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# Storage without nitrite or nitrate enables the long-term preservation of full-scale partial nitritation/anammox sludge

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Abstract: Bioaugmentation with summer harvested sludge during winter could 10 11 compensate for the bacterial activity loss but requires that the sludge activity can be restored after storage. This study assesses the effect of temperature and redox addition 12 13 during the storage of partial nitritation/anammox (PN/A) granular and floccular sludge 14 over 180 days. Anoxic storage conditions (in the presence of nitrite or nitrate and the absence of oxygen) resulted in a loss of 80 – 100% of anammox bacteria (AnAOB) activity 15 capacity at 20°C and 4°C, while anaerobic conditions (without oxygen, nitrite, and nitrate) 16 lost only 45 – 63%. Storage at 20°C was more cost-effective compared to 4°C, and this 17 was confirmed in the sludge reactivation experiment (20°C). Furthermore, AnAOB 18 activity was negatively correlated with the electrical conductivity level ( $R^2 > 0.85$ , p < 19 20 0.05). No significant differences were found in the activity capacity of aerobic ammonia-21 oxidizing bacteria (AerAOB) under different storage conditions (p > 0.1). The relative abundance of dominated AnAOB (Candidatus Brocadia) and AerAOB genera 22

(*Nitrosomonas*) have remained in both sludges. Concluding, preserving PN/A biomass
 without cooling and nitrite or nitrate addition proved to be a cost-effective strategy.
 **Keywords:** Deammonification; Decay; Mainstream; Redox; Sewage treatment; Sludge
 characteristics

## 27 **1. Introduction**

28 Around 25 years after conceptually proposing the importance of anaerobic ammonia 29 oxidation (anammox) bacteria (AnAOB) in energy-positive sewage treatment (Mulder et 30 al., 1995), a current hot topic in wastewater treatment is the implementation of socalled mainstream partial nitritation/anammox (PN/A) or deammonification. Due to the 31 32 lower energy and carbon demand as well as the lower N<sub>2</sub>O emission compared to 33 conventional nitrification/denitrification, it is an economical and environmental-friendly process (Agrawal et al., 2018; Ali et al., 2016) which consists of aerobic ammonium-34 35 oxidizing bacteria (AerAOB), that oxidize roughly half of the NH4<sup>+</sup> to NO<sub>2</sub><sup>-</sup> ('partial 36 nitritation') and AnAOB, that oxidize the produced  $NO_2^-$  and residual  $NH_4^+$  to  $N_2$ ('anammox') (Agrawal et al., 2018). 37

PN/A systems have been successfully implemented in the reject water line (sidestream) all over the world (Lackner et al., 2014). Compared to the sidestream, which has a higher temperature ( $15 - 20^{\circ}$ C higher) and nitrogen concentration (more than 20 times), achieving efficient nitrogen removal in the mainstream is much more challenging. Especially during the winter period, as the mainstream temperature could drop to about  $10 - 12^{\circ}$ C in western Europe ( $20 - 22^{\circ}$ C in summer) according to the data in Nieuwveer sewage treatment plant (STP) (Breda, the Netherlands). This temperature decrease

significantly reduces the activity of functional bacteria, especially for the AnAOB. Lotti
et al. (2014) reported a growth rate of 0.02 d<sup>-1</sup> at 20°C and only 0.005 d<sup>-1</sup> at 10°C. As an
extended sludge retention time in winter will not be sufficient because of the low growth
rates, this problem may be tackled by storing excess PN/A sludge, mainly harvested over
summer, and reinoculated this in winter.

Long-term preservation to maintain enough and activated sludge for at least 180 days 50 is essential for the successful application of this novel concept. Different commonly used 51 storage methods were deemed unfeasible for this bioaugmentation concept. 52 Cryopreservation (-20 °C, -80 °C and -200 °C) with various cryoprotective agents (e.g., 53 dimethyl sulfoxide) that prevent activity loss during sludge or culture collections storage 54 55 has been extensively described (Rothrock et al., 2011; Viancelli et al., 2017), the cooling 56 process and cryoprotective agents are expensive which limit its application at full-scale. Likewise, immobilizing technique (Ali et al., 2014), consortia transformation strategy (Shi 57 et al., 2020), and protective agents addition (e.g., hydrazine, glycerol, skim milk) 58 59 (Ganesan and Vadivelu, 2020; Rothrock et al., 2011; Vlaeminck et al., 2007) is also not 60 feasible for full-scale application because of the operational complexity and high cost, even though many of them have proved useful. 61

In contrast, substrates or redox spikes are expected to be applicable for the bioaugmentation concept since they could well retain anammox activity and low operation cost. The addition of redox buffers (nitrite or nitrate) during sludge preservation was investigated, as it may be effective in preventing sulfate reduction, which produces H<sub>2</sub>S, harmful to biomass (Vlaeminck et al., 2007). Wang et al. (2016) demonstrated that about

67 30% of AnAOB activity was maintained after 180 days of preservation at 35°C with 68 weekly supplying NH<sub>4</sub><sup>+</sup>-N and NO<sub>2</sub><sup>-</sup>-N (50 mg N L<sup>-1</sup> respectively). Ali et al. (2014) stored 69 anammox sludge with 3 mM molybdate (inhibitor of sulfate reduction) and a regular 70 supply of NH<sub>4</sub><sup>+</sup> and NO<sub>2</sub><sup>-</sup> at room temperature and maintained 65% of the activity after 71 five months of storage. Considering that both NH<sub>4</sub><sup>+</sup> and NO<sub>2</sub><sup>-</sup> are substrates for AnAOB, 72 periodical adding them could well avoid starvation.

Besides redox stabilization, the low temperature has also been proved beneficial for anammox sludge preservation. Vlaeminck et al. (2007) reported that 4°C without nitrate storage addition was a recommended strategy for PN/A biofilm storage over five months (maintained 55% AnAOB activity). Xing et al. (2016) also revealed that anammox granules preserved at 4 °C without substrate addition had a lower decay rate and higher nitrogen removal capacity after storage compared to granules stored at 20°C.

To evaluate the feasibility of the novel winter bioaugmentation concept, essential 79 information about PN/A sludge storage and reactivation is currently still lacking. Firstly, 80 81 various preservation methods have been applied in several studies, but there is no study 82 comparing all these different preservation methods, which is essential for a fair comparison, as results can be influenced by the microbial community composition and 83 84 sludge types. Secondly, most studies only assess the preservation of anammox or 85 nitrifying sludge, not PN/A sludge. Thirdly, room or lower temperature reactivation is important since it has more implementation potential for its lower required amount of 86 87 energy (heat), whereas sludge reactivation has only been widely studied at the optimum temperature. The preserved sludge in previous studies could be reactivated at the 88

optimum temperature (30 – 40 °C) from days to weeks (Ali et al., 2014; Viancelli et al.,
2017).

The overall objective of this study is to find a cost-effective, and simple operation 91 strategy to store PN/A sludge on a large scale. Therefore, three parts were examined: i) 92 the effect of temperature and redox stabilization over 180 days' storage of PN/A 93 granules and flocs derived from full-scale STPs, ii) the potential of the stored biomass 94 95 reactivation after 180 days, and iii) the OPEX (operating expenses or expenditure) and cost-effective analysis of different preservation strategies. Over the biomass storage, 96 97 physicochemical characteristics and community composition are closely monitored. The finding will have good guiding significance for the storage of PN/A sludge on a large scale 98 and provide the cost-effective biomass source for the concept of winter 99 100 bioaugmentation with the stored summer sludge.

