

# Enhanced NH<sub>3</sub> Synthesis from Air in a Plasma Tandem-Electrocatalysis System Using Plasma-Engraved N-Doped Defective MoS<sub>2</sub>

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Cite This: *JACS Au* 2023, 3, 1328–1336



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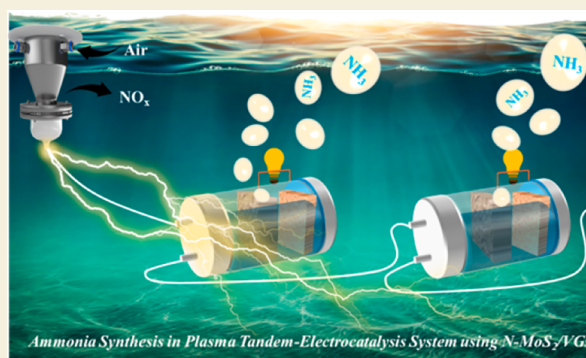
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**ABSTRACT:** We have developed a sustainable method to produce NH<sub>3</sub> directly from air using a plasma tandem-electrocatalysis system that operates via the N<sub>2</sub>–NO<sub>x</sub>–NH<sub>3</sub> pathway. To efficiently reduce NO<sub>2</sub><sup>−</sup> to NH<sub>3</sub>, we propose a novel electrocatalyst consisting of defective N-doped molybdenum sulfide nanosheets on vertical graphene arrays (N-MoS<sub>2</sub>/VGs). We used a plasma engraving process to form the metallic 1T phase, N doping, and S vacancies in the electrocatalyst simultaneously. Our system exhibited a remarkable NH<sub>3</sub> production rate of 7.3 mg h<sup>−1</sup> cm<sup>−2</sup> at −0.53 V vs RHE, which is almost 100 times higher than the state-of-the-art electrochemical nitrogen reduction reaction and more than double that of other hybrid systems. Moreover, a low energy consumption of only 2.4 MJ mol<sub>NH<sub>3</sub></sub><sup>−1</sup> was achieved in this study. Density functional theory calculations revealed that S vacancies and doped N atoms play a dominant role in the selective reduction of NO<sub>2</sub><sup>−</sup> to NH<sub>3</sub>. This study opens up new avenues for efficient NH<sub>3</sub> production using cascade systems.

**KEYWORDS:** sustainable NH<sub>3</sub> production, plasma electrocatalysis, defective N-MoS<sub>2</sub>, plasma engraving, density functional theory



Ammonia Synthesis in Plasma Tandem-Electrocatalysis System using N-MoS<sub>2</sub>/VGs

## INTRODUCTION

Ammonia (NH<sub>3</sub>) is essential for modern agriculture<sup>1,2</sup> and is being explored as a promising carbon-free hydrogen carrier to tackle climate change and energy challenges.<sup>3</sup> However, the conventional centralized Haber–Bosch process for industrial NH<sub>3</sub> production requires extremely harsh conditions,<sup>4</sup> resulting in high energy demands<sup>5</sup> and significant CO<sub>2</sub> emissions.<sup>6</sup> Therefore, developing sustainable, environmentally friendly, and distributable routes for NH<sub>3</sub> production is critical.

One promising approach is electrochemical nitrogen reduction reaction (eNRR) to NH<sub>3</sub>, which can be powered by renewable electricity using abundant N<sub>2</sub>/air and H<sub>2</sub>O under ambient conditions.<sup>7–11</sup> The performance of electrocatalysts is crucial for eNRR kinetics. Among the noble-metal-based,<sup>12,13</sup> transition-metal-based,<sup>14,15</sup> and metal-free electrocatalysts<sup>16,17</sup> explored, Mo, especially MoS<sub>2</sub>, is of particular interest due to its natural occurrence in biological nitrogen fixation and structural similarity to nitrogenase.<sup>18–21</sup> Recently, there has been a surge in efforts to enhance catalyst reactivity through phase transformation,<sup>22</sup> heteroatom doping,<sup>23</sup> and defect engineering.<sup>24</sup> Nevertheless, the ultrastrong N≡N bond,<sup>25–27</sup> competitive hydrogen evolution reaction (HER),<sup>28</sup> and poor solubility of N<sub>2</sub> in the electrolyte<sup>29</sup> have limited the NH<sub>3</sub> production rate to <0.1 mg h<sup>−1</sup> cm<sup>−2</sup>.

To address these challenges, a promising two-step strategy has been proposed that uses plasma to activate inert N<sub>2</sub> into more accessible and clean nitrogen oxides (NO<sub>x</sub>), followed by enhanced electroreduction of NO<sub>x</sub><sup>−</sup> into NH<sub>3</sub>.<sup>30–32</sup> Although NO<sub>x</sub><sup>−</sup> may be abundant in wastewater, it would be unsuitable for this application due to the presence of impurities. The plasma electrocatalysis approach uses air instead of pure nitrogen, eliminating the need for energy-intensive air separation and purification processes, and is suitable for intermittent and decentralized operation using renewable energy sources as a turnkey process.<sup>33–35</sup> While an NH<sub>3</sub> production rate of up to 3.0 mg h<sup>−1</sup> cm<sup>−2</sup> has been achieved,<sup>36,37</sup> investigations into this strategy remain extremely limited. Further development of new electrochemical NO<sub>x</sub><sup>−</sup> reduction reaction (eNO<sub>x</sub><sup>−</sup>RR) processes, including system design and high-performance catalysts such as MoS<sub>2</sub>, is critical to improve the slow conversion of NO<sub>x</sub><sup>−</sup> to NH<sub>3</sub> in the second

