Selective oxidation of CH4 to CH3OH through plasma catalysis : insights from catalyst characterization and chemical kinetics modelling

Selective Oxidation of CH_4 to CH_3OH through Plasma Catalysis: Insights from Catalyst Characterization and Chemical kinetics modelling

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ABSTRACT

The selective oxidation of methane to methanol (SOMTM) by molecular oxygen is a holy grail in catalytic chemistry and remains a challenge in chemical industry. We perform SOMTM in a CH_4/O_2 plasma, at low temperature and atmospheric pressure, promoted by Ni-based catalysts, reaching 81 % liquid oxygenates selectivity and 50 % CH_3OH selectivity, with an excellent catalytic stability. Chemical kinetics modelling shows that CH_3OH in the plasma is mainly produced through radical reactions, i.e., $CH_4 + O(1D) \rightarrow CH_3O + H$, followed by $CH_3O + H + M \rightarrow CH_3OH + M$ and $CH_3O + HCO \rightarrow CH_3OH + CO$. The catalyst characterization shows that the improved production of CH_3OH is attributed to abundant chemisorbed oxygen species, originating from highly dispersed NiO phase with strong oxide support interaction with γ-Al_2O_3, which are capable of promoting CH_3OH formation through E-R reactions and activating H_2O molecules to facilitate CH_3OH desorption.

KEY WORDS: Methane Conversion; Plasma Catalysis; Selective Oxidation; Methanol Synthesis; Plasma Chemistry

1. Introduction

Methane (CH_4), abundant in natural gas, shale gas, coalbed gas, biogas and dry gas (i.e., emission of chemical industry), has become not only an important source of clean fossil energy, but also a feedstock for the chemical industry. At present, the industrial utilization of CH_4 is initiated by high temperature steam reforming to syngas (CO and H_2), which is then transformed into hydrocarbons through the Fischer-Tropsch process, or into methanol (CH_3OH), through a high-pressure reaction over Cu-Zn-Al catalyst. CH_3OH is a versatile molecule for the production of many bulk chemicals, such as ethylene, propylene and aromatics.[1] However, due to the strong C-H bond energy (439 kJ/mol), the negligible electron affinity and low polarizability of CH_4, as well as thermodynamic limitations, the syngas pathway is energy intensive and costly, which stimulates researchers to develop novel approaches for the conversion of CH_4. Thus, the selective oxidation of methane to methanol (SOMTM) is attracting more and more attention. [2, 3]

SOMTM is being studied by homogeneous catalysis, in strong acid media (sulfuric and trifluoroacetic acid), using complex catalysts with noble metals (Pt and Pd) as central atoms.[4-6] Alternatively, SOMTM can also be realized by impressive heterogeneous catalysis, e.g. iron-based zeolites [7, 8] and copper-based zeolites, [9-11] or supported noble metals, such as Au, Pd and Rh.[12, 13] However, numerous works in homogeneous or heterogeneous catalysis adopted high price oxidants such as N_2O or H_2O_2, which made this process economically infeasible in large-scale application. Using the abundant and cheap molecular oxygen (O_2) as oxidant, (R1),

would be highly desirable in industrial application.

$$CH_4 + 1/2\ O_2 \rightarrow CH_3OH \qquad \triangle H^0_{298K} = -126.2\ kJ\ mol^{-1} \qquad (R1)$$

SOMTM by O_2, R1, has been extensively studied. Colloidal Au-Pd nanoparticles exhibited high CH_3OH selectivity (92%) in aqueous solution at mild temperatures on SOMTM with H_2O_2 and O_2 as oxidants. More oxygenated products were formed than the amount of H_2O_2 consumed, suggesting that the controlled breakdown of H_2O_2 activates methane, which subsequently incorporates molecular oxygen through a radical process.[12] CeO_2/Cu_2O catalysts were able to activate methane at room temperature, and water addition could generate centers on the catalyst surface with special electronic properties, on which methane can directly interact to yield methanol. [14, 15] Recently, highly active Au-Pd nanoparticles were encapsulated inside zeolites and modified with a hydrophobic sheath, which can considerably enhance the oxidation of methane to methanol.[16] The silanes appeared to allow diffusion of H_2, O_2, and CH_4 to the catalyst active sites, while confining the in-situ generated H_2O_2 decomposition, which provided a high local peroxide concentration to facilitate methanol production, with 17.3 % methane conversion and 92% methanol selectivity. Additionally, chemical looping was also proposed to inhibit methane overoxidation on Cu- or Fe- containing zeolite catalysts.[17]

Although great progress has been reported, SOMTM is, currently, still being considered as a dream reaction in chemical industry and a holy grail in catalytic chemistry. [3, 17, 18] Generally, it has to overcome two challenges, caused by thermodynamics and kinetics, respectively. The first is how to improve the CH_3OH

selectivity. Thermodynamically, CH_3OH is not the favorable product, as CO and CO_2 are more stable than CH_3OH. Specifically, as shown in Figure S1, a low temperature ($<$890 K) favors the production of CO_2 and H_2O, while a high temperature ($>$ 890 K) favors CO and H_2. In other words, due to the higher reactivity of CH_3OH than the feedstock CH_4, the catalytic sites, capable of oxidizing CH_4 into CH_3OH, can also further oxidize CH_3OH into CO or CO_2 before CH_3OH can desorb from the catalyst surface. The second challenge is how to reduce the kinetic energy barrier (Ea) of SOMTM by O_2 at ambient conditions. The Ea of SOMTM by O_2 is much higher than for SOMTM using N_2O or H_2O_2 as oxidants, because both N_2O and H_2O_2 can more easily release an oxygen atom, as the main species to trigger the oxidation of CH_4 to CH_3OH. Therefore, when using O_2 as oxidant, high temperature and high activity catalysts are needed to overcome the Ea of SOMTM, which unfortunately leads to deep oxidation.

