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1 Dehazing redox homeostasis to foster purple bacteria biotechnology

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14 Abstract

15 Purple non-sulfur bacteria (PNSB) show great potential for environmental and industrial
16 biotechnology, producing microbial protein, biohydrogen, polyhydroxyalkanoates (PHA),
17 pigments, etc. Grown photoheterotrophically, the carbon source is typically more reduced than
18 PNSB biomass, which leads to a redox imbalance. To mitigate the excess of electrons, PNSB
19 can exhibit several ‘electron sinking’ strategies such as CO₂ fixation, N₂ fixation, H₂ and PHA
20 production. The lack of a comprehensive (over)view of these redox strategies is hindering the
21 implementation of PNSB for biotechnology applications. This review paper aims to present the
22 state of the art of redox homeostasis in phototrophically grown PNSB, presenting known and
23 theoretically expected strategies and discussing them from stoichiometric, thermodynamic,
24 metabolic and economic points of view.

25
26 **Keywords:** purple phototrophic bacteria; alternative protein; polyhydroxybutyrate; resource
27 recovery; hydrogen economy; nitrogen fixation

28 Glossary

- 29 • **Bacteriochlorophyll:** Pigment molecule located in the reaction center.
- 30 • **Carbon capture and utilization:** Processes focusing on the capture of CO₂ and reduction
31 with H₂ or electricity to form high-value chemicals such as formate or methanol.
- 32 • **Electron sinking:** Mechanism or strategy to reoxidize metabolic cofactors, deal with the
33 excess of electrons and maintain redox homeostasis.
- 34 • **Gibbs free energy:** Measure to define the thermodynamic equilibrium and direction of a
35 reaction. Reactions with a positive change in Gibbs free energy (endergonic reactions)
36 require external energy input and will not occur spontaneously in that direction, while
37 reactions with a negative change in Gibbs free energy (exergonic reactions) will release
38 energy and can occur spontaneously in that direction. Reactions are in equilibrium if the
39 change in Gibbs free energy is equal to zero.
- 40 • **Membrane potential:** Charge gradient over the bacterial membrane and driving force for
41 metabolic reactions such as ATP synthesis.
- 42 • **Microbial fertilizer:** The use of microbial biomass as organic fertilizer for plant growth.
- 43 • **Microbial protein:** The use of microbial biomass as protein ingredient for human food and
44 animal feed applications.
- 45 • **Phototrophic growth:** Growth mode using light as energy source.
 - 46 ○ **Anoxygenic photosynthesis:** Phototrophic growth without oxygen production.
 - 47 ○ **Photoautotrophic growth:** Phototrophic growth with CO₂ as carbon source.
 - 48 ○ **Photoheterotrophic growth:** Phototrophic growth with organics as carbon and
49 electron source simultaneously.
- 50 • **Proteobacteria:** A phylum of prokaryotes, mainly dominated by Gram-negative bacteria,
51 covering a wide variety of morphologic and metabolic traits.
- 52 • **Reaction center:** Membrane-bound protein complex converting light energy into chemical
53 energy through photooxidation and release of reduced electron transporters.
- 54 • **Redox homeostasis:** Maintenance of the oxidation degree of the cell interior milieu as
55 opposed to the oxidation degree of the exterior environment.
- 56 • **Stoichiometry:** Quantitative association between substrates and formed products in a
57 chemical reaction.
- 58 • **Thermodynamics:** Energetic relationship between substrates and formed products in a
59 chemical reaction.

60 **1 Redox homeostasis in phototrophically grown PNSB**

61 Purple non-sulfur bacteria (PNSB), a group of microbes belonging to the alpha- and beta-
62 **Proteobacteria**, have attracted the curiosity of microbiologists and engineers for decades due
63 to their metabolic versatility and potential for synthesis of societal and economic relevant
64 bioproducts [1]. There is a growing interest in implementing PNSB for environmental and
65 industrial biotechnology applications such as wastewater treatment, bioremediation and
66 production of **microbial protein, microbial fertilizer**, biohydrogen, bioplastics and pigments
67 [2-6]. Especially for wastewater treatment, applications are accelerating these last five years
68 with the construction of pilot and demo scale reactors in Australia [7], India
69 (<https://projectsaraswati2.com/>) and Spain (<https://deep-purple.eu/>; <https://incover-project.eu/>).
70 For biotechnology applications, PNSB are usually explored
71 **photoheterotrophically** where they use light as energy source through **anoxygenic**
72 **photosynthesis** and various organics such as volatile fatty acids (VFA), carbohydrates and
73 amino acids as carbon and electron source [2,8-11]. As for all microbes, PNSB ought to
74 maintain their internal **redox homeostasis** by balancing redox power-producing and
75 consuming pathways. This is particularly challenging when PNSB grow **phototrophically**
76 under anaerobic conditions on carbon sources more reduced than the biomass such as
77 propionate, butyrate or longer chain VFA (Box 1).

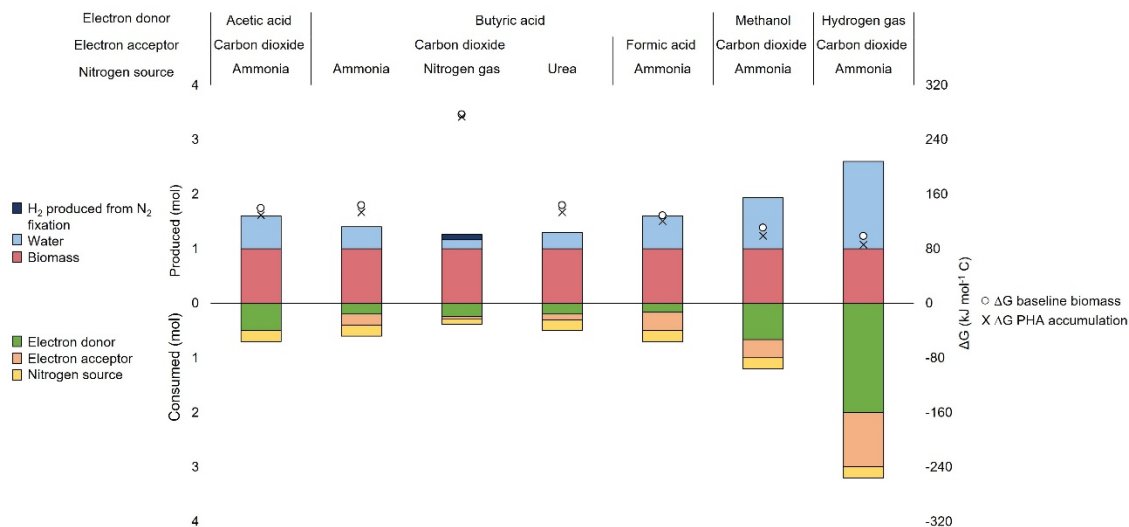
78 Researchers discovered two main ‘**electron sinking**’ strategies in PNSB to deal with
79 this excess of redox power, namely CO₂ fixation through the Calvin cycle and H₂ production
80 (Box 1, Figure I, Key Figure). More recently, several additional metabolic pathways were
81 proposed that participate in redox homeostasis such as polyhydroxyalkanoate (PHA) or
82 isoleucine production [12-14]. A fundamental understanding of redox homeostasis is essential
83 for PNSB biotechnology because these ‘electron sinking’ strategies are often exploited to
84 channel the excess of reducing power to the synthesis of biomass (proteins), PHA or H₂.
85 Despite decades of research, a comprehensive (over)view of redox balancing strategies in
86 phototrophic grown PNSB is missing. Key insights on redox homeostasis remain scattered and
87 recent developments are not yet or only partly picked up by microbial biotechnologists. This
88 review paper aims to present the state of the art of redox homeostasis in phototrophically grown
89 PNSB, presenting known and theoretical strategies and discussing them from **stoichiometric**,
90 **thermodynamic**, metabolic and economic points of view. This will help fundamental scientists

91 to better comprehend the metabolic maze of PNSB and assist applied researchers to pinpoint
 92 novel microbial control tools for the production of value-added bioproducts.