101 **2.** N

## 2. Materials and methods

#### 102 **2.1. PN/A sludge source and characterization**

To verify that the strategy proposed in this study was feasible and stable for different sludge, floccular sludge (with a biomass concentration of  $9.0 \pm 0.2$  g VSS L<sup>-1</sup>) and granular sludge (13.6 ± 0.9 g VSS L<sup>-1</sup>) were collected from full-scale sidestream (990 m<sup>3</sup>, Breda, The Netherlands) and potato-processing wastewater (600 m<sup>3</sup>, Olburgen, The Netherlands) PN/A installations, respectively. The characteristics of both sludges are shown in Table – 1.

#### **2.2. Sludge storage procedure and strategies**

110 The sludge was stored under different storage conditions for 180 days in 5 L plastic

111 containers (0.4 L of headspace, with a small opening to avoid pressure build-up by gas (e.g.,  $N_2$  and  $H_2S$ ) production). Four preservation strategies were tested (Table – 2): 1) no 112 N spike, i.e., sludge storage under anaerobic conditions (without oxygen and redox 113 buffer), 2)  $NO_2^-+NH_4^+$  spikes (substrates for AnAOB), 3)  $NO_3^-+NH_4^+$  spikes (Due to the 114 ammonium produced by biomass decay was always consumed in nitrate strategy from 115 116 our pre-test. In the present research, ammonium was added to ensure adequate supply.), 117 and 4)  $NO_{3}$  spikes (redox buffer to alleviate sulfate reduction). Two preservation strategies (i.e., 'no N spike' and 'NO<sub>2</sub><sup>-</sup>+NH<sub>4</sub><sup>+</sup>) were also duplicate tested at 4°C for 118 119 floccular sludge. Only floccular sludge was chosen to test the strategy of 4°C because the activity maintenance had already been proved in the previous study (Vlaeminck et 120 121 al., 2007), and the high cooling cost was also not expected to be applied in the biomass 122 storage on the large scale. The concentration of ammonium, nitrite, and nitrate was maintained between 30 – 180 mg N L<sup>-1</sup> by regular addition of NH<sub>4</sub>Cl, NaNO<sub>2</sub>, and NaNO<sub>3</sub>, 123 respectively. The determination of NO<sub>2</sub><sup>-</sup>-N concentration is based on previous research 124 125 (Talan et al., 2021). For NH<sub>4</sub><sup>+</sup>-N and NO<sub>3</sub><sup>-</sup>-N, their concentrations were consistent with 126 NO<sub>2</sub><sup>-</sup>-N since no inhibition occurred at the concentration lower than 200 mg N L<sup>-1</sup> (Strous et al., 1999; Zhu et al., 2017). All storage experiments were performed in duplicate, and 127 128 the mean values are reported.

During storage, the pH was controlled manually within 7.2 – 8.0 by 1 M HCl and NaOH addition. The dissolved oxygen (DO) concentration was lower than 0.01 mg  $O_2 L^{-1}$  in all the storage containers. The storage vessels were mixed five times per week.

132 **2.3. Single and consecutive batch activity tests** 

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#### 2.3.1. Single batch test: the maximum potential activities determining

Batch activity tests were performed to determine the maximum potential activities of 134 AnAOB every 30 days. After mixing, about 20 mL of sludge was harvested from each 135 container and stored at 20 ± 1°C for one day to make sure that all the batch tests were 136 carried out at the same temperature. The sludge was washed four times and diluted to 137 a biomass concentration of 1.0 g VSS L<sup>-1</sup> with a buffer solution containing only NaHCO<sub>3</sub> 138 139 (0.4 g L<sup>-1</sup>) and trace elements (1 ml L<sup>-1</sup>) (Van de Graaf et al., 1995). Ammonium and nitrite (50 mg N L<sup>-1</sup>) were spiked in all Erlenmeyer flasks. The AerAOB and NOB activity was 140 141 determined in flasks exposed to the air, whereas the flasks to determine AnAOB activity 142 were sealed with rubber stops after 15 min flushing with N<sub>2</sub> (to provide anoxic conditions). The flasks were incubated on a shaker (200 rpm) at 20 ± 1°C, and pH was 143 144 adapted to 7.5 (with HCl) at the start of the tests. The biomass concentration was only 145 measured at the start of each test. DO and pH levels were also followed during the whole test. The DO concentrations for aerobic tests were higher than 7.0 mg O<sub>2</sub> L<sup>-1</sup> and pH 146 147 values were around 7.5. All the batch tests were performed in duplicates, and the 148 average values were reported. To monitor the nitrogen conversion, samples were taken periodically (every hour) and stored at 4°C until analysis. The maximum specific 149 150 anammox activity was determined from the maximum slope of the curve indicated by 151 the decrease of NH<sub>4</sub><sup>+</sup>-N over time, divided by the biomass concentration in the flask.

#### 152 **2.3.2. Consecutive batch test: bacterial activity reactivation**

After 180 days, consecutive batch tests (i.e., 20 spikes over 7 days) were performed to assess the activities' reactivation. Sludge was pre-treated and spiked every 12h (after washing) to avoid substrate limitation or accumulation. The substrate conversion rate
was quantified every other cycle (7 in total) by measuring the NH<sub>4</sub><sup>+</sup>-N, NO<sub>2</sub><sup>-</sup>-N, and NO<sub>3</sub><sup>-</sup>N concentration. The biomass concentration was only determined at the start of each
test. The activity recovery percentage was defined as the maximum activity obtained in
these seven days divided by the initial activities (before storage).

#### 160 **2.4. Analytical procedures**

161 Liquid and microbial samples were taken periodically from the storage containers (mixed before sampling). In addition, during the batch tests, liquid samples were taken 162 163 from the Erlenmeyer flasks regularly. After filtering by 0.2 µm syringe filter (CHROMAFIL Xtra PVDF) and storing at 4°C, NH<sub>4</sub><sup>+</sup>-N, NO<sub>2</sub><sup>-</sup>-N, and NO<sub>3</sub><sup>-</sup>-N were measured with a San<sup>++</sup> 164 Automated Wet Chemistry Analyzer (SKALAR, the Netherlands). H<sub>2</sub>S in liquid was 165 166 measured using Spectroquant test kits (Merck, Germany). The biomass concentration was followed over time using volatile suspended solids (VSS) measurements (APHA, 167 2005). Handheld meters were used to monitor pH, electrical conductivity (EC), and DO 168 169 concentration (Hach HQ30d, USA). The detailed information about extracellular 170 polymeric substances (EPS) extraction and heme c measurement is shown in S - 1(Supporting Information). The calculation of free nitrous acid (FNA) and free ammonia 171 172 (FA) are shown in S – 2 (Supporting information). The V4 region of the 16S rRNA gene 173 was sequenced for the following-up analysis by Novogene Europe (United Kingdom) 174 after the genomic DNA was extracted using a Powerfecal kit (Qiagen, Germany) in the 175 lab. The detailed method is presented in S - 3 of the Supporting Information.