One approach to overcome the above-mentioned challenges is a stepwise process, i.e., stoichiometric chemical looping, which involves three separate steps: (1) activation of the metal-zeolite catalyst by an oxidant at a relative high temperature (250-500 ^oC), (2) methane reaction at a relative low temperature (25-200 ^oC), and (3) methanol extraction using a solvent or steam at a relative low temperature (25-200 ^oC). [9, 19, 20] Currently, Cu and Fe exchanged zeolites have been extensively studied, and significant attention was given to the elucidation of the nature of copper-oxo and iron-oxo active sites. [17, 20] However, the state-of-the-art conversion of methane to methanol via chemical looping stays a factor ~50 below the industrial threshold in an

overall production rate, and improvement on material productivity and decreased cycle time are highly needed for this process.[21]

Another approach to overcome the above-mentioned challenges is plasma catalysis. Non-thermal plasma (NTP), which is an ionized gas with clear non-equilibrium character, offers a distinct approach to activate molecules by energetic electrons instead of heat, and thus triggers chemical reactions at low temperature.[22-27] Generally, the gas temperature in NTP remains near room temperature, while the generated electrons exhibit a typical temperature of 1-10 eV (~ 10^4 – 10^5 K), which is sufficient to activate feed gas molecules (e.g., CH_4 and O_2) into reactive species, including radicals, excited atoms and molecules, and ions. Several scientists have studied SOMTM by O_2 through plasma and/or plasma catalysis, [28-36] but only a few have reported satisfying CH_3OH selectivity. Nozaki applied a microplasma and obtained a CH_4 conversion to synthetic fuels with maximum organic liquid selectivity of 70 % without catalysts (plasma alone), [28] but the CH_3OH selectivity was below 15 %. Indarto realized CH_3OH synthesis with optimum selectivity of 23 % using a dielectric barrier discharge (DBD) reactor with Ni metal doped over yttria-stabilized zirconia as catalyst.[29] Chawdhury used a packed bed DBD reactor, in which glass beads provided an optimal CH_3OH selectivity of 35.4 %, [30] while further work reported the best CH_3OH selectivity of 37 % using $CuO/\gamma\text{-}Al_2O_3$ catalyst.[31] Recently, $Cu/\gamma\text{-}Al_2O_3$, $Ni/\gamma\text{-}Al_2O_3$ and $Fe/\gamma\text{-}Al_2O_3$ catalysts were compared for plasma-catalytic methane to value-added liquid fuels and chemicals, in which the highest liquid oxygenate (~ 71%) were achieved, with $Fe/\gamma\text{-}Al_2O_3$ catalyst exhibited highest methanol selectivity of 36.0% among three different catalysts.[32] In

addition, insights from microkinetic modelling for plasma-catalytic SOMTM process were obtained on Pt(111) surface and the results showed that vibrational excitation and especially radicals produced from CH_4/O_2 NTP could enhance the turnover frequency (TOF) and improve the selectivity of CH3OH, HCOOH and C2 hydrocarbons. [33] In general, this field is still in the early research stages and fundamental information on the interaction of NTP with a catalyst is still lacking, and the limited CH_3OH selectivity in most studies is attributed to the further oxidation of CH_3OH into CO and CO_2. [34] Additionally, the reaction pathway for the production of CH_3OH and by-products (HCHO, HCOOH, CO and CO_2) from CH_4 and O_2 in NTP is largely unknown.

Inspired by Lustemberg's work that Ni-CeO_2 catalysts shows excellent activity in SOMTM at moderate conditions,[37] in this paper, we report SOMTM in a CH_4/O_2 plasma promoted by Ni-based catalysts, with 50 % selectivity to CH_3OH, and total liquid oxygenates selectivity of 81 %, and with excellent catalytic stability. In addition, we identify the underlying reaction mechanisms by combined experiments and modeling.

2. Experimental section

2.1 Catalyst preparation

The catalysts were synthesized by the incipient wetness impregnation method (Scheme S1). Commercial γ-Al_2O_3 pellets (1-2 mm diameter), synthesized by a hydrothermal method, were calcined at 400 °C in a muffle oven for 5 hours before they were used as supports. All analytical grade chemicals were purchased from Tianjin Kemiou Chemical Reagent Co. Ltd. (Tianjin, China) and used without further

purification. The preparation procedure of the Ni catalysts is described in Scheme S2: First, the precursor salt $Ni(NO_3)_2 \cdot 6H_2O$ was dissolved in deionized water, followed by the addition of γ-Al_2O_3 pellets under stirring. After 12 hours aging at room temperature, the sample was dried at 120 °C overnight. Finally, the sample was calcined by a muffle oven at 540 °C for 5 hours in air condition, and the catalyst was noted as NiO/γ-Al_2O_3. Varied nickel loading, i.e., 2, 6, 10, 15, 20, and 25 wt.% catalysts were synthesized based above method.