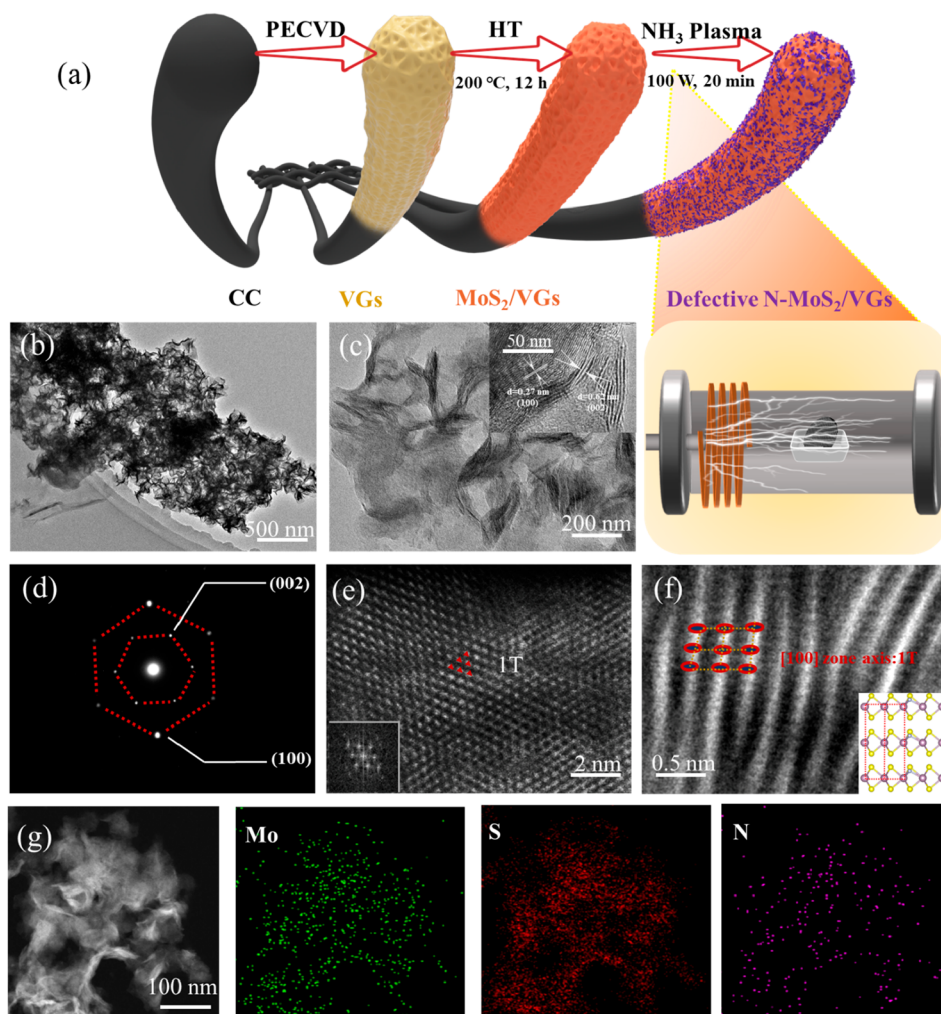
Received: February 20, 2023

Revised: April 12, 2023

Accepted: April 13, 2023

Published: April 26, 2023





**Figure 1.** (a) Schematic illustration for N-MoS<sub>2</sub>/VGs fabrication procedure and RF NH<sub>3</sub> plasma engraving process. (b) TEM image, (c) HRTEM image, (d) SAED pattern, (e) HAADF image, (f) AC-STEM image, and (g) EDX mapping of N-MoS<sub>2</sub>/VGs.

step. Moreover, existing catalyst engineering strategies typically require high temperature (>300 °C)<sup>38</sup> and long-duration treatment (>2 h),<sup>24</sup> calling for a more facile and rational catalyst fabrication approach. Furthermore, a molecular-level understanding of the complex eNO<sub>x</sub><sup>-</sup>RR mechanism remains limited, requiring in-depth experimental and theoretical studies.

Herein we propose a plasma tandem-electrocatalysis system to generate NH<sub>3</sub> from air (see [Plasma Tandem-Electrocatalysis Setup](#) and [Figure S1](#)). We engineered a novel defective N-MoS<sub>2</sub> electrocatalyst supported by vertical graphene arrays on carbon cloth (VGs/CC) with exceptional eNO<sub>x</sub><sup>-</sup>RR reactivity. Advanced physical characterizations and density functional theory (DFT) calculations were conducted to elucidate the eNO<sub>x</sub><sup>-</sup>RR reaction pathways with N-MoS<sub>2</sub>/VGs.