93 2 Stoichiometric and thermodynamic considerations of redox homeostasis

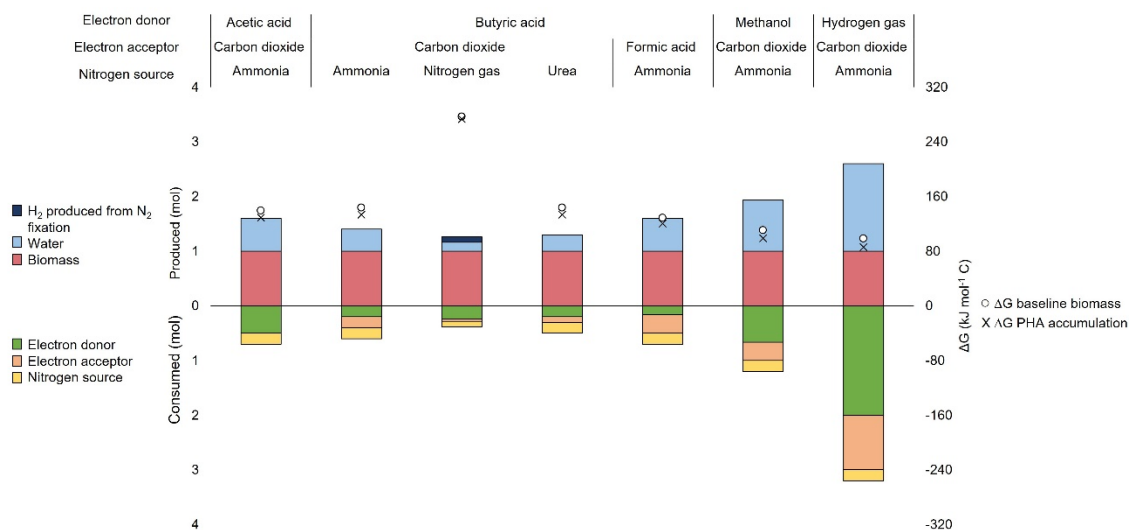
94 The established microbiology theoretical concepts to derive stoichiometries and
 95 thermodynamics are essential to acquiring a fundamental understanding of the catabolic and
 96 anabolic needs and products (Box 2). Element and electron balancing yields stoichiometry, and
 97 the bioenergetics allow judging whether biochemical reactions are possible in natural and
 98 engineered environments [15].

99 For phototrophically grown PNSB, the catabolism consists of anoxygenic
 100 photosynthesis generating the required energy, conserved in the form of ATP to drive the
 101 energy-consuming anabolic reaction. The stoichiometry reaction for growth reflects the
 102 anabolic substrates and products. The more positive the **Gibbs free energy** ΔG (endergonic),
 103 the higher the photosynthetic energy requirement (



104
 105 Figure 1). Two main groups of electron sources are, currently, key in PNSB
 106 biotechnology: (i) VFA such as acetate, propionate and butyrate, for instance, generated
 107 through acidogenic fermentation of solid and liquid waste streams [16,17] and (ii) H₂ and C1
 108 compounds derived from CO₂ reduction (e.g. formate and methanol), relevant in the context of
 109 the H₂ economy and **carbon capture and utilization** processes [18,19].

110 Balancing stoichiometries based on these industrially relevant electron donors yields
 111 several theoretical insights into electron balancing needs (

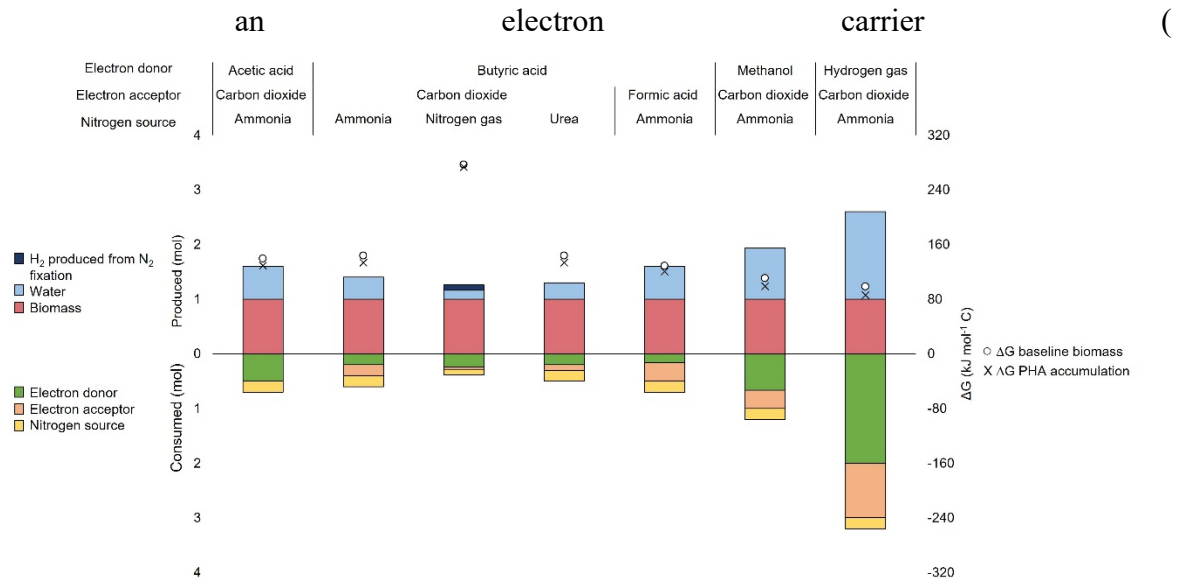


112
 113 Figure 1). For VFA, growth of PNSB on acetate, for example, should theoretically not
 114 require CO₂ fixation through the Calvin cycle because the electron content is the same as for
 115 biomass (4 mol e⁻ mol⁻¹ C; electron content relative to CO₂-C excl. PHA production; Box 1,
 116 Figure 1). However, Laguna et al. [20] have shown that a *Rhodospseudomonas palustris* strain
 117 was unable to grow on acetate when the genes involved in the Calvin cycle were deleted. A
 118 similar observation was made for *Rhodospirillum rubrum*, which benefits from the presence of
 119 bicarbonate for phototrophic growth [21]. Cerruti et al. [22], on the other hand, observed a net
 120 CO₂ production for a *Rps. palustris* strain grown on acetate. Different elemental compositions
 121 and, thus, different biomass electron contents might explain this discrepancy of CO₂ fixation
 122 vs. production. For *Rs. rubrum*, a lower biomass electron content compared to acetate has been
 123 reported (3.7-4.2 vs. 4.0 mol e⁻ mol⁻¹ C_{biomass}; Box 1, Figure 1) [23]. Growth of *Rs. rubrum* on
 124 acetate would, therefore, require some degree of redox balancing.

125 Developments in carbon capture and utilization processes will open new routes for the
 126 production of building blocks such as methanol and formate for the chemical industry and
 127 biotechnology [18,24,25]. Photoassimilation of these carbon sources has been observed for
 128 several PNSB such as *Rhodobacter sphaeroides*, *Rps. palustris* and *Rps. acidophila* [26-28].
 129 From a metabolic perspective, methanol is first converted to formate through a cascade of
 130 enzymes including methanol dehydrogenase, formaldehyde dehydrogenase and S-
 131 formylglutathione hydrolase [27]. For each mole of methanol, 2 moles NAD(P)H are
 132 generated. To assimilate the carbon to biomass, formate is eventually converted to CO₂ through
 133 the enzyme formate dehydrogenase generating an additional amount of 2 moles NAD(P)H. The
 134 CO₂ is finally fixated through the Calvin cycle using 4 moles NAD(P)H. For formate, however,