2.2 Experimental setup

The experimental plasma catalysis setup is shown in Scheme S2. The plasma catalytic SOMTM by O_2 was carried out using a coaxial DBD reactor with a novel water electrode (grounding electrode) at atmospheric pressure. The DBD reactor consists of a pair of coaxial quartz cylinders (inner and outer quartz tubes) in which a stainless-steel (2 mm outer diameter) electrode was placed in the center, and circulating water was pumped into the space between the inner and outer cylinder. A tungsten filament is installed in between both cylinders to connect this circulating water (flowing between this inner and outer wall) with a ground wire (outside of the reactor wall), so that the circulating water acts as a ground electrode of our DBD. The flow rate (6 L/min) and temperature of water was controlled by thermostatic baths with a circulation pump and external temperature controller, which can effectively remove the heat generated by the discharge and maintain a constant reaction temperature. The discharge length is 50 mm (defined by the length of the ground electrode, i.e., region of circulating water) and the inner diameter of the inner quartz cylinder is 10 mm, yielding a discharge gap

of 4 mm. In the plasma catalysis experiments, the discharge space was fully packed by 1.25 g catalyst. CH_4 and O_2 were monitored by calibrated mass flow controllers and mixed homogeneously before passing through the plasma reactor. Before igniting the discharge, this gas mixture passed through the plasma reactor for about 10 minutes to remove air, to ensure a safe operating procedure (outside the explosion limit). The change of gas volume after the reaction was measured using a soap-film flow meter. This is needed to quantitatively analyze the gas composition, and to achieve the exact conversion (CH_4) and selectivity of the gaseous products (CO and CO_2). The discharge voltage and current were detected by a digital phosphor oscilloscope (Tektronix, DPO 3012) with a high voltage probe (Tektronix P6015) and a current probe (Pearson 6585).

The feedstock and gas products were analyzed by an on-line gas chromatograph (Tianmei GC-7900, TDX-01 column, Al_2O_3 packed column) with a thermal conductivity detector (TCD) and a flammable ionized detector (FID). The liquid products were cooled by a liquid trap (mixer of isopropyl alcohol and liquid nitrogen, below -120 ºC) and then analyzed by GC-2014C (Shimadzu, PEG-2000 column), GC-MS (Agilent 5975C, DB-1701 column), FTIR (ThermoFisher 6700) and ^{1}H-NMR (Bruker AVANCE III 500). The reaction products, including H_2O, CO, CO_2, CH_3OH, HCHO, HCOOH, $HCOOCH_3$, C_2H_5OH, CH_3CHO, and CH_3COOH, were analyzed using external standards. The gas products were measured by gas chromatography, while the liquid products were collected by a liquid trap and analyzed by GC, GC-MS, FTIR and ^{1}H-NMR (Figure S2). The formulas of the standard calibrated concentration curves are shown in Table S1. More details about qualitative and quantitative analysis

of products on CH_4/O_2 NTP could be found in supporting information. In this work, the conversion of CH_4 and the selectivity of the gaseous products (CO_x, H_2 and C_2H_6) are calculated as follows. Note that the selectivity of CO_x and C_2H_6 is calculated based on carbon, while the selectivity of H_2 and H_2O is calculated based on hydrogen.

The CH_4 conversion was calculated by:

$$X_{CH_4}\ (\%) = \frac{\text{moles of } CH_4 \text{ converted}}{\text{moles of initial } CH_4} \times 100\ \% \quad (1)$$

The selectivity of the gaseous products was calculated as：

$$S_{CO}\ (\%) = \frac{\text{moles of CO produced}}{\text{moles of } CH_4 \text{ converted}} \times 100\ \% \quad (2)$$

$$S_{CO_2}\ (\%) = \frac{\text{moles of } CO_2 \text{ produced}}{\text{moles of } CH_4 \text{ converted}} \times 100\ \% \quad (3)$$

$$S_{H_2}\ (\%) = \frac{\text{moles of } H_2 \text{ produced}}{2 \times \text{moles of } CH_4 \text{ converted}} \times 100\ \% \quad (4)$$

$$S_{H_2O}\ (\%) = 100\ \% - (S_{CH_3OH} + S_{HCHO} + S_{HCOOH} + S_{H_2} + S_{C_2}) \quad (5)$$

$$S_{C_2H_6}\ (\%) = \frac{2 \times \text{moles of } C_2H_6 \text{ produced}}{\text{moles of } CH_4 \text{ converted}} \times 100\ \% \quad (6)$$

The selectivity of the liquid products was calculated as follows:

$$\text{Total selectivity of liquid products (\%)} = 100\ \% - (S_{CO} + S_{CO_2} + S_{C_2H_6}) \quad (7)$$

The selectivity of the various oxygenates, $C_xH_yO_z$, can be calculated as:

$$S_{C_xH_yO_z}\ (\%) = \frac{X \times N_{C_xH_yO_z}}{\sum X_i N_i} \times \text{eq } 5 \quad (8)$$

Where $N_{C_xH_yO_z}$ represents the number of moles of various oxygenates in the liquid fraction. Note that we define here the carbon-based selectivity, and thus, H_2O and H_2O_2 are not included in this formula.