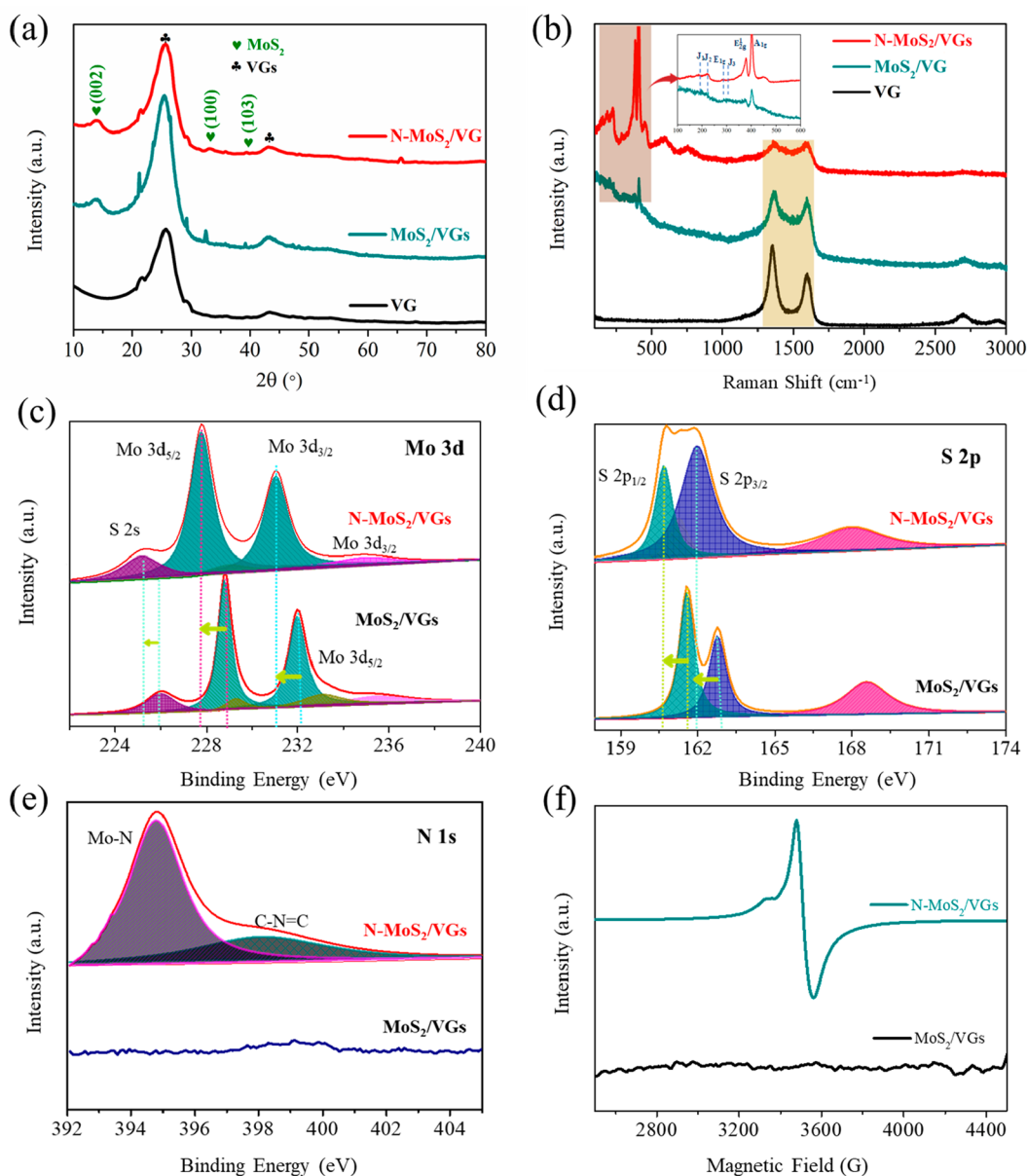
## RESULTS AND DISCUSSION

The MoS<sub>2</sub> nanosheets were assembled by a hydrothermal (HT) method and supported by vertical graphene arrays obtained through plasma-enhanced chemical vapor deposition (PECVD) on CC ([Figure 1a](#) and [Catalyst Synthesis](#)). The transmission electron microscopy (TEM) image ([Figure 1b](#)) confirmed the formation of a well-defined nanosheet profile. The marked space lattice fringe and distinct spots in the high-

resolution transmission electron microscopy (HRTEM) image ([Figure 1c](#)) together with the selected-area electron diffraction (SAED) pattern ([Figure 1d](#)) revealed the (002) and (100) planes of MoS<sub>2</sub>.

Notably, we pioneered a radiofrequency (RF) NH<sub>3</sub> plasma strategy for atomic-level surface engineering of MoS<sub>2</sub> ([Figure 1a](#)). By creation of a plasma sheath on the sample surface, ablated Mo atoms reacted with N atoms in the plasma to form N-MoS<sub>2</sub>. Furthermore, the plasma treatment also generated crystal vacancies via ion sputtering and etching effects of NH<sub>3</sub>.<sup>39–41</sup> This method required only a short duration (20 min) and low temperature (25 °C). The formation of octahedrally coordinated 1T-MoS<sub>2</sub> after the plasma engraving was confirmed by high-angle annular dark-field (HAADF) ([Figure 1e](#)) and spherical aberration corrected scanning transmission electron microscopy (AC-STEM) along the (100) zone axis ([Figure 1f](#)). The HRTEM images of MoS<sub>2</sub>/VGs and N-MoS<sub>2</sub>/VGs further evidenced the distinct phase transformation from 2H to 1T ([Figures S2 and S3](#)). Additionally, energy-dispersive X-ray (EDX) elemental mapping images demonstrated the uniform distribution of Mo, S, and N in the N-MoS<sub>2</sub>/VGs ([Figure 1g](#)).