176 **2.5. Bacterial activity capacity calculation** 

Sludge decay during storage can be attributed to activity decay and biomass loss. As the objective of the present research is to maintain enough and activated sludge after 180 days, an accurate parameter that combines these two factors is proposed to analyze the effects of storage on the sludge: the bacterial activity capacity R<sub>c</sub>, which is calculated using the following equation.

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$$R_c = r_b * C_s * V_t \tag{Eq. 1}$$

183 R<sub>c</sub> is the bacterial activity capacity [mg NH<sub>4</sub><sup>+</sup>-N d<sup>-1</sup>] for AerAOB/AnAOB and [mg NO<sub>3</sub><sup>-</sup>-N 184 d<sup>-1</sup>] for NOB; r<sub>b</sub> is the maximum bacterial (AnAOB, AerAOB, and NOB) activity [mg NH<sub>4</sub><sup>+</sup>-185 N g<sup>-1</sup> VSS d<sup>-1</sup>] for AerAOB/AnAOB and [mg NO<sub>3</sub><sup>-</sup>-N g<sup>-1</sup> VSS d<sup>-1</sup>] for NOB; C<sub>s</sub> is the biomass 186 concentration [g VSS L<sup>-1</sup>]; and V<sub>t</sub> is the sludge volume [L].

The decay rate (d<sup>-1</sup>) of bacterial activity capacity depends on activity decay (decrease in sludge-specific activity) and cell death (decrease in biomass concentration), and is calculated according to Hao et al. (2009). The bacterial decay rates are calculated respectively as the slopes of logarithmic plots of the activity capacity of AnAOB by linear regression (p < 0.5).

#### 192 **2.6. Cost assessment**

As far as the author knows, this is the first research to assess the cost-effectiveness during the PN/A sludge preservation process. Room temperature is assumed stable at  $20^{\circ}$ C, thus only the 4°C conditions need to consume electricity to cool down. During the whole biomass preservation period, the main OPEX is nitrogen compounds addition (NH<sub>4</sub>Cl, NaNO<sub>2</sub>, and NaNO<sub>3</sub>), pH control (HCl and NaOH), and potential cooling ( $20^{\circ}$ C  $\rightarrow$  198 4°C). Mixing cost is negligible compared to the other operational factors (< 0.5% of the total cost). All the OPEX is calculated based on the in-suit sludge storage.-

200 OPEX per specific AnAOB activity (€ d kg NH<sub>4</sub><sup>+</sup>-N<sup>-1</sup>) is put forward to analyze the cost-

effectiveness of different biomass preservation strategies. Its calculation process is the 201

whole OPEX (over 180 days, € ton VSS<sup>-1</sup>) divided by the AnAOB activity of Day-180 (kg 202

NH<sub>4</sub><sup>+</sup>-N ton VSS<sup>-1</sup> d<sup>-1</sup>). The strategy which has the lowest value is regarded as the most 203

204 cost-effective preservation method.

3. Results and discussion 205

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3.1. Anaerobic conditions maintained higher bacterial activity capacity than anoxic 206 conditions 207

#### 208 3.1.1 AnAOB activity capacity

Over time, the AnAOB activity capacity decreased in both sludge types and all storage 209 210 conditions due to a strong decrease in AnAOB activity and a mild decrease in biomass 211 concentration in most conditions (Figure. 1).

Considering only the temperature, sludge stored at 4°C outperformed sludge stored 212 213 at 20°C in AnAOB activity capacity retention. Comparing the 'no N spike' at 20°C and 4°C, 214 the AnAOB activity capacity was respectively 1.95 and 2.98 kg NH<sub>4</sub><sup>+</sup>-N d<sup>-1</sup> on Day-180 in floccular sludge. For the 'NO<sub>2</sub><sup>-</sup>+NH<sub>4</sub><sup>+</sup>', this difference was even more pronounced: 0.05 215 and 1.15 kg NH<sub>4</sub><sup>+</sup>-N d<sup>-1</sup> at 20°C and 4°C, respectively. According to Adav et al. (2007) and 216 217 Gao et al. (2012), the endogenous respiration and cell lysis process that microorganisms 218 use to sustain activity during storage decelerates at low storage temperatures, which probably could explain a lower drop in biomass concentration. Taking 'no N spike' as an 219

example, only 7.5% of biomass concentration loss was observed at 4°C compared to 30.7%
loss at 20°C in floccular sludge. Although there was little variation between activity
preservation (59.47% at 4°C versus 52.36% at 20°C), 'no N spike (4°C)' still maintained
much higher activity capacity than that at 20°C.

224 For the storage strategies at 20°C, sludge stored without N spike ('no N spike (20°C)') retained a higher AnAOB activity capacity (37 – 49%) compared to sludge with redox 225 226 (nitrite or nitrate) addition (0 - 20%) in both floccular and granular sludges. This is contrary to many previous studies, that is, at 20°C, regular NO<sub>3</sub>-N addition is the best 227 228 strategy (Engelbrecht et al., 2016; Vlaeminck et al., 2007). Firstly, pH control under 229 anaerobic conditions in the present research might benefit the AnAOB activity capacity maintenance. The sludge consumed alkalinity during biomass decay and starvation, 230 231 which led to the pH decrease (Anjali and Sabumon, 2014). The low pH values could 232 increase FNA concentration (Figure. S3) that probably inhibited AnAOB activity (Strous et al., 1999). Secondly, the glycogen (one of the intracellular polymers that microbial 233 234 store in cells when there was an adequate supply of substrates) might serve only as a 235 maintenance energy source for microorganisms (Ma and Wang, 2018). However, it possibly also be used by the dissimilatory nitrate/nitrite reduction to ammonium process 236 237 (as electron donor) to generate energy under anoxic condition stress, which increased 238 the decay rate of biomass. That could promote it to have much better resistance, tolerance, and self-adaptation to starvation. 239

Specific for 'NO<sub>2</sub><sup>-</sup>+NH<sub>4</sub><sup>+</sup> (20°C), the addition of substrates during storage resulted in the loss of almost all AnAOB activity even though AnAOB preferentially oxidizes both

242 ammonium and nitrite into N<sub>2</sub> when they are present (Ganesan and Vadivelu, 2020). On one hand, only nitrogen compounds were provided during the preservation process 243 while their metabolic activity requires many other elements (e.g., inorganic carbon, trace 244 245 elements, etc.) (Ma et al., 2015; Van de Graaf et al., 1995). With nitrogen as the only substrate, the starvation of microbes possibly is more serious than that without nitrogen 246 addition (Lu et al., 2018). On the other hand, the EC levels increased rapidly (e.g., 17.53 247 mS cm<sup>-1</sup> in 'NO<sub>2</sub><sup>-</sup>+NH<sub>4</sub><sup>+</sup> (20°C)' versus 5.09 mS cm<sup>-1</sup> in 'no N spike (20°C)' on Day-180 for 248 floccular sludge), which was also harmful to AnAOB (Section – 3.4). However, the higher 249 250 nitrite concentration range (30 – 180 mg N L<sup>-1</sup>) compared to previous studies (e.g., 50 – 251 70 mg N L<sup>-1</sup> (Ali et al., 2014; Wang et al., 2016)) was unlikely to be the main cause for the failure of 'NO<sub>2</sub><sup>-</sup>+NH<sub>4</sub><sup>+'</sup> since this strategy was still unsuitable for biomass preservation 252 253 even at the concentration of 50 mg N L<sup>-1</sup> as studied by Ganesan and Vadivelu (2020).