The corresponding yields of these $C_xH_yO_z$ oxygenates are calculated as:

$$Y_{C_xH_yO_z}(\%) = S_{C_xH_yO_z}(\%) \times X_{CH_4}(\%) \quad (9)$$

Finally, we defined the energy efficiency for CH_3OH formation (mol/kwh) as :

$$\text{Energy efficiency} = \frac{\text{moles of methanol produced (mol/h)}}{\text{discharge power(kW)}} \quad (10)$$

2.3 Catalyst characterization and NTP diagnostics

The structural properties of the NiO/γ-Al_2O_3 catalysts were investigated by X-ray diffraction (XRD), conducted using a SmartLab 9kW diffractometer with Cu Kα radiation (240 kV, 50 mA). The H_2-temperature programmed reduction (H_2-TPR) was performed on a Quanta chrome ChemBET Pulsar Chemisorption instrument. Before the analysis, the samples (0.20 g) were pretreated with He from ambient temperature to 150 °C, and kept at 150 °C for 60 minutes. Afterward, the samples were cooled to 50 °C in He atmosphere. Finally, the H_2-TPR was carried out in a flow of H_2/Ar mixture (120 ml/min, 10％ H_2) from 100 °C to 1000 °C at a heating rate of 10 °C/min. X-ray photoelectron spectroscopy (XPS) was conducted by Thermo Fisher ESCALAB XI^+ with Al Kα X-ray source. The C 1s binding energy value (284.8 eV) was taken as a reference level. Nitrogen physisorption was conducted on a Micromeritics ASAP 2020 instrument at -196 °C to obtain textural information. Prior to the measurement, the samples were degassed at 400 °C for 6 h. The surface area was calculated by the BET method and the pore volume was obtained by the t-plot method. The chemical composition of the NiO/γ-Al_2O_3 catalysts with various loading was analyzed by X-ray fluorescence (XRF) on S8 TICER from Bruker AXS. Thermogravimetry was conducted by Netzsch STA 449 F3 connected to a Balzers QMG 403D mass spectrometer. High-resolution transmission electron microscopy (HRTEM) was conducted on Tecnai G2

F30 S-Twin with 300 kV accelerating voltage. High angle annular dark field scanning transmission electron microscopy (HAADF-STEM) was performed by Titan^{3TM} G2 60-300 with Cs-corrector configuration. The CH_4/O_2 NTP was investigated by optical emission spectroscopy (OES) through a spectrograph (SP2758, Princeton instrument company). A fiber was directly connected at the wall of the plasma reactor, to detect the emission, which was analyzed by a spectrograph (750 mm, 300 G/mm gratings). A CCD (PIXIS:400BR_eXcelon) was used to record the spectra with an on-line computer.

3 Results and discussion

3.1 Catalytic Performance

As shown in Figure 1A, the CH_4 conversion is zero when using only the $NiO/\gamma\text{-}Al_2O_3$ catalyst in the absence of NTP, indicating that SOMTM by O_2 cannot be triggered over $NiO/\gamma\text{-}Al_2O_3$ catalyst without help of NTP. In plasma alone, 4.1 % CH_4 conversion is achieved with 42.2 % CH_3OH selectivity, and no hydrocarbons have been detected by the GC. Hence, plasma alone is able to quite selectively produce CH_3OH in our setup, while it is generally stated in literature that it is not selective at all, and needs a catalyst for the selective production of target compounds. [22, 34] This is attributed to the short residence time, as will be explained by the modeling results below. Furthermore, the influence of NTP (CH_4/O_2 molar ratio, temperature of grounding electrode, discharge power and residence time) was also been studied, as shown in Figure S3-S6. After packing by $\gamma\text{-}Al_2O_3$, the CH_4 conversion is slightly enhanced to 4.6 %, while the CH_3OH selectivity is reduced to 41.4 %. However, when using $NiO/\gamma\text{-}Al_2O_3$ catalyst (10 wt.% loading), the CH_4 conversion and CH_3OH selectivity increase to 6.4 % and

49.7 %, respectively, indicating that NiO/γ-Al_2O_3 catalyst has a positive effect on the CH_3OH production in CH_4/O_2 NTP. The CH_4 conversion is still limited, attributed to the short residence time of the gas inside the DBD reactor (high space velocity). By tuning the flow rates and other discharge conditions, it should be possible to enhance the conversion, but in this paper, we mainly focus on inhibiting the CH_4 overoxidation, to increase the liquid oxygenates selectivity, especially for CH_3OH production. The complete product distribution is shown in Figure S7 and S8, and the total selectivity of liquid oxygenates reaches 80.7 %. This striking result is again attributed to the short residence time, as illustrated by the modeling below.