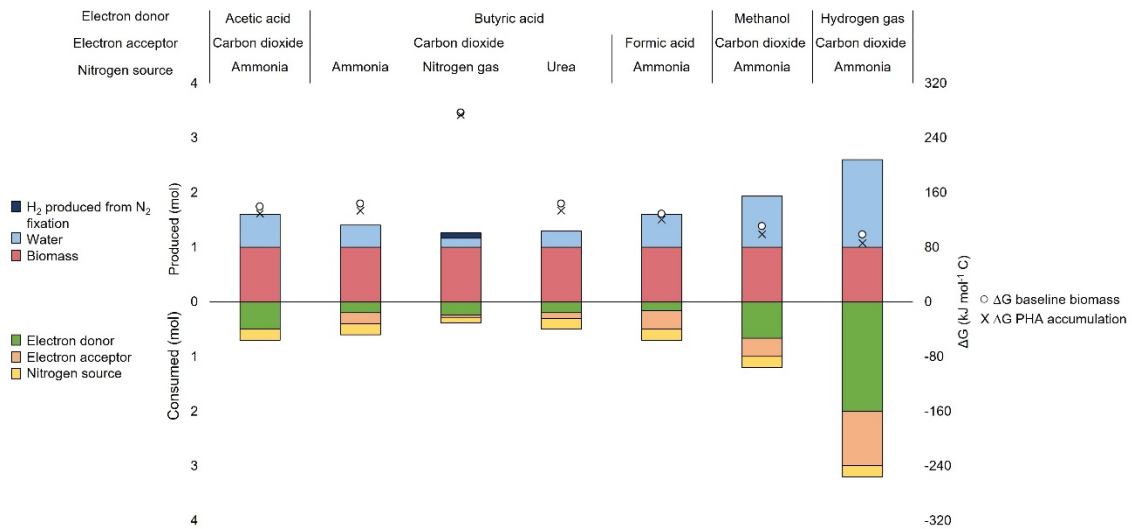
135 a net input of NAD(P)H is required because the Calvin cycle requires more NAD(P)H than
 136 generated from the oxidation of formate. Formate will, therefore, act as an electron acceptor
 137 for phototrophic growth on reduced carbon sources. Compared to CO₂, formate can be
 138 considered a less efficient electron acceptor because it contains a higher amount of electrons
 139 (Box 1, Figure I). More moles of formate are, therefore, required per mole carbon assimilated
 140 compared to CO₂.

141 The nitrogen source seems to have an important role in redox homeostasis as it can also
 142 be



143
 144 Figure I). N₂ fixation, a common metabolic trait of PNSB, will decrease the CO₂
 145 fixation requirement because the nitrogenase enzyme consumes electrons (8 mol e⁻ mol⁻¹ N₂
 146 fixed). This is also true if urea (0 mol e⁻ mol⁻¹ N; Box 1, Figure I) is used as a nitrogen source,
 147 only requiring 0.1 mol CO₂ mol⁻¹ C_{biomass} for photoheterotrophic growth on butyrate (excl. PHA
 148 or H₂ production). External CO₂ requirements are probably lower because hydrolysis of urea
 149 releases one mole of CO₂. Equal amounts of CO₂ will, hence, be fixed during growth on urea
 150 as would be required for photoheterotrophic growth on NH₃.

151 In terms of thermodynamics, all anabolic reactions on NH₃ and organics require roughly
 152 the same photosynthetic energy regardless of the electron donor or acceptor (98-144 kJ mol⁻¹



154

155 Figure 1). There is, however, a great discrepancy in energy need compared to
 156 phototrophic growth on N_2 ($274 \text{ kJ mol}^{-1} C_{\text{biomass}}$). N_2 fixation is an energy-intensive pathway,
 157 which requires 8 moles of ATP per mole N assimilated for molybdenum nitrogenase [29]. The
 158 thermodynamic advantage of the Calvin cycle is probably the reason why it is favored as redox
 159 balancing mechanism over N_2 fixation combined with H_2 production. Recently, H_2 production
 160 for phototrophic growth of *Rs. rubrum* on a mixture of butyrate and propionate in the presence
 161 of NH_3 was observed [30]. The nitrogenase enzyme can also, in the absence of N_2 and NH_3 ,
 162 channel all electrons to H_2 production without N_2 fixation. This is typically performed by
 163 sparging photobioreactors with argon [29]. Photoheterotrophic growth on NH_3 as nitrogen
 164 source and butyrate as carbon source, using a hydrogenase enzyme to dump excess reducing
 165 power, would require $155 \text{ kJ mol}^{-1} C_{\text{biomass}}$. This is thermodynamically more appealing than the
 166 N_2 fixation route, yet less energy efficient compared to the Calvin cycle. Thermodynamics fall
 167 short to clarify the observed H_2 production in the presence of NH_3 and there is, thus far no
 168 metabolic explanation (section 3.1).

169 Next to CO_2 fixation and H_2 production, PNSB can also accumulate PHA as carbon and
 170 energy storage. PHA accumulation is, from a thermodynamic perspective, slightly more
 171 appealing as redox balancing mechanism compared to CO_2 fixation ($86\text{-}133$ vs. $98\text{-}144 \text{ kJ mol}^{-1}$
 172 C_{biomass}). It can, therefore, be anticipated that PNSB shift towards a combination of CO_2
 173 fixation and PHA accumulation when conditions are favorable (e.g. carbon source preferably
 174 VFA, high carbon to nitrogen ratios and high light intensity) [31]. This ‘hierarchy’ in redox
 175 balancing was also observed by Cerruti et al. [22], showing that the electrons first flow to CO_2
 176 fixation and PHA production and only secondary to H_2 production when PHA storage is
 177 saturated. These experiments were performed with continuous illumination and with light-dark

178 cycles. Constant CO₂ production of 0.075 mmol h⁻¹ was observed during continuous
179 illumination. During light-dark cycles, CO₂ peaks appeared. Only minor levels of H₂ were
180 produced (0.025 mmol h⁻¹). Cerruti et al. [22], therefore, concluded that H₂ production did not
181 play a major role in redox homeostasis for their experiments.

182 Overall, the thermodynamic analysis helps to understand which redox balancing
183 strategy is more appealing from an energy perspective (lowest ΔG). Even for the
184 photoheterotrophic PNSB that generate their energy from cyclic photophosphorylation (BOX
185 1), light can be limiting and, thus, metabolic choices need to be made to balance energy
186 production, consumption and redox stress. These choices in terms of redox strategies are
187 partially regulated by gene expression. Masepohl [32] has written an extensive review on the
188 regulation of N₂ fixation for *Rs. rubrum*, *Rps. palustris* and *Rb. capsulatus*. N₂ fixation
189 apparently responds to NH₃, oxygen, light, molybdenum and iron. For *Rb. capsulatus*, for
190 example, in the absence of NH₃, the NtrC protein is phosphorylated which then activates the
191 expression of the nifA genes leading to N₂ fixation through molybdene nitrogenase activity.
192 An increase in NH₃ results in dephosphorylation of the NtrC protein and inhibition of the NifA
193 proteins. Oxygen also influences N₂ fixation by inhibiting nitrogenase activity.

194 **3 Metabolic considerations of redox homeostasis**

195 **3.1 Key redox strategies for phototrophic growth on volatile fatty acids**

196 Since the first scientific discovery of PNSB in 1931, no systematic overview of redox
197 homeostasis has been described thus far [33]. In the following section, five key ‘electron
198 sinking’ strategies essential for the phototrophic growth of PNSB are proposed.