X-ray diffraction (XRD) patterns ([Figure 2a](#)) reveal characteristic peaks at 14.37°, 32.68°, and 39.54° that

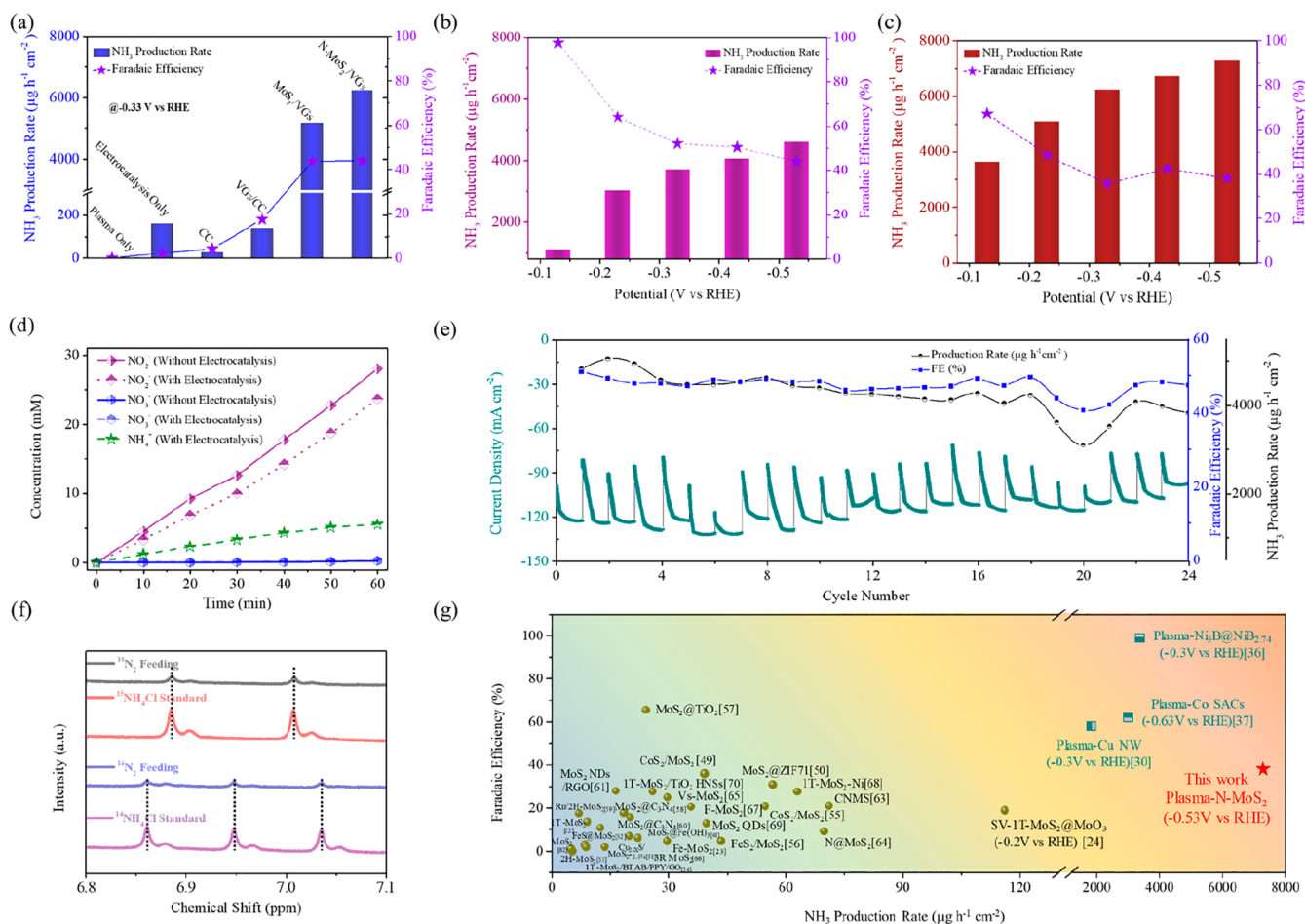


**Figure 2.** (a) XRD patterns and (b) Raman spectra of N-MoS<sub>2</sub>/VGs, MoS<sub>2</sub>/VGs, and VGs. (c–e) XPS spectra of (c) Mo 3d, (d) S 2p, and (e) N 1s over N-MoS<sub>2</sub>/VGs and MoS<sub>2</sub>/VGs. (f) EPR spectra of N-MoS<sub>2</sub>/VGs and MoS<sub>2</sub>/VGs.

correspond to the (002), (100), and (103) planes of MoS<sub>2</sub> (PDF no. 37-1492) for N-MoS<sub>2</sub>/VGs, MoS<sub>2</sub>/VGs, and VGs. The 1T phase of N-MoS<sub>2</sub>/VGs is further confirmed by Raman spectroscopy (Figure 2b). The E<sub>2g</sub> and A<sub>1g</sub> peaks at 380 and 405 cm<sup>-1</sup>, respectively, are observed in both MoS<sub>2</sub>/VGs and N-MoS<sub>2</sub>/VGs, with N-MoS<sub>2</sub>/VGs also exhibiting three additional peaks (148, 207, and 335 cm<sup>-1</sup>) associated with vibrational modes of the 1T phase. The E<sub>2g</sub> peak (380 cm<sup>-1</sup>) is also found in N-MoS<sub>2</sub>/VGs due to the well-organized tetragonal symmetry.<sup>42–44</sup> X-ray photoelectron spectroscopy (XPS) (Figure 2c–e) revealed the presence of Mo, S, and N in N-MoS<sub>2</sub>/VGs and the absence of N in MoS<sub>2</sub>/VGs. The Mo 3d spectrum of MoS<sub>2</sub>/VGs can be deconvoluted into four peaks, with two dominant peaks at 232.0 eV (Mo 3d<sub>3/2</sub>) and 229.1 eV (Mo 3d<sub>5/2</sub>) assigned to the 1T phase and two other peaks at 233.5 eV (Mo 3d<sub>3/2</sub>) and 229.6 eV (Mo 3d<sub>5/2</sub>) allocated to the 2H phase.<sup>45,46</sup> Conversely, only two typical 1T phase peaks at 231.2 eV (Mo 3d<sub>3/2</sub>) and 229.1 eV (Mo 3d<sub>5/2</sub>) are detected in