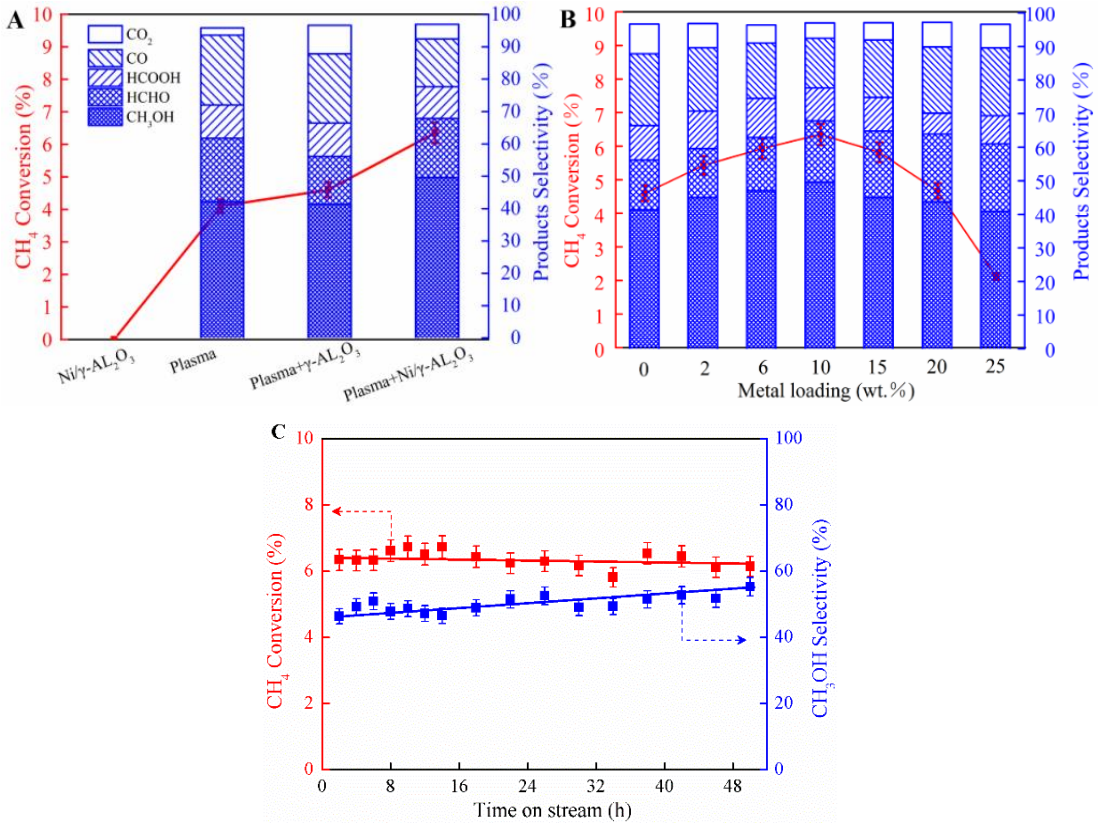


Figure 1. Experimental results of SOMTM. (A). CH_4 conversion and products selectivity, using only NiO/γ-Al_2O_3 catalyst, only plasma, plasma with γ-Al_2O_3 beads, and plasma with (10 wt.%) NiO/γ-Al_2O_3 catalyst (400 ml/min CH_4, 200 ml/min O_2, 85 °C circulating water, 1.25 g NiO/γ-Al_2O_3 catalyst, 30 W discharge power and 0.375

s residence time). (B). Effect of Ni loading on CH_4 conversion and products selectivity, for plasma with NiO/γ-Al_2O_3 catalyst. (C). Stability test of the (10 wt.%) NiO/γ-Al_2O_3 catalyst in CH_4/O_2 NTP during 50 h continuous operation.

Furthermore, we studied NiO/γ-Al_2O_3 catalysts with varied loading (Figure 1B). The highest CH_4 conversion and CH_3OH selectivity were both achieved at 10 wt.% loading. Moreover, we operated the CH_4/O_2 NTP with 10 wt.% NiO/γ-Al_2O_3 catalyst continuously for 50 hours, and the CH_4 conversion and CH_3OH selectivity remained stable (Figure 1C), indicating the excellent catalytic stability of the NiO/γ-Al_2O_3 catalyst in CH_4/O_2 NTP for CH_3OH production. The results obtained in this paper have been compared with those in literature. As shown in Figure 2A, the CH_3OH productivity (27.3 mmol•g_{cat}^{-1}•h^{-1}) calculated by formula (1) of the SI is two orders of magnitude higher than the best results obtained through stoichiometric chemical looping using O_2 as the oxidant. [20, 38] As shown in Figure 2 B, the CH_3OH selectivity is higher than the best results obtained through plasma catalysis, using various catalysts, albeit at a lower CH_4 conversion. [30-32]

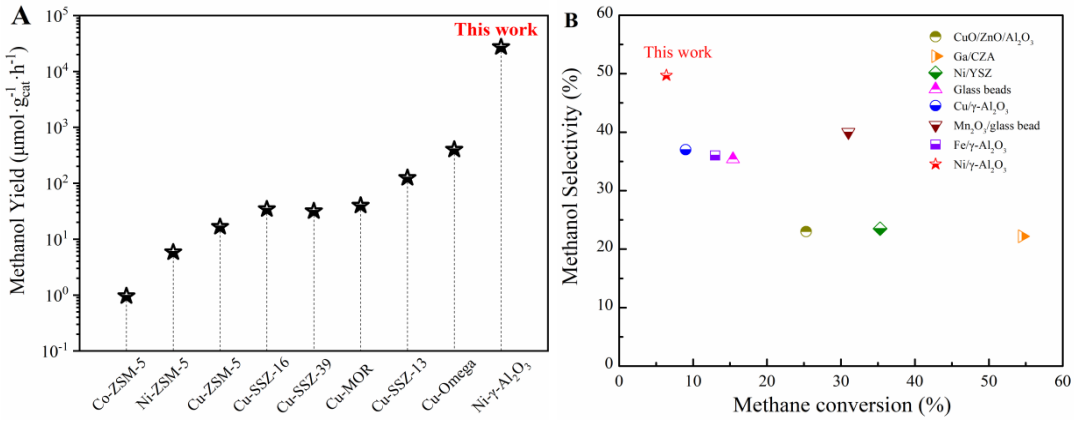


Figure 2. Comparison of this work with literature results. A: CH_3OH productivity by stoichiometric chemical looping using O_2 as the oxidant, for different catalyst materials (calculated based on the results adapted from references 20 and 38); B: CH_3OH

