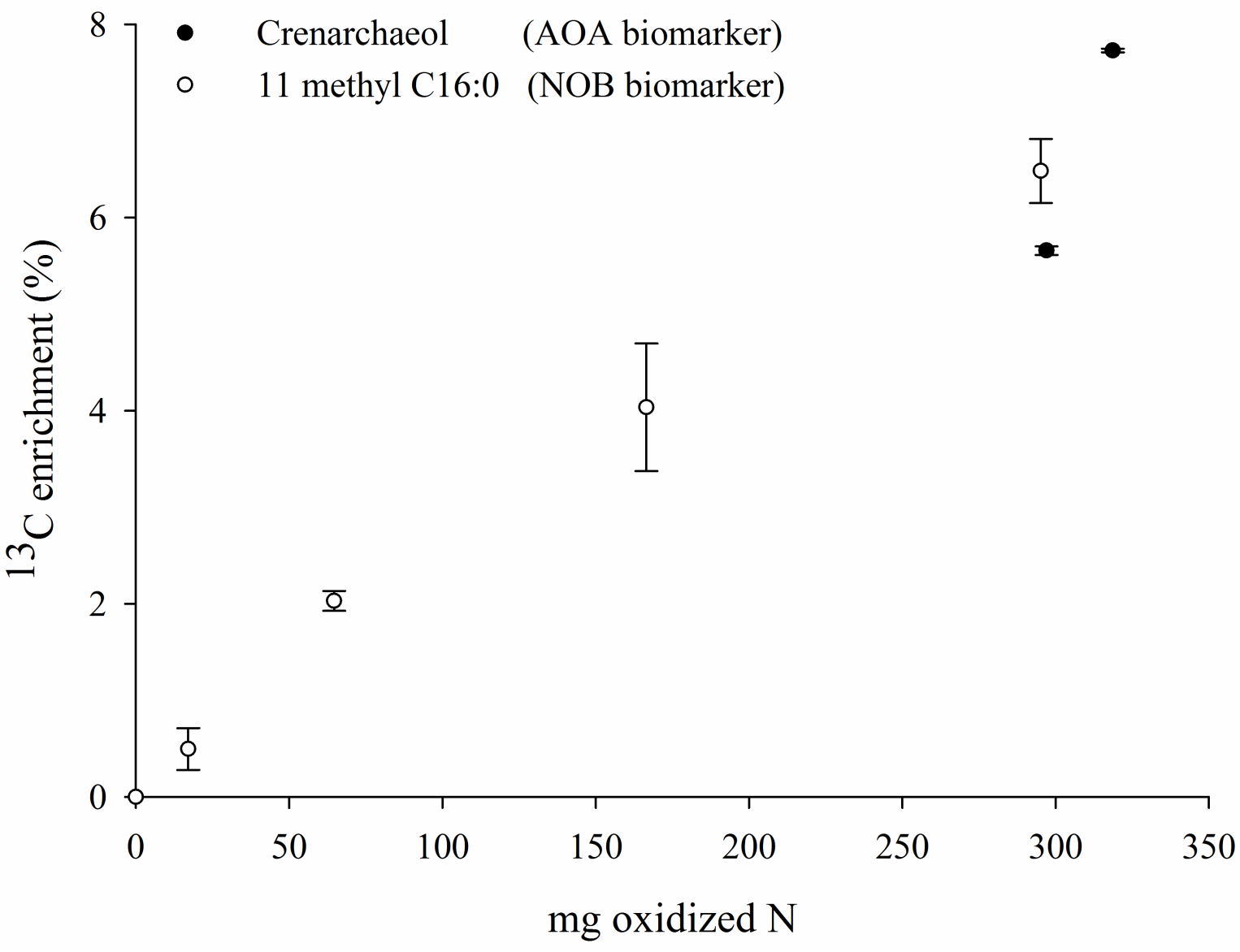
NH ₄ ⁺	19 ± 2	37 ± 11	32 ± 25	34 ± 9	66 ± 25	123 ± 20
NO ₂ ⁻	20 ± 3	35 ± 14	35 ± 18	46 ± 8	38 ± 9	-





0.02

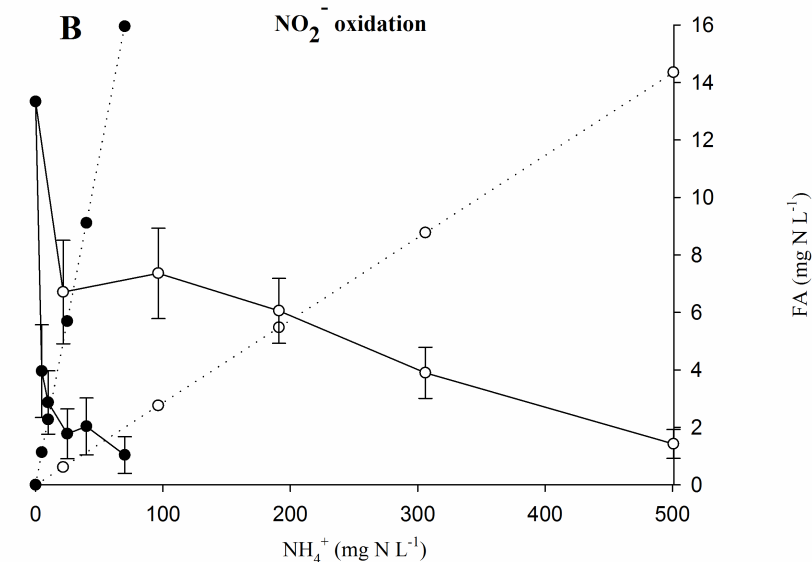
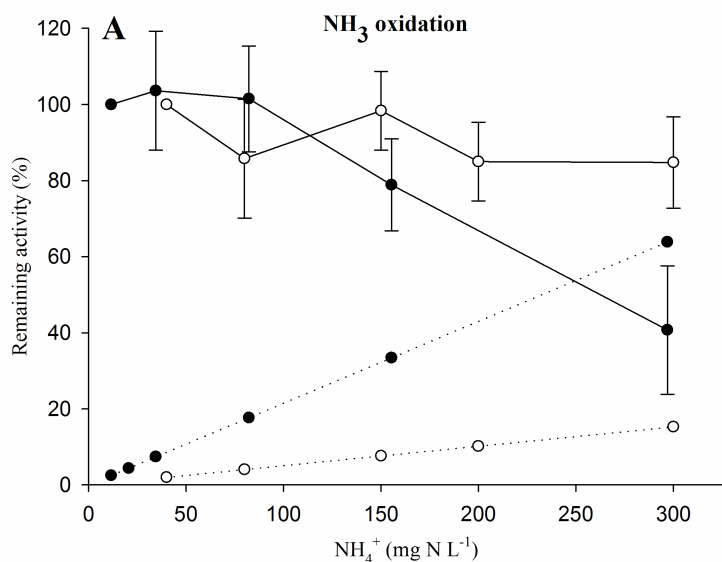