N-MoS<sub>2</sub>/VGs. Furthermore, the positive shift of N-MoS<sub>2</sub>/VGs to MoS<sub>2</sub>/VGs also confirms the phase transformation from 2H to 1T. Notably, the S:Mo ratio decreased from 1.74 to 1.37, according to quantized EDX data (Table S1), likely due to the substitution of N and possible S vacancies induced by plasma engraving. This hypothesis is explicitly proven by the electron paramagnetic resonance (EPR) spectroscopy results (Figure 2f), which display a prominent signal at *g* = 2.004 assigned to S vacancies in N-MoS<sub>2</sub>/VGs and no signal in MoS<sub>2</sub>/VGs, suggesting the partial deletion of thiol–Mo bonds in N-MoS<sub>2</sub>/VGs.<sup>47</sup>

Comparative experiments in the plasma or electrocatalysis alone system and the plasma electrocatalysis system with different catalysts were performed at –0.33 V versus reversible hydrogen electrode (V vs RHE). As shown in Figure 3a, neither the plasma- or electrocatalysis-alone system nor the eNO<sub>x</sub>RR over the substrates (CC and VGs/CC) yielded significant NH<sub>3</sub>. However, the MoS<sub>2</sub> catalyst dramatically



**Figure 3.** (a–c) NH<sub>3</sub> production rates and FEs for (a) plasma only, N-MoS<sub>2</sub>/VGs electrocatalysis only, and plasma electrocatalysis with different catalysts, (b) plasma single-electrocatalysis, and (c) plasma tandem-electrocatalysis. (d) Time-dependent concentrations of nitrate, nitrite, and NH<sub>4</sub><sup>+</sup> with/without electrocatalysis in the hybrid system. (e) Stability tests. (f) <sup>1</sup>H NMR (600 MHz) spectra in <sup>14</sup>N<sub>2</sub> or <sup>15</sup>N<sub>2</sub> atmosphere after N-MoS<sub>2</sub>/VGs electrocatalysis. (g) Comparison of eNRR using different MoS<sub>2</sub> catalysts (green symbols), other plasma-electrocatalysis systems (indigo symbols), and this work (red star). See Tables S6 and S7 for more details.

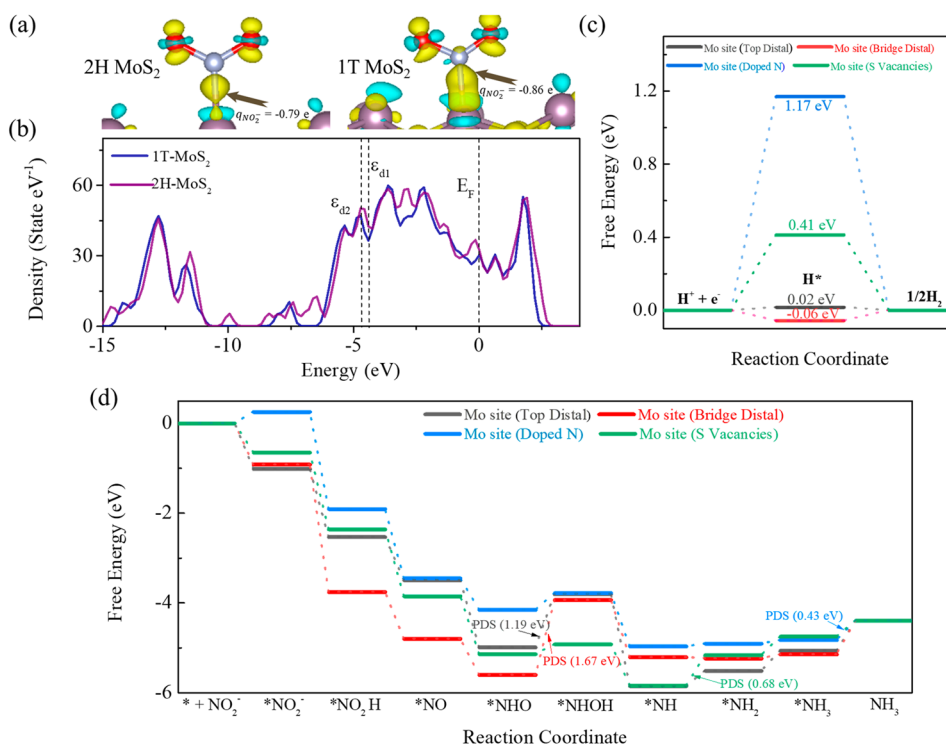
enhanced the NH<sub>3</sub> production rate (5.2 mg h<sup>-1</sup> cm<sup>-2</sup>) by a factor of approximately 38 over the substrates. Notably, the defective N-MoS<sub>2</sub>/VGs catalyst further improved the catalytic reactivity by over 20%, reaching a production rate of up to 6.2 mg h<sup>-1</sup> cm<sup>-2</sup>. This enhancement is attributed to the improved electron conductivity, higher charge polarization, and increased active sites of N-MoS<sub>2</sub>/VGs, as discussed above.