In the present research, NO<sub>3</sub><sup>--</sup>N was supplied as a redox buffer to prevent sulfate 254 reduction. Low temperature (4°C) and NO<sub>2</sub><sup>-</sup>-N could also play the same role to suppress 255 256 sulfate reduction (Vlaeminck et al., 2007). A higher H<sub>2</sub>S concentration after 180 days of 257 preservation was detected in the 'no N spike (20°C)' compared to the other conditions (i.e., 'no N spike (4°C)' and anoxic conditions) for both floccular (0.23 versus < 0.19 mg S 258 259  $L^{-1}$ ) and granular (0.08 versus < 0.06 mg S  $L^{-1}$ ) sludge (Figure. 2). This confirmed the 260 inhibition of sulfate reduction under low temperature conditions or in the presence of NO<sub>3</sub><sup>-</sup>-N and NO<sub>2</sub><sup>-</sup>-N. However, this H<sub>2</sub>S concentration probably did not affect the AnAOB 261 262 activity according to the previous research (Jin et al., 2013).

263 In short, for both sludges, the AnAOB activity decay rates under anaerobic conditions

(i.e., 'no N spike') ( $0.0028 - 0.0041 d^{-1}$ ) were more than twice as low compared to under anoxic conditions (i.e., 'NO<sub>2</sub><sup>-</sup>+NH<sub>4</sub><sup>+'</sup>, 'NO<sub>3</sub><sup>-</sup>+NH<sub>4</sub><sup>+'</sup>, and 'NO<sub>3</sub><sup>-'</sup>) ( $0.0094 - 0.0239 d^{-1}$ ). The results were in line with Ma and Wang (2018), who got an AnAOB activity decay rate of 0.0049 d<sup>-1</sup> in anaerobic conditions and 0.0129 d<sup>-1</sup> in anoxic conditions after 60 days of storage. The biomass decay was much less critical than activity decay during the sludge storage under different storage strategies (3 – 20 times lower, Figure. 1G/H).

#### 270 **3.1.2 AerAOB and NOB activity capacity**

The floccular sludge stored at  $4^{\circ}$ C ('no N spike ( $4^{\circ}$ C)' and 'NO<sub>2</sub><sup>-</sup>+NH<sub>4</sub><sup>+</sup> ( $4^{\circ}$ C)') maintained 271 272 the highest AerAOB activity capacity (75 % and 66% of the initial value, respectively) 273 after 180 days of storage (Figure. 3). Floccular sludge stored at 20°C without N spike ('No 274 N spike (20°C)') or with nitrate (and ammonium) spikes ('NO<sub>3</sub><sup>-</sup>+NH<sub>4</sub><sup>+</sup> (20°C)' and 'NO<sub>3</sub><sup>-</sup> 275 (20°C)') also retained more than 50% of the AerAOB activity capacity. Sludge spiked with 276 nitrite and ammonium (' $NO_2$  + $NH_4$  (20°C)'), in contrast, lost more than 70% of its activity capacity. Similarly, in the granular sludge, about ~65% of the AerAOB activity capacity 277 278 could be retained in all conditions, except for 'NO<sub>2</sub><sup>-+</sup>NH<sub>4</sub><sup>+</sup> (20°C)' (28%).

The difference in AerAOB activity capacity between different storage strategies was similar to that on AnAOB activity capacity retention which might attribute to the change of EC levels, FNA and/or FA concentrations, and nitrite concentration range mentioned above (Section – 3.1.1). Specific for low-temperature, a high AerAOB activity capacity could be retained at 4°C (3.36 and 2.81 kg NH<sub>4</sub><sup>+</sup>-N d<sup>-1</sup> for 'no N spike (4°C)' and 'NO<sub>2</sub><sup>-</sup> +NH<sub>4</sub><sup>+</sup> (4°C)' compared to that 2.40 and 1.30 kg NH<sub>4</sub><sup>+</sup>-N d<sup>-1</sup> at 20°C), which was confirmed

by Gao et al. (2012) who reported that 4°C was significantly better to store aerobic
granules compared to room temperature.

287 NOB was more sensitive to starvation compared to AerAOB. A very low NOB activity capacity was obtained after 180 days of storage except for 'no N spike (4°C)' (floccular 288 sludge) and 'NO<sub>3</sub><sup>-</sup> (20°C)' (floccular and granular sludge). 'NO<sub>2</sub><sup>-</sup>+NH<sub>4</sub><sup>+</sup> (20°C)' had the 289 lowest NOB activity capacity, which was followed by 'NO<sub>2</sub><sup>-+</sup>NH<sub>4</sub><sup>+</sup> (4°C)' and 'NO<sub>3</sub><sup>-+</sup>NH<sub>4</sub><sup>+</sup> 290 291  $(20^{\circ}C)'$  for both floccular and granular sludge. The high FA  $(0 - 4 \text{ mg L}^{-1}, \text{ Figure. S1})$  in 292 the storage vessels might lead to the low NOB activity capacity maintenance. According 293 to Vadivelu et al. (2007), a concentration of 1 - 6 mg FA-N L<sup>-1</sup> eliminated the NOB in 294 PN/A sludge during reactor treatment. That was also proved by the higher NOB decay rate than AerAOB at the same preservation conditions (e.g., 0.003 d<sup>-1</sup> versus 0.015 d<sup>-1</sup> in 295 296 'no N spike (20°C)' of floccular sludge). NOB suppression appeared during storage was 297 beneficial for PN/A application.

Compared to the decay rate of AnAOB and NOB, the AerAOB was lower. That was 298 299 likely because AerAOB promoted cellular adaptation to starvation by stabilizing 300 intracellular macromolecular levels (Ma et al., 2017). Apart from that, three physiological advantages might also be attributed to (Geets et al., 2006): i) AerAOB has 301 302 stable catabolic cellular components (e.g., energy-generating enzymes), which 303 corresponded to their fast reactivation (Section-3.2) ii) AerAOB has low maintenanceenergy demand than other bacterial, and iii) signaling pathways involved in starvation 304 305 survival would be initiated in AerAOB during storage.

306 3.2 Both AnAOB and AerAOB activity of sludge stored under anaerobic conditions
 307 were reactivated

#### 308 **3.2.1 AnAOB activity reactivation**

The AnAOB activity was increased during the first 3 - 4 days but decreased afterward (Figure. 4). The decline can be attributed to the biomass loss during the reactivation in the flasks (the medium was replaced every day, resulting in an estimated biomass loss of 10% - 15% per day).

The anaerobically preserved sludge (i.e., 'no N spike') could recover faster (activity 313 314 doubled after 2 – 3 days) than the anoxically preserved sludge and showed a higher 315 recovery percentage (87 – 114% versus 6 – 50%) at 20°C (Figure. 4E/F). Without substrate supply during preservation (i.e., 'no N spike'), AnAOB might still maintain 316 317 activity through the internal endogenous metabolism and intercellular substrates from biomass decay by inducing starvation proteins (especially enzymes related to the PN/A 318 process) (Ma and Wang, 2018). In addition, the anoxic storage conditions changed 319 320 rapidly (pH adjustment and nitrate or nitrite addition periodically, EC increased gradually) 321 could probably harm AnAOB that affected its reactivation. Ma et al. (2017) demonstrated that AnAOB sludge, starved in anaerobic conditions (during 40 h), almost 322 323 completely recovered after 6 h whereas sludge stored in anoxic conditions could only be 324 reactivated for 34%.