199 The role of the Calvin cycle as redox balancing mechanism in PNSB has been well
200 established by using mutants deleted of key enzymes (e.g. RuBisCO or phosphoribulokinase)
201 [34,35]. The Calvin cycle is effective in reoxidizing the reduced cofactors because the fixation
202 of one mole CO₂ oxidizes two moles of NADPH (Figure 2). In terms of energy use, the Calvin
203 cycle consumes three moles of ATP per fixed CO₂. For VFA assimilation, alternative carbon
204 fixation routes have been observed in PNSB namely, the ethylmalonyl-CoA pathway and
205 reverse tricarboxylic acid pathway. Researchers demonstrated that the ethylmalonyl-CoA
206 pathway is mainly used in PNSB during acetate and butyrate assimilation [21,36,37]. When
207 using the ethylmalonyl-CoA pathway for acetate assimilation to 2-oxoglutarate, two moles CO₂
208 are fixed for every ATP consumed (Figure 2). Ethylmalonyl-CoA based acetate assimilation
209 also results in the reoxidation of four reduced cofactors. In terms of redox balancing strategies,

210 the Calvin cycle is, thus, more efficient than the ethylmalonyl-CoA, yet the latter consumes
211 lower levels of ATP. Some PNSB possess a functional glyoxylate shunt which is used for
212 acetate assimilation. In this case, assimilation of two moles acetate and one mole CO₂ to 2-
213 oxoglutarate does not lead to the reoxidation of reduced cofactors (Figure 2). PNSB species
214 that use the glyoxylate shunt for acetate assimilation, therefore, require a functional Calvin
215 cycle for carbon assimilation. Species that do not possess a functional glyoxylate shunt rely on
216 ethylmalonyl-CoA for acetate assimilation and, therefore, do not require the Calvin cycle for
217 redox balancing [20,38,39].

218 H₂ production, another key redox sink for phototrophically grown PNSB, is generated
219 by the activity of two types of enzymes namely hydrogenase and nitrogenase. Hydrogenase
220 can either produce or consume hydrogen gas, while nitrogenase can only produce hydrogen
221 gas [29]. Nitrogenase derepression was observed in RuBisCO mutants of *Rs. rubrum* and *Rb.*
222 *sphaeroides*, even in the presence of NH₃, probably through *regB* gene activity [40,41].

223 More recently, PHA production was proposed to serve as an ‘electron sinking’
224 mechanism, in addition to its more typical function as carbon storage [13,14,42,43]. From
225 acetate, the production of PHA effectively conduces to the reoxidation of cofactors which could
226 help cells deal with redox imbalance (Figure 2) [13,44]. This is, however, only transiently since
227 stored PHA are always reconsumed when the carbon source is limiting [31]. When propionate
228 or butyrate are assimilated, PHA synthesis does not act anymore as ‘electron sinking’
229 mechanism because no cofactor can be reoxidized during their synthesis (Figure 2). This is in
230 agreement with our observation for *Rs. rubrum*. Only acetate triggered high-level PHA
231 production, which was negatively influenced by the presence of bicarbonate [21,30,45-47]. A
232 sudden increase in light intensity, which also results in redox imbalance (Box 3), has been
233 shown to trigger PHA production [13], thereby, reinforcing the role of PHA in transient redox
234 balancing.

235 Just recently, it was observed that proteins from the branched-chain amino acid
236 synthesis and degradation pathways were often upregulated during VFA assimilation [9,13,21].
237 This new pathway could indeed represent an assimilation route converting acetyl-CoA to
238 propionyl-CoA and then 2-oxoglutarate. The rationale for the existence of such an alternative
239 assimilation route remains, however, unclear. The level of intracellular isoleucine was
240 subsequently observed to be significantly higher in conditions that trigger redox imbalance in
241 *Rs. rubrum*. Inhibiting the isoleucine synthesis by adding this amino acid to the environment
242 also delayed the growth of *Rs. rubrum* on acetate [12]. From three moles of acetyl-CoA, the
243 production of one mole of isoleucine allows the reoxidation of two reduced cofactors (Figure

244 2). Accumulation of isoleucine, could thus also be a way for *Rs. rubrum* to cope with redox
245 stress. Accumulation of isoleucine was also observed in response to light-induced redox stress
246 (Box 3). This newly proposed ‘electron sinking’ mechanism still requires definitive
247 demonstration (see Outstanding Questions).

248 The reverse tricarboxylic acid pathway could also be used by bacteria as an ‘electron-
249 sinking’ pathway for alpha-ketoglutarate production and its derived amino acid (Figure 2)
250 [42,48]. McCully et al. [49] recently demonstrated that the flux through the reverse
251 tricarboxylic acid pathway increased in a Calvin cycle mutant strain of *Rs. rubrum*, suggesting
252 its involvement in redox balancing. Such a compensatory mechanism is dependent on the
253 presence of adequate enzymes allowing fumarate reduction and reductive alpha-ketoglutarate
254 synthesis which is apparently not possible for all PNSB and notably not in *Rp. palustris*.

255 Auxiliary oxidants (e.g. trimethylamine N-oxide, dimethyl sulfoxide, sulfate, nitrate)
256 are also known electron acceptors that allow PNSB to reach redox homeostasis through
257 anaerobic respiration [50,51]. Formation of hydrogen sulfide from sulfate is also an alternative
258 respiratory mechanism for ‘electron sinking’, yet it is apparently not used as a compensatory
259 route in a Calvin cycle mutant strain of *Rs. rubrum* [49] [52]. Nitrate respiration to nitrite can
260 also be performed by PNSB that possess a dissimilatory nitrate reductase. Interestingly, *Rb.*
261 *sphaeroides* possesses two different Nap-type nitrate reductases [53], one being specifically
262 expressed under low oxygen levels which can thus also fulfill the role of ‘electron sinking’ in
263 the presence of nitrate.

264 Next to phototrophy on VFA, some PNSB species such as *Rb. sphaeroides* are also able
265 to use methanol [27]. This carbon source has a high electron content ($6 \text{ mol e}^- \text{ mol}^{-1} \text{ C}$; Box 1,
266 Figure I) and will, therefore, impose high levels of redox stress in phototrophically grown
267 PNSB. Thus far, research on the growth of PNSB on methanol is limited to studies from the
268 70s merely focusing on initial screening and growth characterization [28,54,55]. Redox
269 homeostasis strategies for methanol have never been described, yet are crucial with regards to
270 the developments in carbon capture and utilization processes [25].

271 **3.2 Complexity to elucidate: Mixed electron sources and open cultures**

272 For the photoassimilation of VFA, only CO₂ fixation and H₂ production have been analyzed to
273 some extent. The role played by anaerobic respiration and PHA or isoleucine synthesis in a
274 biotechnological relevant context still requires detailed analysis. An even greater knowledge
275 gap exists for growth on VFA mixtures, conditions more likely in natural and engineered
276 systems. Recently, it was observed that *Rs. rubrum* does not rely on bicarbonate

277 supplementation when a mixture of butyrate and propionate is supplied. Instead of using the
278 Calvin cycle for CO₂ fixation, *Rs. rubrum* turns to H₂ production [30]. Cultures growing on
279 VFA mixtures also perform better in terms of growth and resistance to redox stress [17,56], yet
280 how redox balancing is regulated remains largely unclear.

281 Differences in redox balancing strategies also exist between PNSB species. In terms of
282 carbon assimilation efficiency, for instance, variation was observed for different strains [17].
283 The genetic background also influences how PNSB respond to different carbon and electron
284 contexts [42,49] and notably the presence of a functional glyoxylate shunt is of major
285 importance for ‘electron sinking’ (Figure 2). This was demonstrated by Shimizu et al. [38] who
286 successfully increased H₂ production in *Rb. sphaeroides* by genetically introducing a functional
287 glyoxylate shunt.

288 Next to the five key ‘electron sinking’ strategies (section 3.1), differences in redox
289 balancing might also arise due to the particular enzyme deployed. For N₂ fixation, for example,
290 three structurally and phylogenetically isoforms exist namely, molybdenum, iron and
291 vanadium nitrogenase [57]. Luxem et al. [58] have shown for a *Rps. palustris* strain that these
292 nitrogenases have different H₂ production to N₂ fixation ratios, ranging from 0.9-1.4 mol H₂
293 mol⁻¹ N₂ for molybdenum nitrogenase and 3.9-6.9 mol H₂ mol⁻¹ N₂ for iron nitrogenase. The
294 extensive allocation of electrons to H₂ for each N₂ fixated in the iron nitrogenase strain
295 eventually leads to slower growth [58]. Additional research is required to elucidate whether
296 enzyme isoforms play a role in other redox pathways.