In this study, plasma tandem-electrocatalysis was utilized by coupling double electrocatalyst cells, and for comparison, a plasma single-electrocatalysis system was also tested. The results, depicted in Figure 3b,c, demonstrated that increasing potentials had a positive effect on the average NH<sub>3</sub> production rate but had a negative impact on the Faradaic efficiency (FE) in both modes. A maximum production rate of 4.6 mg h<sup>-1</sup> cm<sup>-2</sup> (FE = 44%) and a highest FE of 97.6% (NH<sub>3</sub> production = 1.12 mg h<sup>-1</sup> cm<sup>-2</sup>) were achieved, respectively, at -0.53 and -0.13 V vs RHE in the single-electrocatalysis mode. The tandem-electrocatalysis system significantly increased the production rate to 7.3 mg h<sup>-1</sup> cm<sup>-2</sup> (FE = 38.1%) at -0.53 V vs RHE (Figure 3c) (see Figures S6–S10 for more comparative results).

The air plasma produced a substantial NO<sub>x</sub> concentration (up to 1.87% with NO:NO<sub>2</sub> ≈ 5:1) for subsequent eNO<sub>x</sub><sup>-</sup>RR process. To elucidate the origin of NH<sub>3</sub> in eNO<sub>x</sub><sup>-</sup>RR, we

measured the concentrations of NO<sub>2</sub><sup>-</sup>, NO<sub>3</sub><sup>-</sup>, and NH<sub>4</sub><sup>+</sup> in the electrolyte during plasma discharge with and without electrocatalysis. NO<sub>2</sub><sup>-</sup> was found to be the dominant NO<sub>x</sub><sup>-</sup> (Figure 3d) with a formation rate of 28 mM h<sup>-1</sup>, and it was significantly consumed in the presence of electrocatalysis, strongly indicating that NH<sub>3</sub> is primarily produced from NO<sub>2</sub><sup>-</sup> (referred to as eNO<sub>2</sub><sup>-</sup>RR hereafter).

The catalyst stability was validated by successive repetitive (24 times in 24 h) tests at -0.33 V vs RHE (Figure 3e). The scanning electron microscopy (SEM) images of the N-MoS<sub>2</sub>/VGs catalyst before and after stability tests revealed no noticeable morphological changes (Figure S13). To confirm the origin of nitrogen for the produced NH<sub>3</sub>, we conducted an isotopic labeling experiment using <sup>15</sup>N<sub>2</sub>. Consistent with the standard sample, the spectra in Figure 3f exhibited two and three characteristic peaks indexed to <sup>15</sup>NH<sub>4</sub><sup>+</sup> and <sup>14</sup>NH<sub>4</sub><sup>+</sup>. Moreover, their production rates determined by NMR spectroscopy exhibited insignificant differences (Figure S14), excluding the influence of the surroundings. Remarkably, the system achieved a maximum NH<sub>3</sub> production rate of 7.3 mg h<sup>-1</sup> cm<sup>-2</sup>, which is almost 100 times higher than that of state-of-the-art MoS<sub>2</sub> eNRR<sup>22–24,48–70</sup> and over 2 times better than that of other hybrid systems (Figure 3g).<sup>30,36,37</sup>



**Figure 4.** (a) Differential charge densities of adsorbed NO<sub>2</sub><sup>-</sup> on 1T-MoS<sub>2</sub> and 2H-MoS<sub>2</sub>. (b) DOS plots of 1T-MoS<sub>2</sub> and 2H-MoS<sub>2</sub>. (c) HER and (d) NRR Gibbs free energy diagrams on various adsorption sites.

Moreover, we conducted DFT calculations to elucidate the enhanced eNO<sub>2</sub><sup>-</sup>RR kinetics of the N-MoS<sub>2</sub> system (see Section S-VII-1 in the Supporting Information (SI) for details). Our simulation model (Figure S15) featured N-MoS<sub>2</sub>(100) with S vacancies, which correlated with the catalyst characterization results. Figures 4a, S16, and S17 illustrate significant differences in the differential charge density of adsorbed NO<sub>2</sub><sup>-</sup> on 2H and 1T phases of MoS<sub>2</sub>. In the 1T phase, the electron accumulation (yellow areas) and electron loss (blue areas) are more extensive, reflecting greater electron delocalization. Bader charge calculations<sup>71</sup> revealed that NO<sub>2</sub><sup>-</sup> chemisorption is more favorable on the metastable 1T-MoS<sub>2</sub>, with an average charge transfer of  $-0.86e$ , compared to  $-0.79e$  on 2H-MoS<sub>2</sub>. Furthermore, Figure 4b compares the densities of states (DOS) of 1T-MoS<sub>2</sub> and 2H-MoS<sub>2</sub>, showing that the d-band center position of 1T-MoS<sub>2</sub> ( $\epsilon_{d2} = -3.99$  eV) is closer to the Fermi level ( $E_F$ ) than that of 2H-MoS<sub>2</sub> ( $\epsilon_{d2} = -4.17$  eV), which favors NO<sub>2</sub><sup>-</sup> adsorption. The partial density of states also indicates that 1T-MoS<sub>2</sub> has a larger overlap of the Mo d valence orbitals with the N p valence orbitals than 2H-MoS<sub>2</sub> (Figure S18), suggesting that 1T-MoS<sub>2</sub> has more occupied Mo orbitals and a stronger binding with N atoms from adsorbates such as NO<sub>2</sub><sup>-</sup>.