Even though the preserved biomass at both 4°C and 20°C could be reactivated, 4°C conditions had a higher recovery percentage than 20°C (114% versus 99% in 'no N spike' and 17% versus 6% in 'NO<sub>2</sub><sup>-</sup>+NH<sub>4</sub><sup>+'</sup> for floccular sludge). That was in line with the

performance during the biomass storage that 4°C could maintain higher AnAOB activity
 after 180 days of preservation.

330 Sludge reactivation is essential for the full-scale application of stored sludge in the concept of 'winter bioaugmentation with stored summer sludge'. Mainstream 331 inoculation and high sludge retention time (SRT) applied may be sufficient to achieve 332 333 AnAOB reactivation which is in order of days (i.e., 3-4 days) while the SRT is in order of 334 weeks (i.e., ~4 weeks, based on the original reactors of both sludges). So, this is a good chance that dedicated the reactivation tank would not be needed in practice. Even if the 335 336 reactivation reactors are applied, their volume is limited. Because several batches of sludge can be sequentially reactivated, not only one, which can save space. 337

338

#### 3.2.2 AerAOB activity reactivation

339 Even though the AerAOB in principle can be obtained through the activated sludge inoculating with activated sludge from other conventional mainstream sewage 340 341 treatment plants, the AerAOB preservation and reactivation together with AnAOB could 342 still have some benefits. Because the activated sludge inoculation would introduce high 343 levels of potential NOB activity, which could connect the NOB to AerAOB rather than the AerAOB to AnAOB. That will add extra competition for nitrite. NOB suppression remains 344 345 the main challenge for mainstream PN/A application (Peng et al., 2020), and the yearly 346 introduction of new NOB could hamper the overall performance by disturbing the microbial balance. 347

AerAOB has higher activity recovery percentage than AnAOB at 20°C (56 – 110% vs. 5
- 114%) in total (Fig. 4E/F). Except for the sludge stored in 'no N spike' which recovered

350 93 – 100% of activity, more than 57% of activity was reactivated for the other sludges. For the recovery of AerAOB activity, that sensitivity difference compared to AnAOB 351 could be explained by the 10-times higher growth rate of AerAOB (0.04 h<sup>-1</sup> for AerAOB 352 and 0.003 h<sup>-1</sup> for AnAOB at 32-33°C (Jetten et al., 2001)). Similar to the present research, 353 Gao et al. (2012) reported that AerAOB activity could be fully restored within ten days 354 after eight months of storage from almost 0 for all different storage conditions. The 355 356 present research results indicated that even when AerAOB was stored together with AnAOB (PN/A sludge), they were still easy to be reactivated. 357

#### 358 **3.3. Dominant genera retained their relative abundance over the storage period**

Since ammonium was always present in the sludge stored with only nitrate spikes (i.e.,  $(NO_3^- (20^\circ C)')$  due to biomass decay, the storage conditions resembled the conditions in  $(NO_3^- + NH_4^+ (20^\circ C)')$  which resulted in a similar bacterial activity capacity. Therefore, only the samples from the  $(NO_3^- + NH_4^+ (20^\circ C)')$  strategy were analyzed.

The Shannon index decreased over time in the floccular sludge (e.g., from 7.125 on 363 364 day-0 to 5.498 on day-180 in 'no N spike (20°C)') that the diversity of the communities 365 decreased during storage (Table – S1). The DO levels during the whole experiments were lower than 0.01 mg O<sub>2</sub> L<sup>-1</sup>, some species related to aerobic processes might be not 366 367 adapted to the conditions were eliminated. In addition, a salinity condition was created 368 due to a gradual increase of the EC value during preservation (Section – 3.4), which possibly also affected the diversity according to the finding of He et al. (2019). That was 369 370 also the possible explanation for the higher diversity at 4°C (lower EC levels) than 20°C. The index exhibited opposite results in granular sludge (e.g., from 6.096 on day-0 to 371

6.777 on day-180) (Table – S1). In both sludges, 'NO<sub>2</sub><sup>-</sup>+NH<sub>4</sub><sup>+</sup> (20°C) groups had the lowest diversity than others, which probably indicated the substrates addition strategy was not suitable for biomass preservation at the community level.

375 The microbial community composition at the phylum level is shown in Figure. S2A/B. There were twenty main microbial phyla (relative abundance  $\geq$  0.1 % in at least one 376 377 sample) detected in all samples, Planctomycetes, Proteobacteria, Bacteroidetes, and 378 Chloroflexi among them accounted for more than 87 % and 83% in floccular and granular sludge, respectively. For floccular sludge, the relative abundance of Planctomycetes (a 379 380 subset of AnAOB) (14.7 – 38.2%), increased under all different strategies except 4°C groups and 'NO<sub>3</sub><sup>-</sup>+NH<sub>4</sub><sup>+</sup> (20°C)', suggesting that low temperature or nitrate addition 381 382 could help AnAOB to tolerate starvation to some extent. Proteobacteria (27.1 - 40.8%), 383 containing nitrite reductase genes (nir) and possibly almost all AerAOB (Wu et al., 2020), showed a trend of decrease under all the conditions. Contrary to that, Chloroflexi (2.2 – 384 7.0%), facultative anaerobes widely existed in autotrophic systems (Chen et al., 2016), 385 386 increased with increasing preservation time. Different from floccular sludge, granular 387 sludge has the stable Planctomycetes (~30%) and Proteobacteria (~22%). It was likely due to the microbial community of granules being more resistant to the external effects 388 389 than flocs according to Wang et al. (2018). In addition, for the heterotrophic bacterium, 390 Firmicutes (2.4 – 5.1%) kept stable in different groups which were the same as floccular sludge. 391

The taxonomic results of dominant nitrogen removal-related bacteria in genus level are shown in Figure. S2C/D. The common AnAOB genera, Candidatus *Brocadia*,

394 Candidatus Kuenenia, and Candidatus Jettenia were identified in floccular and granular sludge. Representative microbial genera were also found for AerAOB (Nitrosomonas) 395 396 and NOB (Nitrospira and Candidatus Nitrotoga). Candidatus Brocadia (belongs to 397 Planctomycetes) dominated the microbial community in both floccular and granular sludge over the 180 days preservation with a relative abundance of 15% and 32%, 398 respectively. For floccular sludge, the relative abundance of Candidatus Brocadia 399 400 increased (up to 20 - 30%), whereas it was stable for granular sludge (25 - 31%). The characteristics of floccular and granular (different particle size distribution) probably 401 402 determined the difference. Ma and Wang (2018) also reported a stable relative 403 abundance of AnAOB in granular sludge (dominated by Candidatus Kuenenia). The 404 relative abundance of *Nitrosomonas*, the only identified AerAOB, was stable around 2 – 405 6% and 1 – 2% in the floccular and granular sludge, respectively. The lower relative abundance in the granular sludge corresponded with the lower AerAOB activity capacity 406 (Section – 3.1.2). A low relative abundance of representative NOB genera (Nitrospira < 407 408 0.6% and Candidatus Nitrotoga < 0.1%) was found in both sludge types. Denitratisoma, 409 another nitrogen removal related genus following denitrifying route, was abundant in all different storage conditions (7 – 14% and 3 – 6% in floccular and granular sludge, 410 411 respectively), which could convert  $NO_2^{-}-N$  or  $NO_3^{-}-N$  (redox in the present study) to  $N_2$ 412 (Vlaeminck et al., 2007). It was likely one of the reasons for the reduction of redox. Moreover, according to Kartal et al. (2007), AnAOB could reduce NO<sub>3</sub><sup>-</sup>-N or NO<sub>2</sub><sup>-</sup>-N to 413 414 NH4<sup>+</sup>-N through dissimilatory reduction. That is probably another possible route for redox removal, but that was not proved in this study. 415