299 selectivity by plasma catalysis using O_2 as the oxidant (adapted from reference 30-32).
300
301 The hydrogen-based products selectivity is shown in Figure S9. The selectivity of
302 CH_3OH is almost 50 % in the case of "plasma + NiO/γ-Al_2O_3 catalyst, i.e., over 18 %
303 higher than in the case of plasma or plasma + γ-Al_2O_3 beads. The H_2 and H_2O
304 selectivities reach 5.6 % and 29.1 %, respectively, while the selectivities of HCHO and
305 HCOOH are around 9 % and 4.9 %, respectively, in the case of "plasma + NiO/γ-Al_2O_3
306 catalyst (10 wt.% loading).
307 Energy efficiency is a key performance indicator for plasma-catalytic SOMTM. We
308 defined the energy efficiency for CH_3OH formation by formula (7), in which the plasma
309 power was calculated through mathematical integration using the waveform of
310 discharge voltage (Figure S10) and discharge current (Figure S11). As illustrated by
311 Figure S12, the energy efficiency in the plasma-only case is 0.76 mol/kWh; it rises
312 slightly to 0.95 mol/kWh with γ-Al_2O_3, but with NiO/γ-Al_2O_3, it rises dramatically to
313 1.4 mol/kWh. Thus, while the CH_4 conversion and CH_3OH selectivity only increase by
314 2.3 % and 7.5 %, respectively, in case of plasma catalysis compared to plasma alone,
315 the energy efficiency rises by 84 %. Furthermore, the produced methanol with high
316 concentration (1.3 mol/L) in liquid can be condensed in the online cold-trap, without
317 further methanol extraction using a solvent or steam, which can avoid a stepwise
318 process on heterogeneous catalysis. This continuous operation condition under low
319 temperature and atmosphere pressure exhibited the great potential for plasma-catalytic
320 SOMTM by CH_4/O_2 NTP.
321 **3.2 Chemical kinetics modelling of CH_4/O_2 DBD plasma**

As mentioned above, in plasma alone, we achieved 42 % CH_3OH selectivity (Figure 1A), which is much better than most results in literature. [28-36] To explain this result, we performed chemical kinetics modelling of CH_4/O_2 DBD plasma using ZDPlaskin.[39] Details about the modelling, the species (Table S2) and reactions (Tables S3-S5) in the model, are presented in SI.

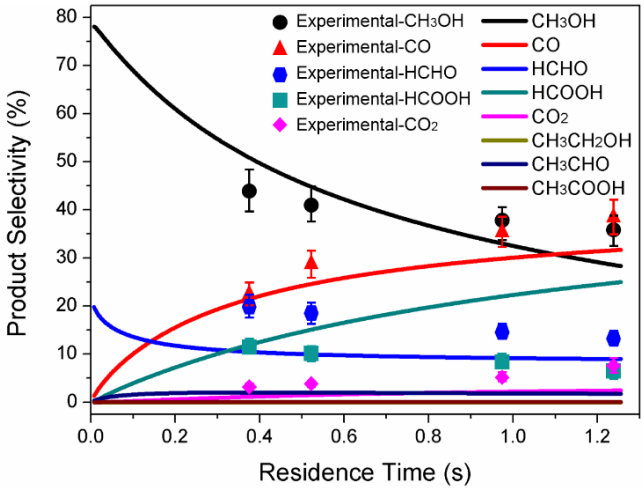
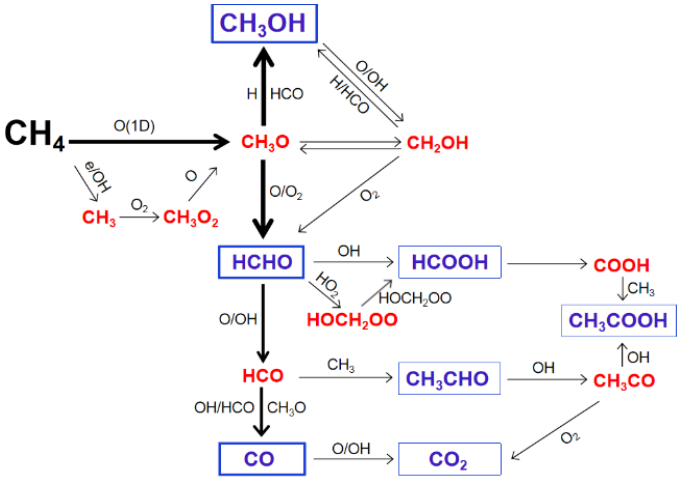


Figure 3. Products selectivity in CH_4/O_2 plasma, obtained by chemical kinetics modeling (lines) and experiments (symbols) as function of residence time, for the same conditions as in Figure 1.



Scheme 1. Reaction pathways for the formation of CH_3OH and other oxygenates in the CH_4/O_2 plasma, predicted by chemical kinetics modelling (ZDPlaskin). Red color indicates reaction intermediates and blue color with rectangles means stable products. The size of the products is approximately proportional to their selectivity and the

thickness of the arrow lines is proportional to the net rate of that reaction.