We also investigated various adsorption sites of NO<sub>2</sub><sup>-</sup> and H<sup>+</sup> on N-MoS<sub>2</sub>, including Mo top distal (TD), Mo–Mo bridge distal (BD), Mo with N-doped sites (ND), and Mo with S vacancy sites (SV) (Figure S19). We found that eNO<sub>2</sub><sup>-</sup>RR is inhibited on VGs due to the extremely high adsorption energy (1.54 eV; Table S3). As shown in the Gibbs free energy diagrams for HER in Figure 4c, compared to the adsorption sites for pristine MoS<sub>2</sub> ( $\Delta G_{BD}^{*H} = -0.06$  eV and  $\Delta G_{TD}^{*H} = 0.02$  eV), N-doped sites and S vacancy sites in N-MoS<sub>2</sub> ( $\Delta G_{ND}^{*H} = 1.17$  eV and  $\Delta G_{SV}^{*H} = 0.41$  eV) yield higher

energy barriers, confirming that the enhanced eNO<sub>2</sub><sup>-</sup>RR selectivity correlates with the suppression of HER. Importantly, the free energy changes of the eNO<sub>2</sub><sup>-</sup>RR pathways at different adsorption sites (Figure 4d; see Figures S21–S25 for more details) indicate that the energy barrier of the potential-determining step (PDS) for eNO<sub>2</sub><sup>-</sup>RR in N-doped MoS<sub>2</sub> ( $\Delta G_{ND}^{PDS} = 0.43$  eV and  $\Delta G_{SV}^{PDS} = 0.68$  eV) exhibits significantly better eNO<sub>2</sub><sup>-</sup>RR preference than MoS<sub>2</sub> ( $\Delta G_{TD}^{PDS} = 1.19$  eV and  $\Delta G_{BD}^{PDS} = 1.67$  eV). These findings lead us to conclude that 1T-MoS<sub>2</sub> facilitates stronger binding and faster electron transfer and that Mo with N doping and S vacancies is beneficial for NH<sub>3</sub> synthesis.

The optimal energy cost of the system is 1.41 MJ mol<sub>NH<sub>3</sub></sub><sup>-1</sup> for plasma NO<sub>x</sub> generation and 0.99 MJ mol<sub>NH<sub>3</sub></sub><sup>-1</sup> for eNO<sub>2</sub><sup>-</sup>RR, yielding a total energy cost of 2.4 MJ mol<sub>NH<sub>3</sub></sub><sup>-1</sup>. This corresponds to a total of 39.2 kWh kg<sub>NH<sub>3</sub></sub><sup>-1</sup>, which is at least 24.5% lower than that of the state-of-the-art plasma electrocatalysis systems (Table S7). Moreover, the proposed system has the potential to be extended to a cascade system by coupling plasma with multistage electrocatalyst cells, which can be powered flexibly by intermittent renewable electricity (Tables S8 and S9).

## CONCLUSIONS

In summary, we have developed a plasma tandem-electrocatalysis system for NH<sub>3</sub> synthesis directly from air, achieving an impressive NH<sub>3</sub> production rate of 7.3 mg h<sup>-1</sup> cm<sup>-2</sup> at  $-0.53$  V vs RHE. We engineered a novel defective N-MoS<sub>2</sub>/VGs electrocatalyst, which incorporates metallic 1T-MoS<sub>2</sub> phase, N doping, and S vacancies through a one-step plasma engraving process. Experimental and DFT investigations confirmed the crucial role of plasma engraving in catalyst

fabrication. The adsorption sites of Mo with N doping and S vacancies possess a lower energy barrier for PDS for  $\text{NH}_3$  formation than for  $\text{H}_2$  generation, explaining the enhanced  $\text{eNO}_2\text{-RR}$  performance. This system provides a carbon-free and sustainable approach to  $\text{NH}_3$  synthesis with an enhanced production rate. It also serves as a promising solution for chemical storage of carbon-neutral fuels with high location and scale flexibility, adapting readily to the irregular supply of renewable electricity.

## EXPERIMENTAL SECTION

### Plasma Tandem-Electrocatalysis Setup

The plasma tandem-electrocatalysis system used in this study is schematically shown in Figure S1. A small-scale atmospheric gliding arc plasma (GAP) reactor was designed to generate  $\text{NO}_x$  from air. The reactor consisted of a stainless steel inner anode rod with a diameter of 4 mm and a length of 58 mm and an outer cathode shell (grounded) with a convergent nozzle having a diameter of 21 mm and a thickness of 7.5 mm. The plasma discharge was powered by an AC high voltage power supply (GK-10020L). Dry air was fed into the reactor at a flow rate of  $9 \text{ L min}^{-1}$ , which was controlled by a mass flow controller (MFC, TJ-700C). The arc was ignited at the narrowest gap (kept at 1 mm). The GAP reactor had three radial gas inlets to create more intense flow disturbances inside the reactor, allowing for the formation of an extended plasma area. The reactive plasma system effectively activated the nitrogen bond, leading to the formation of  $\text{NO}_x$ . To quantify the  $\text{NO}_x$  produced with high concentration ( $\text{NO}$  and  $\text{NO}_2$ ), the outlet gas was diluted with pure nitrogen and measured using a gas analyzer (MRU VARIO). The generated  $\text{NO}_x$  was continuously fed into the electroreduction cells (single or tandem) for 1 h, absorbed by the alkaline electrolyte, and catalyzed into  $\text{NH}_3$ .