#### 416 **3.4 Properties of sludges during preservation**

#### 417 **3.4.1 EC levels increased and negatively corrected with AnAOB activity**

The EC value (Figure. S3) increased in all storage conditions due to biomass decay 418 (releasing ions, e.g., PO<sub>4</sub><sup>3-</sup>, NH<sub>4</sub><sup>+</sup>, etc.), pH control (HCl or NaOH addition), and chemical 419 addition (NH<sub>4</sub>Cl, NaNO<sub>2</sub>, or NaNO<sub>3</sub>). Under anaerobic conditions, it only slightly 420 increased over 180 days since no chemicals were added. In contrast, the EC value of the 421 422 sludge stored in anoxic conditions rapidly increased, especially for 'NO<sub>2</sub><sup>-</sup>+NH<sub>4</sub><sup>+</sup> (20°C)' 423 probably due to the redox buffer and acid addition. There are two possible reasons to 424 consume redox, i) the existence of denitrifiers (Section – 3.3), and ii) the occurrence of 425 dissimilatory reduction (Kartal et al., 2007). That could also explain the lower EC levels of the sludge stored at 4°C than 20°C. The levels in anoxic conditions were close to or 426 427 even higher than the half inhibition value (IC<sub>50</sub>, 14.6 mS cm<sup>-1</sup> (Lin et al., 2020)) after 180 days of storage. Besides, salinity suppression might be more serious on starved biomass 428 than fresh ones. A negative correlation between EC values and AnAOB activity ( $R^2$  = 429 0.8513, p < 0.05 for floccular sludge and  $R^2$  = 0.8863, p < 0.05 for granular sludge) was 430 431 found (Figure. 5A/B).

### 432 **3.4.2 Heme c decreased**

Heme c was positively decreased during the sludge preservation (Figure. S4), but there was no significant correlation between AnAOB activity and the heme c in both floccular ( $R^2 = 0.8286$ , p > 0.1) and granular ( $R^2 = 0.4703$ , p > 0.1) sludge. Even though the positive correlation has been proven during reactor operation and enrichment (Tang et al., 2010), this rule did not apply in the biomass storage process. Ma and Wang (2018) reported the heme c remained stable during anammox starvation, although the AnAOB activity
gradually decreased. That difference might cause by the different sludge types
(anammox versus PN/A sludge) and dominant genera (Candidatus *Kuenenia* versus
Candidatus *Brocadia*).

#### 442 **3.4.3 EPS decreased**

EPS are metabolic products in bacteria and can represent the cell viability to a content 443 444 (Wang et al., 2013). Regardless of the storage strategy, the EPS content in floccular and granular sludge gradually decreased (Figure-S5). That was in line with Zhang and Bishop 445 446 (2003), who demonstrated that the EPS could be secreted from cells to serve as the energy source for the functional bacteria when suffering from starvation. Gao et al. 447 (2012) also found a significant reduction of EPS in aerobic granular after storage. 448 449 According to Figure – S5, the low temperature probably reduced the EPS hydrolysis rate, 450 whereas the redox buffer addition did not affect that.

#### 451 **3.5 Anaerobic conditions at 20°C were cost-effective sludge storage strategy**

452 An OPEX analysis (Figure. 6) demonstrates that the sludge stored under 'no N spike 453 (20°C)' has the lowest operational expense. Only 104 € ton VSS<sup>-1</sup> and 22 € ton VSS<sup>-1</sup> are needed when storing floccular and granular sludge over 180 days, respectively, which is 454 455 considerably below the storage costs in the continuous presence of redox buffers (at 456 least around 340 € ton VSS<sup>-1</sup>). For 'no N spike (20°C)', pH control (base addition) is the main expense. Except for this, there are no additional costs (e.g., reagents and cooling, 457 458 etc.). As the storage condition which could maintain the highest anammox activity, 'no N spike  $(4^{\circ}C)'$  has the lowest cost in pH control, whereas the cooling price is extremely 459

high (752 € ton VSS<sup>-1</sup>). This leads to the total cost of 'no N spike (4°C)' being more than 460 461 20 times higher than 'no N spike (20°C)'. Considering the most residual anammox activity after storage, 'no N spike (4°C)' is suitable for storing a small amount of sludge in the lab. 462 The cost of pH control (acid addition) during the sludge storage is higher when 463 applying anoxic conditions than for anaerobic conditions. This may be due to the 464 occurrence of denitrification or denitritation, gradually consuming H<sup>+</sup> and increasing pH. 465 466 In addition, the redox buffer addition is another major expense. Even though 'NO<sub>3</sub><sup>-</sup>+NH<sub>4</sub><sup>+</sup>  $(20^{\circ}C)'$  cost less in pH control than 'NO<sub>3</sub><sup>-</sup> (20°C)', it could consume more redox buffer 467 468 probably due to the occurrence of both anammox and denitrification. Both strategies need a much lower cost than 'NO<sub>2</sub><sup>-</sup>+NH<sub>4</sub><sup>+</sup> (20°C)', but they are still at least 5 times higher 469 than that of 'no N spike (20°C)'. 470

The results of the OPEX per specific AnAOB activity (cost-effective analysis) reveal that only 2.3 and  $0.6 \in d \text{ kg NH}_4^+-N^{-1}$  in 'no N spike (20°C)' from the stored floccular and granular sludge are needed. That is more than 15 times lower than anoxic storage strategies. Except for the 'no N spike (20°C)', 'no N spike (4°C)' is the best option even though it needs extremely high cooling costs. That proves the anaerobic condition is more cost-effective for PN/A sludge storage than anoxic ones, especially for the large scale.

478 **3.6 Research application and prospect** 

The findings on the anammox-related parameters (e.g., AnAOB activity) are generical and can be extrapolated to any other sludge. While biomass decay is specific to the sludge tested (e.g., composition and proportion of functional microbes) and should not 482 be extrapolated directly. However, the dominant genus of the sludges in the present is Candidatus Brocadia, which is a typically anammox genus that present in many studied 483 sludges (Ali et al., 2014; Oshiki et al., 2011). For another common AnAOB genus, 484 485 Candidatus Kuenenia, similar findings to the present research were also found by other researchers (Ma and Wang, 2018; Ma et al., 2017). Thus, the conclusions proposed in 486 487 the present research are expected most likely also applicable for other PN/A sludges 488 with different dominant genera. Additionally, for the effect of proportions of functional microbes on the biomass decay, convergence is also expected between different PN/A 489 sludge since most of the microbes in PN/A sludge are heterotrophs (85-90% in the 490 491 mainstream versus 67-84% in this study) (Henze et al., 2000; Lotti et al., 2015; Strous et 492 al., 1998).