The lines in Figure 3 depict the calculated products selectivity as function of residence time, derived from the densities of the species in the plasma (Figure S13). Initially, the calculated CH_3OH selectivity is extremely high (~ 78 %), but it decreases gradually upon increasing residence time, until about 30 % for a residence time of 1.2s. HCHO exhibits a similar evolution (but with maximum selectivity around 20 %), while CO, HCOOH and CO_2 exhibit the opposite trend. To verify the modelling, we performed experiments at varying residence time (symbols in Figure 3). The experimental selectivities of CH_3OH, HCHO, CO and CO_2 agree reasonably well with the modelling results (similar trends), indicating that the model provides a realistic picture of the formation of these products in the CH_4/O_2 plasma. For HCOOH, however, the agreement is not yet satisfying, suggesting that important production or loss processes for HCOOH might be missing in the model, or that their rate coefficients are not correct, but we can only rely on the input data (chemical reactions and corresponding rate coefficients) available in literature, and we don't want to tune the model to fit it to the experiments without scientific basis. However, it means that our model cannot yet be used to predict the reaction pathways for HCOOH, but we can use it for the other possible reaction pathways in the CH_4/O_2 plasma. As shown in Scheme 1, CH_3OH is mainly produced from CH_3O species through the reactions $CH_3O + H + M \rightarrow CH_3OH + M$ and $CH_3O + HCO \rightarrow CH_3OH + CO$.

3.3 NiO/γ-Al_2O_3 Catalysts characterization

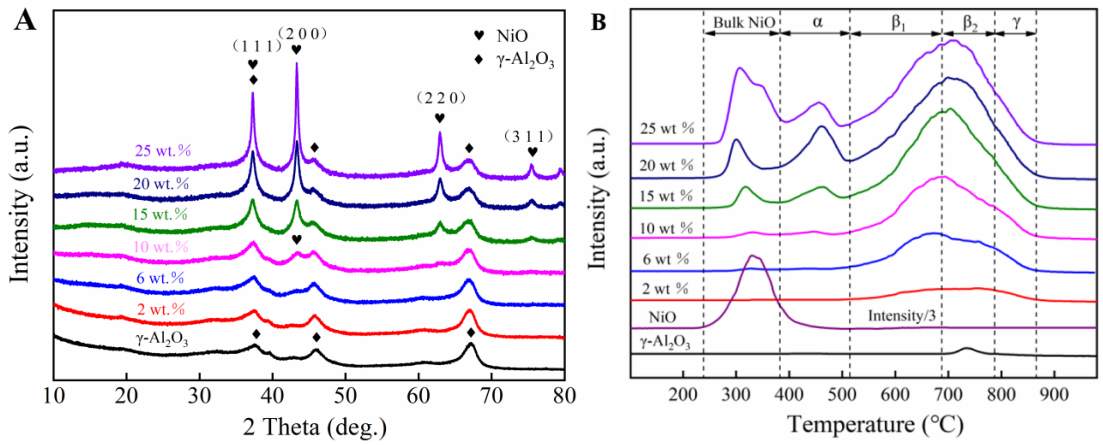
In spite of the high CH_3OH selectivity at short residence time, the CH_4 conversion is

358 quite low (4.1 %), caused by the high space velocity. However, as shown in Figure 1,
359 the Ni catalyst (with 10 wt. % loading) enhances both the CH_4 conversion and CH_3OH
360 selectivity. It is very interested that both CH_4 conversion and CH_3OH selectivity
361 synchronously reached the highest value at 10 wt.% loading, since generally CH_3OH
362 selectivity decreases with the increase of CH_4 conversion. To reveal the unique role of
363 the Ni-based catalysts, we characterized them by XRD, HAADF-STEM, H_2-TPR, XPS,
364 HRTEM, XRF and N_2 physisorption.

365 The XRD result (Figure 4 A) reveals no evident NiO peak for Ni loadings below 10
366 wt.%, indicating the high dispersion of the NiO particles on γ-Al_2O_3. However, a group
367 of NiO diffraction peaks gradually appears upon increasing metal loading, showing the
368 formation of larger NiO particles. The NiO crystal size is estimated by the
369 Debye−Scherrer equation, presented in Table S6. It is observed that NiO particles on
370 NiO/γ-Al_2O_3 with Ni loading from 15 to 25 % are in the range of 10.3−22.1 nm. In
371 addition, the adsorption-desorption isotherm and pore size distribution curve of the
372 catalysts are shown in Figure S14, and the corresponding surface values are presented
373 in Table S6. Clearly, surface area of NiOγ-Al_2O_3 catalysts gradually declined with the
374 increasing of Ni loading, and γ-Al_2O_3 support shows the highest surface area (216.5
375 m^2/g). By correlating the surface area (Table S6) with the reaction performance (Figure
376 1), it can be concluded that surface area is not the key factor in determining catalytic
377 performance of NiO/γ-Al_2O_3 catalysts in DOMTM.

378 Figure 4 C, D and E show HAADF-STEM images of 2 wt.% NiO/γ-Al_2O_3, 10
379 wt.% NiO/γ-Al_2O_3 and 25 wt.% NiO/γ-Al_2O_3 catalysts, respectively. Clearly, the NiO

particle size in 2 wt.% NiO/γ-Al_2O_3 and 10 wt.% NiO/γ-Al_2O_3 is very small (< 5 nm), but the size in 25 wt.% NiO/γ-Al_2O_3 is bigger (>10 nm). Figure S15 shows the HAADF-STEM mapping results of 6 wt.% NiO/γ-Al_2O_3, 15 wt.% NiO/γ-Al_2O_3 and 20 wt.% NiO/γ-Al_2O_3. It can be seen that NiO was uniformly dispersed in 6 wt.% NiO/γ-Al_2O_3. In 15 wt.% NiO/γ-Al_2O_3 and 20 wt.% NiO/γ-Al_2O_3, however, NiO particles with size more than 10 nm can be clearly observed. HRTEM images (Figure S16) show similar results. These morphology results indicate that NiO was highly dispersed on the surface of γ-Al_2O_3 with low loading (2, 6 and 10), and also demonstrate the larger NiO particles at higher Ni loadings. Furthermore, a lattice space of 0.21 nm and 0.24 nm, attributed to the (200) and (111) planes, was observed by HRTEM (Figure S17), and similar results were also obtained from fast Fourier transformation (FFT) of NiO particles in the HAADF-STEM images (Figure 4 C, D and E), consistent with the XRD results (Figure 4 A).