297 Next to experimental research, valuable insight on redox strategies can also be
298 extrapolated from genome-scale metabolic models and metabolic and expression models.
299 These models are a mathematical description of known metabolic pathways encoded in the
300 organism’s genome with or without cellular expression [59]. Chowdhury et al. [60], for
301 example, predicted that malate dehydrogenase and 3 phosphate dehydrogenase are essential to
302 maintain redox homeostasis in a *Rps. palustris* strain next to the Calvin cycle. Another
303 metabolic model for *Rps. palustris* predicted that the oxidation state of the quinone pool relates
304 to the CO₂ fixation rate, as the accumulation of reduced quinols will limit the electron flow and
305 ATP generation for the Calvin cycle [61]. A recent study by the same authors indicated that
306 high molecular weight and reduced carbon sources result in excess production of carbon and
307 NAD(P)H, which can be channeled to PHA production Alsiyabi et al. [62].

308 4 Economic considerations

309 In biotechnology, the redox balancing strategies described in previous sections are often
310 exploited to boost the flow of the excess of electrons to the synthesis of biomass (proteins),
311 PHA or H₂. In this section, a cost estimation of the main feedstocks allows assessing the
312 viability of several options for industrial biotechnology. This main feedstocks-based cost
313 estimation is a considerable fraction of the overall operational expenditure. It accounts for the
314 electron donor/acceptor and nitrogen source (Figure 3). It can, therefore, be anticipated that the
315 market price of the bioproduct, estimated as three times the main feedstock cost, ought to be
316 lower than the market price of their conventional alternatives. The particular bioprocess will,
317 otherwise, not be economically viable.

318 For PNSB applications as food or feed ingredient, a.k.a. microbial protein, surplus
319 redox power should mainly flow to microbial biomass (and hence protein). Replacing fishmeal
320 in aquaculture with protein-rich PNSB biomass [3,63] appears to be interesting for several
321 biotechnology routes as the selling price is comparable (Figure 3). Substituting soybean, on the
322 other hand, typically used as a feed ingredient for cattle and poultry, will not be sustainable
323 from an economic perspective. In terms of electron donor, growth on methanol appears to be
324 the most appealing route for microbial protein production. Research, however, on methanol
325 and C1-compounds is limited (section 3.1). Current developments in carbon capture and
326 utilization processes will probably make CO₂-derived methanol more interesting for PNSB
327 production in future research and applications [18,25]. In terms of VFA, only acetate shows to
328 be attractive (€474-947 ton⁻¹ biomass). Production of PNSB biomass on recovered VFA from
329 fermented waste streams may be more appealing than using synthetic VFA [16,17]. This would
330 avoid the cost of the electron donor and acceptor, yet might introduce new challenges such as
331 microbial selectivity for high PNSB abundance and stability in nutritional quality [17,64]. Next
332 to heterotrophy, PNSB are also able to grow **photoautotrophically** on H₂ and CO₂ as electron
333 donor and acceptor, respectively [19]. From a purely economic perspective, however,
334 photoautotrophic microbial protein production will be challenging as costs for the electron
335 acceptor are high because it is the only carbon source for the cell (€300-510 ton⁻¹ CO₂) [65,66].
336 Cultivation of PNSB as an added-value food ingredient might be more fit for this route,
337 especially with the growing interest in the H₂ economy [25].

338 Next to microbial protein, PNSB are also explored for PHA and H₂ production. Based
339 on the main feedstock cost estimation, particularly PHA shows to be interesting. PHA
340 production will result in a slight increase in cost relative to microbial protein production, yet

341 this will be offset by the higher market price of the commodity (€3,500-5,340 ton⁻¹ PHA) [67].
342 For H₂ production, waste streams are typically targeted because the market value of H₂ as
343 energy source is too low (€1300-1900 ton⁻¹ H₂) to even cover the feedstock costs [68].

344 **5 Concluding remarks and future perspectives**

345 Since the discovery of PNSB 91 years ago, they have predominantly been studied from a
346 microbiological perspective. Last years, however, there is a growing trend in implementing
347 PNSB for environmental and industrial biotechnology. Redox balancing is central here because
348 researchers and engineers aim to maximize the excess of electrons to the synthesis of PNSB
349 bioproducts. This paper is the first initiative to present a comprehensive (over)view of redox
350 homeostasis in phototrophically grown PNSB. From a stoichiometric perspective, we could
351 partly explain how differences in ‘electron sinking’ requirements occur for different carbon
352 and nitrogen sources. Growth on acetate and urea, for example, reduces redox stress for PNSB
353 relatively to butyrate or NH₃. Thermodynamics predict a ‘hierarchy’ in redox strategies.
354 ‘Electron sinking’ through CO₂ fixation and PHA accumulation is energetically more favorable
355 compared to H₂ production. From a metabolic perspective, several key redox strategies exist in
356 phototrophically grown PNSB namely, CO₂ fixation, PHA accumulation, H₂ and alpha-
357 ketoglutarate production and potentially intracellular isoleucine accumulation. Finally, the
358 economic feedstock estimation highlights opportunities for methanol and VFA as electron
359 donor for industrial biotechnology applications.

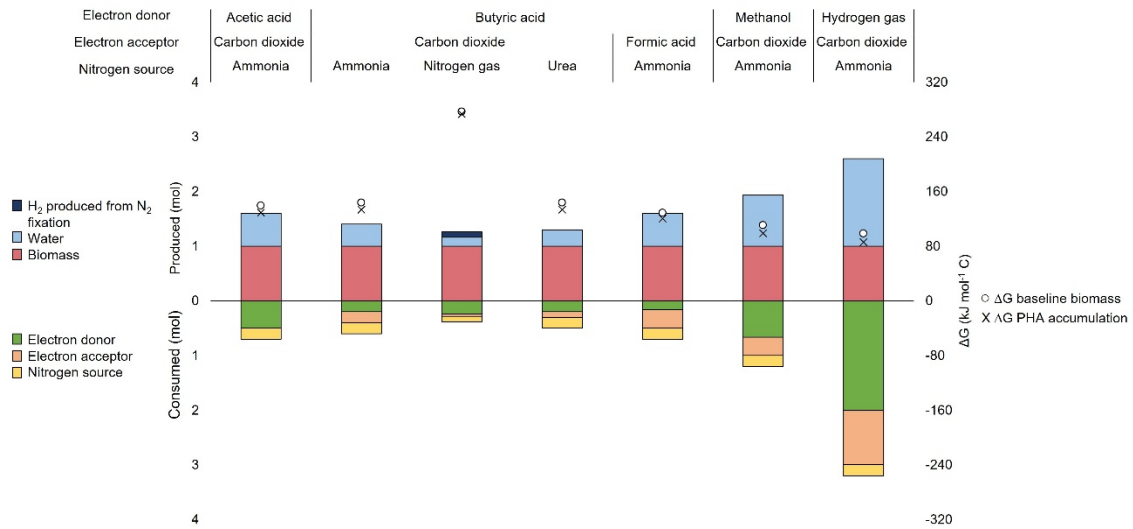
360 Future researchers should, first of all, focus on elucidating the ‘hierarchy’ in redox
361 balancing. This ‘hierarchy’ has been observed for a *Rps. palustris* strain [22], yet additional
362 research should confirm whether it is a general trait for PNSB (see Outstanding Questions).
363 Dedicated research initiatives on redox homeostasis are, therefore, necessary with a complete
364 characterization of the ‘electron sinking’ routes (i.e. CO₂, PHA, H₂ and isoleucine). How PNSB
365 deal with redox homeostasis when multiple carbon and electron sources are present remains
366 largely unexplored, even though this situation would be closer to natural and engineered
367 environments. The number of PNSB species studied should be expanded and the respective
368 gene clusters involved should also be characterized. This will allow for rapid *in-silico* testing
369 of the genetic capacity for certain redox strategies through genome mining (section 3.2). Redox
370 homeostasis in mixed cultures should also be studied because in natural and engineered
371 environments PNSB thrive in open communities with other (non-)PNSB species. First, it
372 should be explored whether there exists a kind of specialization in open PNSB cultures supplied
373 with mixtures of electron sources. PNSB communities may, for example, exhibit division of
374 labor, with PNSB species using different electron sources. Secondly, natural ecosystems and
375 photobioreactors are not continuously illuminated or anaerobic, triggering (an)aerobic

376 chemotrophy next to the central phototrophic metabolism. These potential shifts from
377 photosynthetic redox balancing to oxygen-driven ‘electron sinking’ need to be elucidated. The
378 next step for the economics requires a full cost assessment, taking capital and operational
379 expenditure into account as well as uncertainty. Dedicated life cycle assessment can support
380 the economic insights and help direct researchers to target the most sustainable and opportune
381 electron donors for the production of PNSB products.