### Catalyst Synthesis

VG arrays were first prepared using an RF PECVD method powered by a high-frequency generator (Kmate, HERO-500 W, 13.56 MHz). A piece of CC was used as the substrate and thoroughly rinsed before use. First, the CC was placed in a quartz tube with a diameter of 48 mm and a length of 1000 mm, and the entire process was carried out under low-pressure conditions ( $\sim 0.5$  Torr), which is vital for the growth of graphene. Subsequently, a mixed gas of methane ( $\text{CH}_4$ ), hydrogen ( $\text{H}_2$ ), and argon (Ar) was then introduced at a total flow rate of  $35 \text{ mL min}^{-1}$  ( $\text{CH}_4$ :  $20 \text{ mL min}^{-1}$ ;  $\text{H}_2$ :  $5 \text{ mL min}^{-1}$ ; Ar:  $10 \text{ mL min}^{-1}$ ). The RF plasma was generated at 500 W for 10 min, resulting in the decoration on the CC substrate.

$\text{MoS}_2$  nanosheets were fabricated using a conventional hydrothermal method. The VGs obtained were immersed in a homogeneous solution containing 4.8 mmol of  $\text{Na}_2\text{MoO}_4 \cdot 2\text{H}_2\text{O}$  (sodium molybdate dihydrate), 20 mmol of  $\text{CH}_3\text{CSNH}_2$  (thioacetamide), and 80 mL of deionized water after vigorous stirring for 30 min. Then the mixture was transferred to a Teflon-lined autoclave, and the temperature was maintained at  $200^\circ\text{C}$  for 12 h. The obtained sample was then annealed at  $300^\circ\text{C}$  to obtain  $\text{MoS}_2/\text{VG}$  arrays. The  $\text{MoS}_2/\text{VGs}$  sample was further treated with RF plasma under an  $\text{NH}_3$  atmosphere at a flow rate of  $40 \text{ mL min}^{-1}$  for 20 min to obtain  $\text{N-MoS}_2/\text{VGs}$ .

### Catalyst Characterizations

Field-emission SEM images were recorded using a Hitachi SU8010. TEM images, EDX elemental mappings, and a SAED pattern were collected using a JEOL 2100F microscope. HAADF images were collected using a JEM-ARM200F microscope. XRD patterns were obtained using Cu  $K\alpha$  radiation on a Rigaku D/Max-2550 diffractometer. Raman spectra were collected using a Renishaw-in Via Raman microscope with 514 nm laser excitation. XPS was obtained using an ESCALAB\_250Xi X-ray photoelectron spectrometer. Specific surface area distributions were determined using a JW-BK112 analyzer. EPR spectra were taken using a JES FA-200 continuous-wave spectrometer with a sweeping magnetic field and an

X band (9.2 GHz) at room temperature. Details of these methods are available in SI.

## ASSOCIATED CONTENT

### Supporting Information

The Supporting Information is available free of charge at <https://pubs.acs.org/doi/10.1021/jacsau.3c00087>.

Additional experimental details and methods; energy consumption calculations; phase transformation and kinetic enhancement enabled by plasma engraving; calibration curves of  $\text{NH}_4^+$  and  $\text{N}_2\text{H}_4$  and  $^1\text{H}$  NMR spectra, chronoamperometry curves, UV-vis absorption spectra, and NRR performance for each reaction; morphology of the catalyst before and after stability tests; ammonia quantification by  $^{15}\text{N}$  and  $^{14}\text{N}$  isotope labeling; DFT calculation details; energy consumption comparison of plasma  $\text{NO}_x$  generation and  $\text{eNO}_2\text{-RR}$ ; summary of reported ammonia syntheses in conventional eNRR and plasma tandem-electrocatalysis systems; and summary of reported solar-powered plasma setups and solar-driven electrocatalysis and tables of performance comparison (PDF)

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#J.Z. and H.Z. contributed equally. CRediT: **Jiageng Zheng** formal analysis, investigation, writing-original draft; **Hao Zhang** conceptualization, formal analysis, supervision, writing-original draft, writing-review & editing; **Jiabao Lv** formal analysis, investigation, writing-original draft; **Meng Zhang** validation, writing-review & editing; **Jiaying Wan** investigation, validation; **Nick Gerrits** formal analysis, investigation, validation, writing-review & editing; **Angjian Wu** validation; **Bingru Lan** investigation; **Weitao Wang** formal analysis, investigation, validation; **Shuangyin Wang** supervision, writing-review & editing; **Xin Tu** conceptualization, project administration, supervision, writing-review & editing; **Anne-mie Bogaerts** supervision, writing-review & editing; **Xiaodong Li** conceptualization, funding acquisition, project administration, supervision, writing-review & editing.

### Notes

The authors declare no competing financial interest.

### ACKNOWLEDGMENTS

This work was supported by the National Natural Science Foundation of China (51976191, 5227060056, 52276214) and the National Key Technologies R&D Program of China (2018YFE0117300). N.G. was financially supported through an NWO Rubicon Grant (019.202EN.012). X.T. acknowledges the support of the Engineering and Physical Sciences Research Council (EP/X002713/1).

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