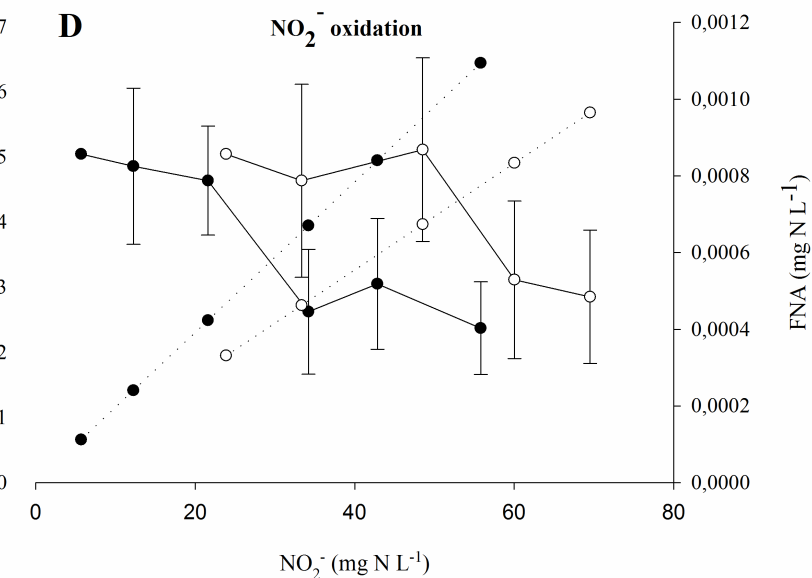
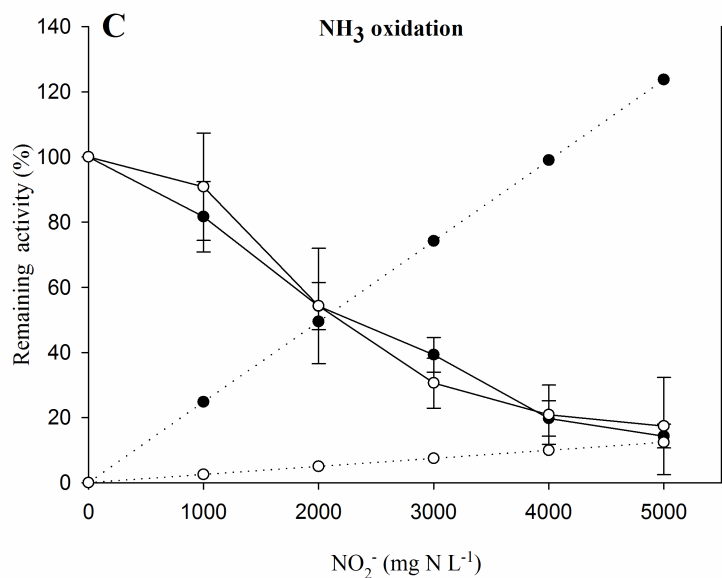
NH₄⁺-FA effect

— Remaining activity

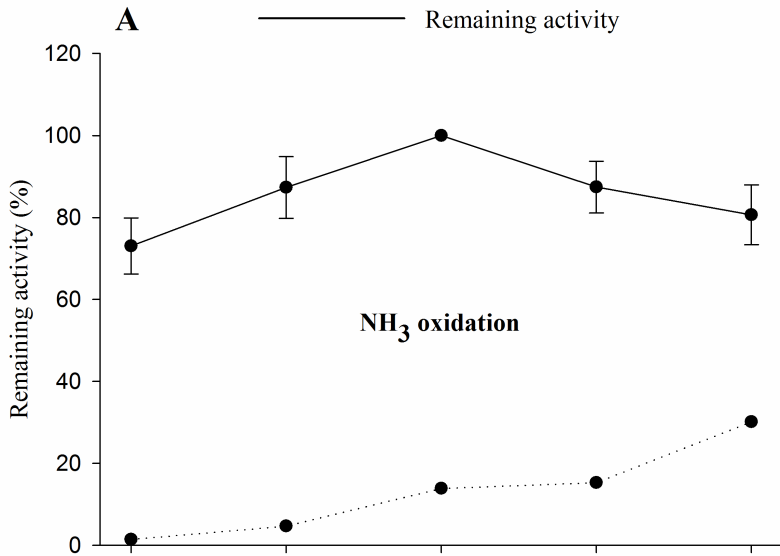
..... FA or FNA



NO₂⁻-FNA effect



pH effect



Temperature effect