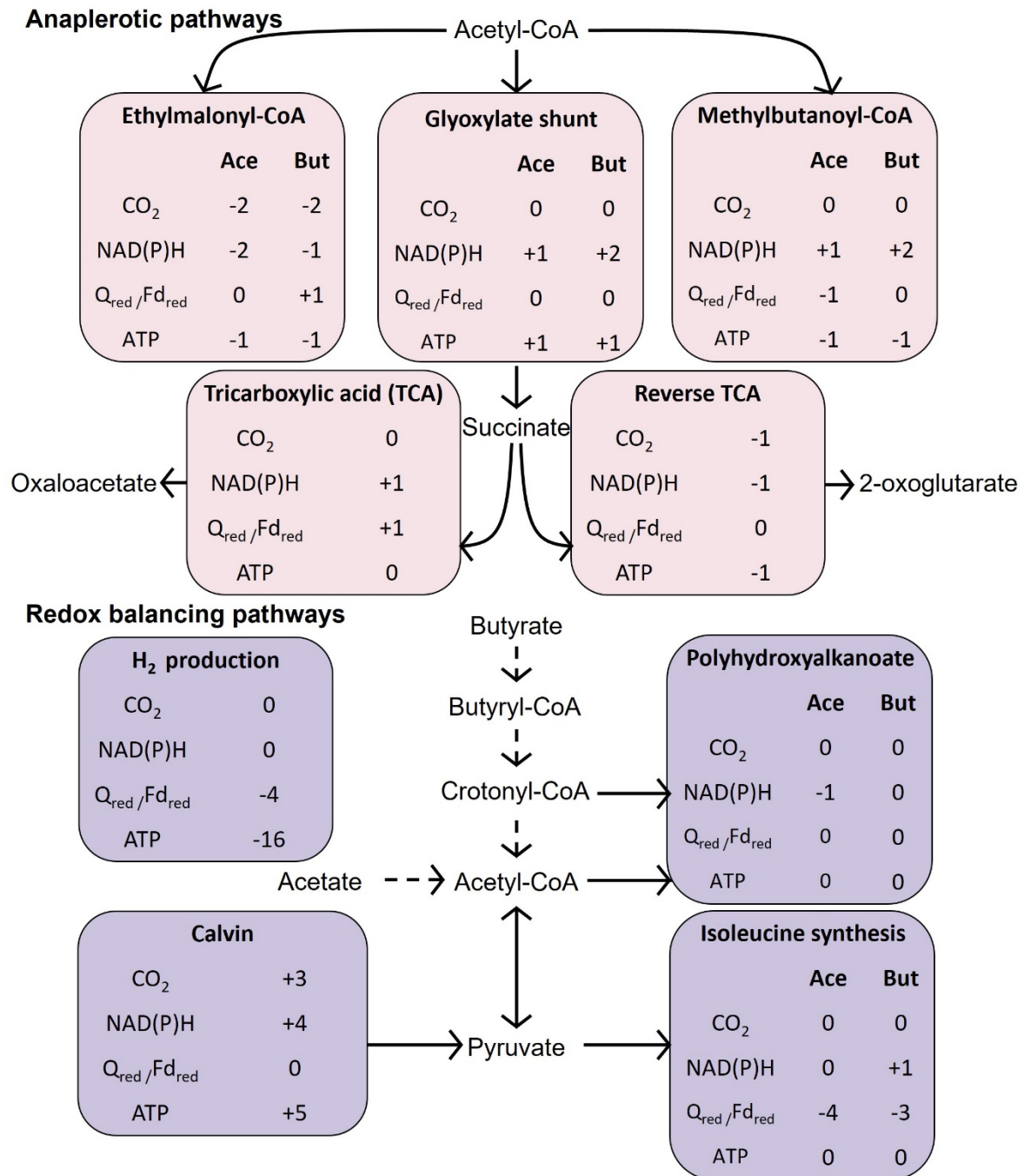
382 **Acknowledgments**

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389 **Figure legends**



390
 391 **Figure 1 Stoichiometry and thermodynamics for phototrophically grown purple bacteria**
 392 Theoretical stoichiometry on a molar basis (left y-axis) and associated Gibbs free energy
 393 requirements (right y-axis) for phototrophically grown purple bacteria on four electron donors,
 394 two electron acceptors and three nitrogen sources. For the stoichiometry, one scenario is shown
 395 based on biomass ($C_5H_7O_2N$) production excluding polyhydroxyalkanoates (PHA). Two Gibbs
 396 free energy scenarios were simulated: (i) biomass production without PHA, and (ii) biomass
 397 production including 20% of the electrons stored as PHA. PHA was composed of 50%
 398 polyhydroxybutyrate ($C_4H_6O_2$) and 50% polyhydroxyvalerate ($C_5H_8O_2$). Stoichiometries and
 399 associated Gibbs free energy values were calculated according to methodologies and values
 400 from *Kleerebezem and Van Loosdrecht [15]* and Metcalf et al. [69], respectively (pH 7 and
 401 25°C). Light was not included in the thermodynamic calculations and, thus, the more positive
 402 the Gibbs free energy, the higher the photosynthetic energy requirement. Data and calculations
 403 are available upon request.
 404