493 According to the results of this study, the 4°C without N spike ('no N spike (4°C)') storage strategy was the most effective in maintaining the highest biomass activity 494 capacity after long-term storage. This strategy is recommended for preserving small 495 496 amounts of sludge in the laboratory, but it is too costly for large-scale applications. For 497 the winter bioaugmentation concept in the STPs, the 20°C without N spike ('no N spike (20°C)') strategy deserves to be chosen, since it is the most cost-effective storage strategy. 498 499 Before the full-scale application, there are still several aspects that need to be studied. 500 Firstly, whether the activity of stored sludge can be reactivated quickly at low 501 temperature (<15°C) is essential for the winter bioaugmentation application (stored 502 sludge directly bioaugmented into the mainstream reactor). Secondly, the applicability of the conservation strategy on other AnAOB species (e.g., Candidatus Kuenenia and 503

504 Candidatus Jettenia, etc.) will be tested since the appropriate biomass preservation strategy is usually species-dependent (Ali and Okabe, 2015). Both floccular and granular 505 506 sludge in this study were dominated by Candidatus Brocadia, which is the limitation of 507 this research. Additionally, the Candidatus Brocadia has a higher growth rate, but low substrates affinity (r-strategist) compared to other AnAOB genera (Oshiki et al., 2011), 508 which may be beneficial for 'no N spike' in the present research. Thirdly, whether the 509  $(NO_2 + NH_4)$  is suitable for biomass preservation in the presence of other elements that 510 the metabolic activity requires. Finally, a pilot-scale system should also be established 511 512 to verify the stability of the concept. Using the preservation strategy in large-scale sludge is still a challenge. 513

## 514 **4. Conclusions**

The anaerobic conditions resulted in the higher preservation of the AnAOB activity 515 516 capacity (37 – 55%) than anoxic conditions during storage for 180 days. Despite the 517 higher activity capacity retention at 4°C, 'no N spike (20°C)' is recommended to preserve 518 sludge on a large scale, since it has the lowest value in OPEX per specific AnAOB activity (i.e., OPEX/anammox activity on Day-180, 2.3 and 0.6 € d kg NH<sub>4</sub><sup>+</sup>-N<sup>-1</sup> for floccular and 519 granular sludge, respectively) making it the most cost-effective alternative. Successful 520 biomass reactivation (20°C) and the remained predominant genus (Candidatus Brocadia) 521 furthermore strengthen the potential of this approach. An exponential negative 522 523 correlation between the electrical conductivity and the AnAOB activity was also found.

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## 531 **References:**

Adav, S.S., Chen, M.Y., Lee, D.J., Ren, N.Q., 2007. Degradation of phenol by aerobic

533 granules and isolated yeast Candida tropicalis. Biotechnol. Bioeng. 96, 844-852.

Agrawal, S., Seuntjens, D., De Cocker, P., Lackner, S., Vlaeminck, S.E., 2018. Success of

535 mainstream partial nitritation/anammox demands integration of engineering,

536 microbiome and modeling insights. Curr. Opin. Biotech. 50, 214-221.

537 Ali, M., Okabe, S., 2015. Anammox-based technologies for nitrogen removal: advances

in process start-up and remaining issues. Chemosphere 141, 144-153.

Ali, M., Oshiki, M., Okabe, S., 2014. Simple, rapid and effective preservation and

540 reactivation of anaerobic ammonium oxidizing bacterium "Candidatus Brocadia

- sinica". Water Res. 57, 215-222.
- Ali, M., Rathnayake, R.M., Zhang, L., Ishii, S., Kindaichi, T., Satoh, H., Toyoda, S., Yoshida,
- 543 N., Okabe, S., 2016. Source identification of nitrous oxide emission pathways from a
- single-stage nitritation-anammox granular reactor. Water Res. 102, 147-157.
- 545 Anjali, G., Sabumon, P., 2014. Unprecedented development of anammox in presence of
- 546 organic carbon using seed biomass from a tannery Common Effluent Treatment

- 547 Plant (CETP). Bioresour. Technol. 153, 30-38.
- APHA, 2005. Standard Methods for the Examination of Water and Wastewater. American
   Public Association, Washington, DC.
- 550 Chen, C., Sun, F., Zhang, H., Wang, J., Shen, Y., Liang, X., 2016. Evaluation of COD effect
- 551 on anammox process and microbial communities in the anaerobic baffled reactor
- 552 (ABR). Bioresour. Technol. 216, 571-578.
- 553 Engelbrecht, S., Fondengcap, M.T., Rathsack, K., Martienssen, M., 2016. Highly efficient
- long-term storage of carrier-bound anammox biomass. Water Sci. Technol. 74, 1911-
- 555 1918.
- Ganesan, S., Vadivelu, V.M., 2020. Effect of storage conditions on maintaining anammox
   cell viability during starvation and recovery. Bioresour. Technol. 296, 122341.
- Gao, D., Yuan, X., Liang, H., 2012. Reactivation performance of aerobic granules under
- 559 different storage strategies. Water Res. 46, 3315-3322.
- Hao, X., Wang, Q., Zhang, X., Cao, Y., van Mark Loosdrecht, C., 2009. Experimental
   evaluation of decrease in bacterial activity due to cell death and activity decay in
- activated sludge. Water Res. 43, 3604-3612.
- 563 Henze, M., Gujer, W., Mino, T., van Loosdrecht, M.C.M., 2000. Activated sludge models
- ASM1, ASM2, ASM2d and ASM3: IWA Scientific and Technical Report No. 9. London:
   IWA Publishing.
- He, S., Yang, W., Li, W., Zhang, Y., Qin, M., Mao, Z., 2019. Impacts of salt shocking and the
  selection of a suitable reversal agent on anammox. Sci. Total Environ. 692, 602-612.
- Jetten, M.S., Wagner, M., Fuerst, J., van Loosdrecht, M., Kuenen, G., Strous, M., 2001.

- 569 Microbiology and application of the anaerobic ammonium oxidation ('anammox') 570 process. Curr. Opin. Biotech. 12, 283-288.
- Jin, R.C., Yang, G.F., Zhang, Q.Q., Ma, C., Yu, J.J., Xing, B.S., 2013. The effect of sulfide
  inhibition on the ANAMMOX process. Water Res. 47, 1459-1469.
- 573 Kartal, B., Rattray, J., van Niftrik, L.A., van de Vossenberg, J., Schmid, M.C., Webb, R.I.,
- 574 Schouten, S., Fuerst, J.A., Damsté, J.S., Jetten, M.S., 2007. Candidatus 575 "Anammoxoglobus propionicus" a new propionate oxidizing species of anaerobic 576 ammonium oxidizing bacteria. Syst. Appl. Microbiol. 30, 39-49.
- Lackner, S., Gilbert, E.M., Vlaeminck, S.E., Joss, A., Horn, H., van Loosdrecht, M.C., 2014.
- Full-scale partial nitritation/anammox experiences—an application survey. Water Res.
  579 55, 292-303.
- Lu, Y.Z., Fu, L., Li, N., Ding, J., Bai, Y.N., Samaras, P., Zeng, R.J., 2018. The content of trace
- element iron is a key factor for competition between anaerobic ammonium
  oxidation and methane-dependent denitrification processes. Chemosphere, 198,
  370-376.
- Lin, L., Pratt, S., Rattier, M., Ye, L., 2020. Individual and combined effect of salinity and
  nitrite on freshwater Anammox bacteria (FAB). Water Res. 169, 114931.
- Lotti, T., Kleerebezem, R., Hu, Z., Kartal, B., de Kreuk, M.K., van Erp Taalman Kip, C., Kruit,
- 587 J., Hendrickx, T.L.G., van Loosdrecht, M.C.M., 2015. Pilot-scale evaluation of
- anammox-based mainstream nitrogen removal from municipal wastewater. Environ.
- 589 Technol. 36, 1167-1177.
- Lotti, T., Kleerebezem, R., van Erp Taalman Kip, C., Hendrickx, T.L., Kruit, J., Hoekstra, M.,