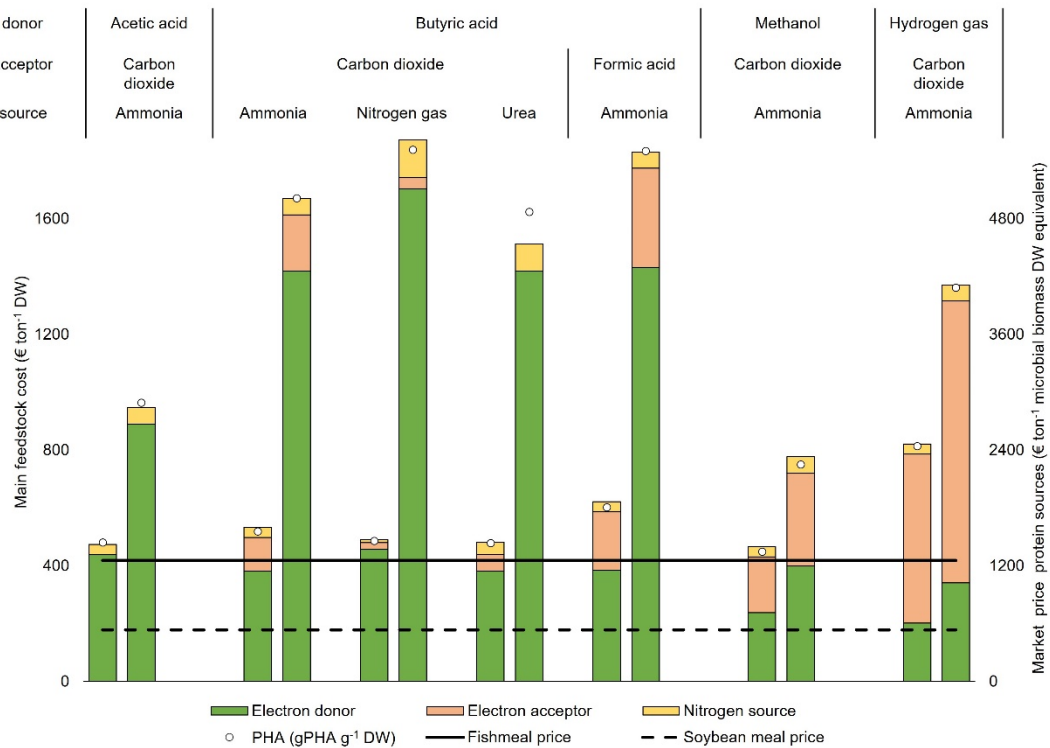


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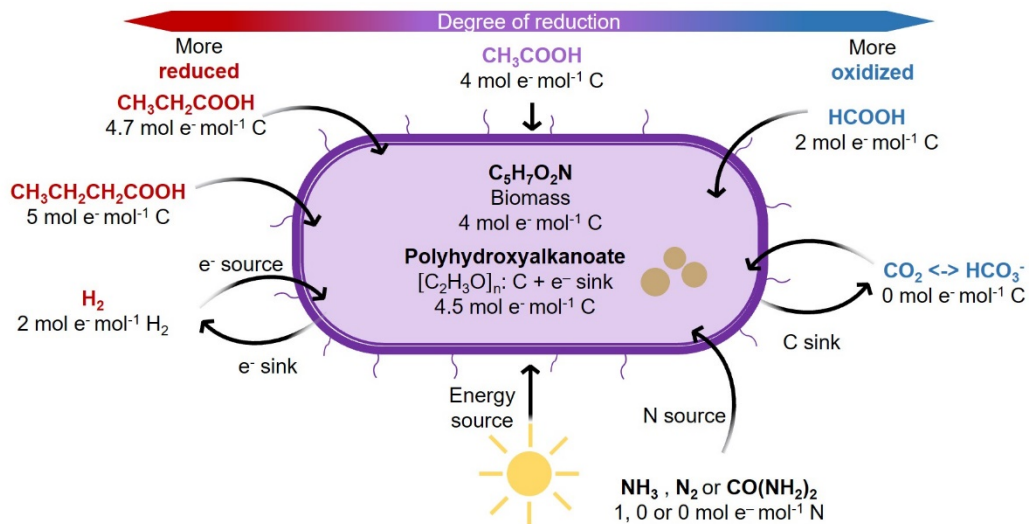
406 **Figure 2 Redox and energy balance of key metabolic pathways involved in**
 407 **phototrophically grown purple bacteria**

408 Net productions (+) or consumptions (-) of CO₂, reduced nicotinamide adenine dinucleotide
 409 (NAD), reduced quinone (Q_{red}) or ferredoxin (FD_{red}) and ATP for the main anaplerotic (pink)
 410 or redox balancing pathways (purple) based on reported enzymatic reactions (KEGG database).
 411 Acetate (Ace) and butyrate (But) were considered to account for the electron content of the
 412 carbon source. Succinate was used as a precursor for oxaloacetate and 2-oxoglutarate as it
 413 represents a common intermediate for acetate and butyrate assimilation. All calculations are

414 presented per mole of produced compound/monomer. Arrows: multi-reaction pathways;
 415 Dashed arrows: single-reaction.
 416



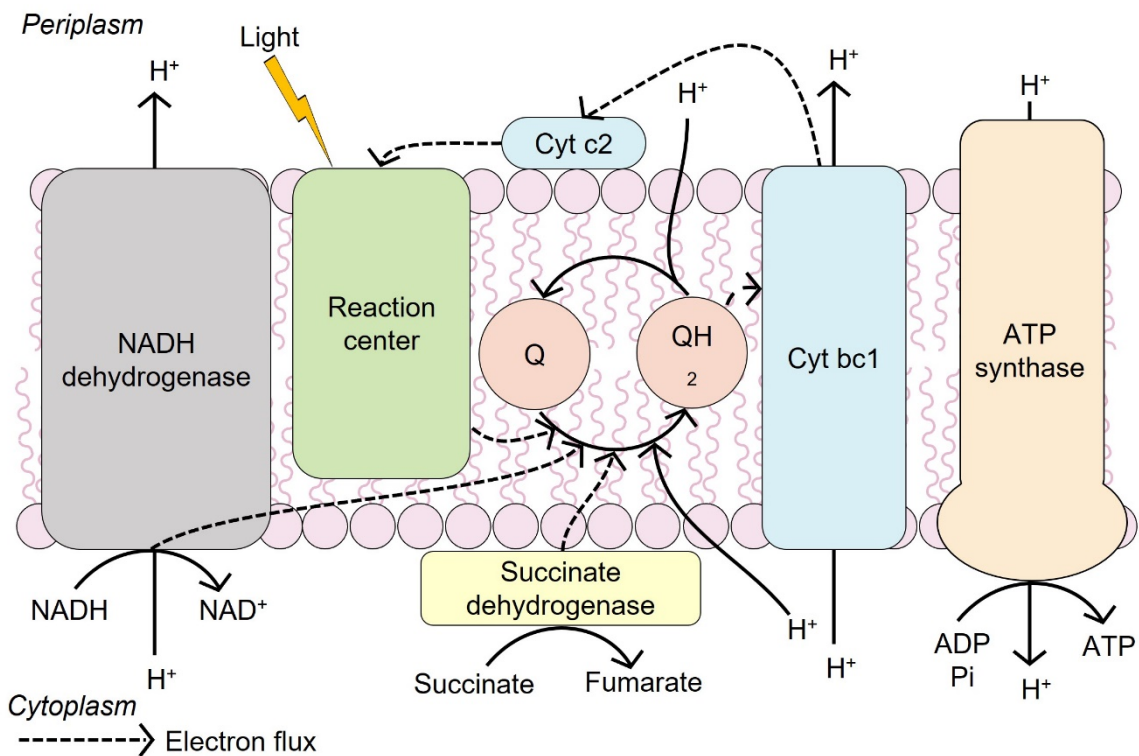
417
 418 **Figure 3 Main feedstock cost estimation for phototrophically grown purple bacteria**
 419 Main feedstock cost for phototrophic cultivation of purple bacteria on four electron donors,
 420 two electron acceptors and three nitrogen sources. Only carbon sources typically considered
 421 for industrial biotechnology applications were considered. Two scenarios were simulated: (i)
 422 biomass production without polyhydroxyalkanoate (PHA), and (ii) biomass production
 423 including 20% of the electrons stored as PHA. PHA was composed of 50%
 424 polyhydroxybutyrate ($C_4H_6O_2$) and 50% polyhydroxyvalerate ($C_5H_8O_2$). A lower and higher
 425 cost estimation was simulated for each scenario to account for uncertainty. Cost of main
 426 feedstock for microbial biomass ($0.65 \text{ kg protein kg}^{-1}$ dry weight) was compared to recalculated
 427 market prices of two conventional protein sources namely, fishmeal ($\text{€}1250 \text{ ton}^{-1}$ product;
 428 $\text{€}1250 \text{ ton}^{-1}$ microbial biomass dry weight (DW) equivalent at $0.65 \text{ kg protein kg}^{-1}$ product) and
 429 soybean meal ($\text{€}410 \text{ ton}^{-1}$ product; 530 ton^{-1} microbial biomass DW equivalent at 0.5 kg protein
 430 kg^{-1} product) [70]. Market price axis ranges a factor three above the cost axis, to reflect a typical
 431 industrial bulk product price/cost ratio. For the electron donors, current industrial prices of
 432 fossil counterparts were used.



433

434 **Box 1, Figure I Redox homeostasis strategies for phototrophically grown purple bacteria**

435 Conceptual sketch of redox homeostasis strategies including CO₂ fixation, and production of
 436 polyhydroxyalkanoates and H₂. A theoretical relative electron content for the carbon (C)
 437 sources, nitrogen (N) sources and H₂ is given compared to the oxidized form CO₂. Values are
 438 expressed in moles. The theoretical relative electron content for the carbon (C) sources,
 439 nitrogen (N) sources and H₂ is expressed in moles. CO(NH₂)₂: urea.



440

441 **BOX 3, Figure I Electron exchange for phototrophically grown purple bacteria**

442 Main intracellular membrane electrons exchange between the different actors involved in the
443 photosynthesis and respiratory chain. Reduction of the quinone pool (Q/QH₂) by the electron
444 donor is represented by both the activity of succinate dehydrogenase (SDH) and NADH
445 dehydrogenase. The conversion of light energy into chemical energy is represented by the
446 cycling of electrons between the photosynthesis **reaction center**, the membranous pool of
447 quinone (Q), the proton pumping cytochrome bc₁ complex (Cyt bc₁) and the soluble
448 cytochrome c₂ (Cyt c₂). ATP is generated by ATP synthase using the produced proton
449 gradient. Dashed arrows indicate the flow of electrons.

450 **Text boxes**

451 **Box 1: Metabolic diversity and cyclic photophosphorylation of purple non-sulfur bacteria**

452 Purple non-sulfur bacteria (PNSB) are a group of metabolically diverse alfa- and beta-
453 Proteobacteria. To date, 28 genera and 95 species are known [1]. These microbes are
454 characterized by their notable color, due to their pigmentation for energy capture from light.
455 This enables them to grow phototrophically, using energy from light. Next to phototrophy,
456 PNSB are also able to grow chemotrophically in the dark, using oxygen as terminal electron
457 acceptor [8,71]. Almost all PNSB can grow heterotrophically on acetate, however, other
458 volatile fatty acids are also suitable. Organic acids, amino acids and carbohydrates can be
459 metabolized as well. A few PNSB species are also able to grow on citrate or aromatic
460 compounds. For autotrophic growth, PNSB rely on CO₂ as carbon source and either sulfate,
461 iron or H₂ as electron donor. Apart from NH₃, most PNSB can also utilize dinitrogen or nitrogen
462 containing organic molecules (amino acids...) as nitrogen source. Some PNSB are also able to
463 assimilate nitrate [72].

464 When PNSB grow phototrophically, they perform cyclic photophosphorylation. In this
465 type of metabolism, electrons excited by photons in the photosystem are transported through
466 several electron carriers and recycled back to the photosystem. The photosynthetic reaction is
467 in this case not providing reducing power as for oxygenic photosynthesis. During
468 photoheterotrophic growth, electrons are thus obtained from external sources and notably from
469 organic carbon. When a carbon source more reduced than the biomass is used, such as butyrate,
470 PNSB have to oxidize the carbon source in an anabolic reaction. The reduced cofactors which
471 are produced during this oxidizing anabolic reaction have to be recycled. When PNSB grow
472 phototrophically, aerobic respiration cannot be used to reoxidize these cofactors. PNSB,
473 therefore, have to exhibit several redox balancing strategies to dump the excess electrons and
474 maintain redox homeostasis.

475 **Box 2: Methodology stoichiometric and thermodynamic calculations**

476 Stoichiometric calculations are based on the method described by Kleerebezem and Van
477 Loosdrecht [15]. In short, the overall anabolic reaction (An) is divided into two half-reactions,
478 namely the biomass synthesis reaction (An*) and an external electron donor (D) or acceptor
479 (A) reaction, depending on the oxidation state of the carbon source (C), nitrogen source (N)
480 and the biomass. To balance the reactions, coefficient Y_{X^Z} was included, with X referring to
481 the reagent and Z referring to the type of reaction.

$$482 \quad \text{An}^* = -Y_C^{\text{An}^*} \text{C} - Y_N^{\text{An}^*} \text{N} + 1 * \text{C}_1\text{H}_{1.4}\text{O}_{0.4}\text{N}_{0.2} + Y_{\text{H}_2\text{O}}^{\text{An}^*} \text{H}_2\text{O} + Y_{\text{H}^+}^{\text{An}^*} \text{H}^+ + Y_{e^-}^{\text{An}^*} e^-$$

$$483 \quad \text{An} = \text{An}^* - Y_{e^-}^{\text{An}^*} / Y_{e^-}^{\text{A}} \text{A} \text{ or } \text{An} = \text{An}^* - Y_{e^-}^{\text{An}^*} / Y_{e^-}^{\text{D}} \text{D}$$

484 To illustrate this concept, an example is provided for the anabolic reaction of growth on
485 butyrate as carbon source, NH₃ as nitrogen source and CO₂ as external electron acceptor.

$$486 \quad \text{An}^* = -0.25 \text{CH}_3(\text{CH}_2)_2\text{COO}^- - 0.2 \text{NH}_3 + 1 \text{C}_1\text{H}_{1.4}\text{O}_{0.4}\text{N}_{0.2} + 0.1 \text{H}_2\text{O} + 0.75 \text{H}^+ + 1 e^-$$

$$487 \quad \rightarrow Y_{e^-}^{\text{An}^*} = 1$$

$$488 \quad \text{A} = -1 \text{CH}_3(\text{CH}_2)_2\text{COO}^- - 6 \text{H}_2\text{O} + 4 \text{CO}_2 + 19 \text{H}^+ + 20 e^- \rightarrow Y_{e^-}^{\text{A}} = 20$$

$$489 \quad \text{An} = -0.2 \text{CH}_3(\text{CH}_2)_2\text{COO}^- - 0.2 \text{NH}_3 - 0.2 \text{H}^+ + 1 \text{C}_1\text{H}_{1.4}\text{O}_{0.4}\text{N}_{0.2} + 0.4 \text{H}_2\text{O}$$

490 For the thermodynamics, the Gibbs free energy for the reaction was calculated as described in
491 Metcalf et al. [69]. Light was not included in the thermodynamic calculations and, thus, the
492 more positive the Gibbs free energy, the higher the photosynthetic energy requirement. In short,
493 the Gibbs free energy required to produce cell material (ΔG_S) is divided into three parts: (i)
494 energy required to convert the carbon source to a pyruvate intermediate (ΔG_P), a frequent
495 intermediate in the metabolism of microorganisms, (ii) energy to convert the pyruvate into cell
496 material (ΔG_C), and (iii) energy required to reduce the nitrogen source to ammonia. These three
497 factors are corrected with the efficiency of the captured energy (K), and m, equal to +1 if ΔG_P
498 is positive and -1 if ΔG_P is negative.

$$499 \quad \Delta G_S = \Delta G_P / K^m + \Delta G_C + \Delta G_N / K$$

500

501 **Box 3: NAD⁺ photoreduction and light-induced redox stress**

502 Under phototrophic conditions, PNSB generate a proton motive force through electron cycling,
503 which converts light energy to chemical energy in the form of reduced quinone and cytochrome
504 bc1 complex (Box 3, Figure I) [73]. **Bacteriochlorophyll**, which is part of the reaction center,
505 recovers its lost electron from reduced cytochrome c2. Under photoautotrophic conditions, with
506 CO₂ as carbon source and H₂ as an electron donor, electrons obtained by membrane-bound
507 uptake hydrogenase have been shown to flow through the quinone pool from H₂ to NAD⁺
508 through the NADH dehydrogenase complex [74]. This reverse electron transfer to NAD⁺, also
509 called uphill electron transfer, allows the production of the redox poise required for CO₂
510 fixation. Under photoheterotrophic conditions, the carbon source also brings electrons required
511 for biomass production. Electrons from the biomass can also be transferred to the quinone pool,
512 notably through the membranous succinate dehydrogenase. Under illuminated conditions, it
513 has been proposed that the NADH dehydrogenase complex is responsible for the oxidation of
514 quinones through a mechanism relying on the light-driven **membrane potential** [74-76]. By
515 modeling the electron transfer chain of *Rs. rubrum*, it was observed that higher light intensities,

516 induce a higher membrane potential (or high proton motive force), and a higher reverse electron
517 flow to NAD^+ from the quinone pool. This leads to a more oxidized quinone and reduced
518 nicotinamide cofactor pool [77]. We proposed that the NAD^+ photoreduction is responsible for
519 the so-called light-induced redox stress which results from an overreduction of the NAD^+
520 cofactor pool. This light stress could occur upon a sudden light increase [13] or at the very
521 beginning of a culture [21]. The sudden light increase supposedly triggered a higher flux of
522 electrons toward the production of NADH thus blocking oxidative reaction necessary for cell
523 metabolism.

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