- 591 Van Loosdrecht, M.C., 2014. Anammox growth on pretreated municipal wastewater.
- 592 Environ. Sci. Technol. 48, 7874-7880.
- 593 Ma, X., Wang, Y., 2018. Anammox bacteria exhibit capacity to withstand long-term 594 starvation stress: a proteomic-based investigation of survival mechanisms. 595 Chemosphere 211, 952-961.
- Ma, X., Wang, Y., Zhou, S., Yan, Y., Lin, X., Wu, M., 2017. Endogenous metabolism of
  anaerobic ammonium oxidizing bacteria in response to short-term anaerobic and
  anoxic starvation stress. Chem. Eng. J. 313, 1233-1241.
- Ma, Y., Sundar, S., Park, H., Chandran, K., 2015. The effect of inorganic carbon on
   microbial interactions in a biofilm nitritation–anammox process. Water Res. 70, 246
   254.
- ----
- Mulder, A., Van de Graaf, A.A., Robertson, L., Kuenen, J., 1995. Anaerobic ammonium
  oxidation discovered in a denitrifying fluidized bed reactor. FEMS Microbiol. Ecol. 16,
  177-183.
- Oshiki, M., Shimokawa, M., Fujii, N., Satoh, H., Okabe, S., 2011. Physiological
   characteristics of the anaerobic ammonium-oxidizing bacterium 'Candidatus
   Brocadia sinica'. Microbiology 157, 1706-1713.
- Peng, L., Xie, Y., Van Beeck, W., Zhu, W., Van Tendeloo, M., Tytgat, T., Lebeer, S., Vlaeminck,
- 609 S.E., 2020. Return-Sludge Treatment with Endogenous Free Nitrous Acid Limits
- Nitrate Production and N<sub>2</sub>O Emission for Mainstream Partial
  Nitritation/Anammox. Environ. Sci. Technol. 54, 5822-5831.
- Rothrock, M.J., Vanotti, M.B., Szögi, A.A., Gonzalez, M.C.G., Fujii, T., 2011. Long-term

- preservation of anammox bacteria. Appl. Microbiol. Biot. 92, 147-157.
- 614 Shi, Z.J, Huang, B.C., Jin, R.C., 2020. A novel strategy for anammox consortia preservation:
- Transformation into anoxic sulfide oxidation consortia. Sci. Total Environ. 723, 138094.
- 517 Strous, M., Heijnen, J.J., Kuenen, J.G., Jetten, M.S.M., 1998. The sequencing batch 618 reactor as a powerful tool for the study of slowly growing anaerobic ammonium-619 oxidizing microorganisms. Appl. Microbiol. Biotechnol. 50, 589-596.
- 620 Strous, M., Kuenen, J.G., Jetten, M.S., 1999. Key physiology of anaerobic ammonium
- oxidation. Appl. Environ. Microb. 65, 3248-3250.
- Talan, A., Tyagi, R., Drogui, P., 2021. Critical review on insight into the impacts of different
- 623 inhibitors and performance inhibition of anammox process with control strategies.
- 624 Environ. Technol. Inno. 23, 101553.
- Tang, C.J., Zheng, P., Wang, C.H., Mahmood, Q., 2010. Suppression of anaerobic
- ammonium oxidizers under high organic content in high-rate Anammox UASB
  reactor. Bioresour. Technol. 101, 1762-1768.
- Vadivelu, V.M., Keller, J., Yuan, Z., 2007. Effect of free ammonia on the respiration and
- growth processes of an enriched Nitrobacter culture. Water Res. 41, 826-834.
- Van de Graaf, A.A., Mulder, A., de Bruijn, P., Jetten, M., Robertson, L., Kuenen, J.G., 1995.
- 631 Anaerobic oxidation of ammonium is a biologically mediated process. Appl. Environ.
- 632 Microb. 61, 1246-1251.
- Viancelli, A., Pra, M., Scussiato, L., Cantão, M., Ibelli, A., Kunz, A., 2017. Preservation and
- 634 reactivation of Candidatus Jettenia asiatica and Anammoxoglobus propionicus using

- different preservative agents. Chemosphere 186, 453-458.
- Vlaeminck, S.E., Geets, J., Vervaeren, H., Boon, N., Verstraete, W., 2007. Reactivation of
- aerobic and anaerobic ammonium oxidizers in OLAND biomass after long-term
  storage. Appl. Microbiol. Biot. 74, 1376-1384.
- Vlaeminck, S.E., Terada, A., Smets, B.F., De Clippeleir, H., Schaubroeck, T., Bolca, S.,
  Demeestere, L., Mast, J., Boon, N., Carballa, M., 2010. Aggregate size and
  architecture determine microbial activity balance for one-stage partial nitritation
  and anammox. Appl. Environ. Microb. 76, 900-909.
- Wang, C., Liu, S., Xu, X., Guo, Y., Yang, F., Wang, D., 2018. Role of cyclic diguanylate in
  affecting microbial community shifts at different pH during the operation of
  simultaneous partial nitrification, anammox and denitrification process. Sci. Total
  Environ. 637, 155-162.
- Wang, D., Wang, G., Zhang, G., Xu, X., Yang, F., 2013. Using graphene oxide to enhance
  the activity of anammox bacteria for nitrogen removal. Bioresour. Technol. 131, 527530.
- Wang, T., Zhang, H., Yang, F., 2016. Long-term storage and subsequent reactivation of
  Anammox sludge at 35 °C. Desalin. Water Treat. 57, 24716-24723.
- 653 start-up of single and two-stage Anammox processes with real low-strength 654 wastewater treatment. Chemosphere 245, 125572.

Wu, P., Zhang, X., Wang, X., Wang, C., Faustin, F., Liu, W., 2020. Characterization of the

- 655 Xing, B.S., Guo, Q., Jiang, X.Y., Chen, Q.Q., He, M.M., Wu, L.M., Jin, R.C., 2016. Long-term
- 656 starvation and subsequent reactivation of anaerobic ammonium oxidation

- 657 (anammox) granules. Chem. Eng. J. 287, 575-584.
- Zhang, X., Bishop, P.L., 2003. Biodegradability of biofilm extracellular polymeric
  substances. Chemosphere 50, 63-69.
- 260 Zhu, W., Li, J., Dong, H., Wang, D., Zhang, P., 2017. Effect of influent substrate ratio on
- anammox granular sludge: performance and kinetics. Biodegradation 28, 437-452.