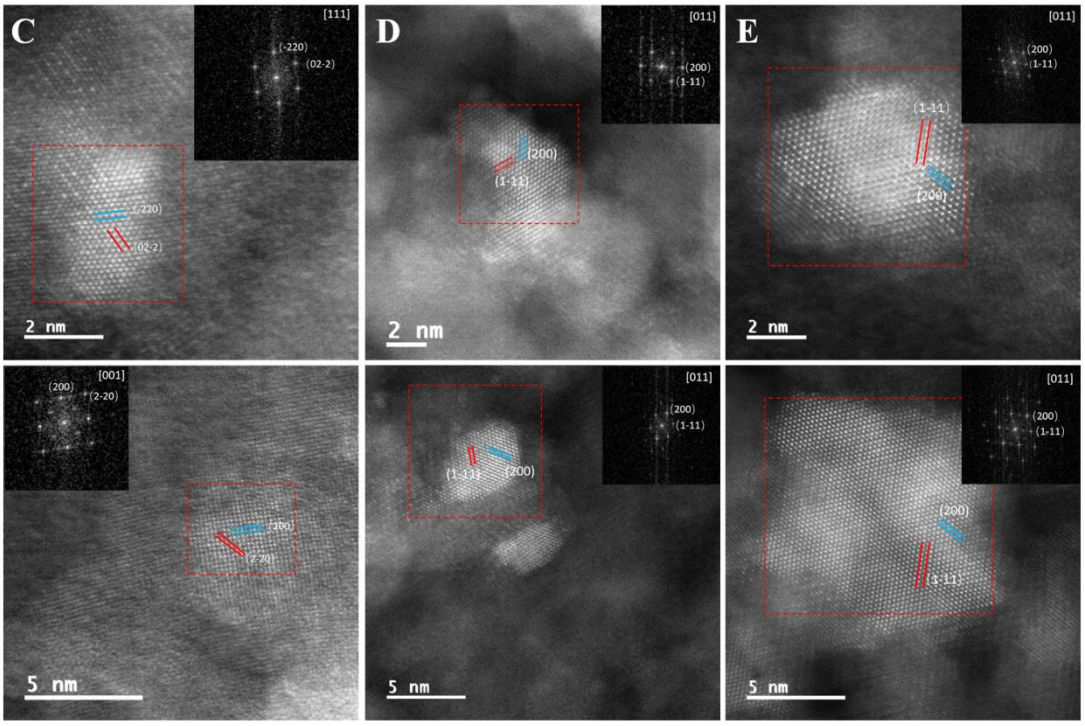


Figure 4. Characterization results of the NiO/γ-Al_2O_3 catalysts with varying loadings. (A) XRD patterns; (B) H_2-TPR profiles; (C) HAADF-STEM image of NiO/γ-Al_2O_3 catalyst with 2 wt.% loading; (D)HAADF-STEM image of NiO/γ-Al_2O_3 catalyst with 10 wt.% loading; (E) HAADF-STEM image of NiO/γ-Al_2O_3 catalyst with 25 wt.% loading.

The H_2-TPR profiles of the NiO/γ-Al_2O_3 catalysts are shown in Figure 4 B (NiO was used as a reference), and quantitative TPR results are presented in Figure S18 and Table S7. Five reducible peaks, at 280-350 ºC, 390-510 ºC, 510-690 ºC, 690-790 ºC and 790-840 ºC, were detected, attributed to the reduction of five kinds of NiO species, i.e., bulk NiO (without interaction with Al_2O_3), α-type NiO (weak oxide-support interaction, WOSI), β_1-type NiO (strong oxide-support interaction (SOSI), with Ni abundant on surface), β_2-type NiO (SOSI, with Al abundant on surface) and γ-type NiO (nickel aluminum spinel; strongest interaction with Al_2O_3), respectively. [40-42] Obviously, β_1, β_2 and γ-type NiO are present in all NiO/γ-Al_2O_3 catalysts. On the other hand, α-type

and bulk NiO only appear for Ni loadings above 10 wt.%. This corresponds to the XRD results, where obvious diffraction peaks of NiO (larger particles) were formed at high loading (15%, 20% and 25%). This is also consistent with the morphology results, where bigger NiO particles have been observed at high loading (15%, 20% and 25%).

The XPS profiles of the Ni 2p and O 1s of the NiO/γ-Al_2O_3 catalysts with various Ni loadings are shown in Figure 5 A and B, respectively (Al 2p results are shown in Figure S19). For Ni 2p, three peaks, corresponding to a binding energy at 854.0, 855.8 and 856.9 eV, have been detected. The low binding energy peak (854.0 eV) is assigned to free-NiO species (big NiO particles). [43, 44] The moderate binding energy peak (855.8 eV) is usually attributed to NiO species with WOSI. [45] The high binding energy peak (856.9 eV), however, generally results from NiO species with SOSI or Ni^{3+} species. [44, 46] On the other hand, the intensity of the satellite peak of Ni^{3+} is extremely low (it can nearly be ignored), which means that there is few Ni^{3+} species on the catalyst surface, and thus the peak of binding energy at 856.9 eV is mainly attributed to NiO species with SOSI.

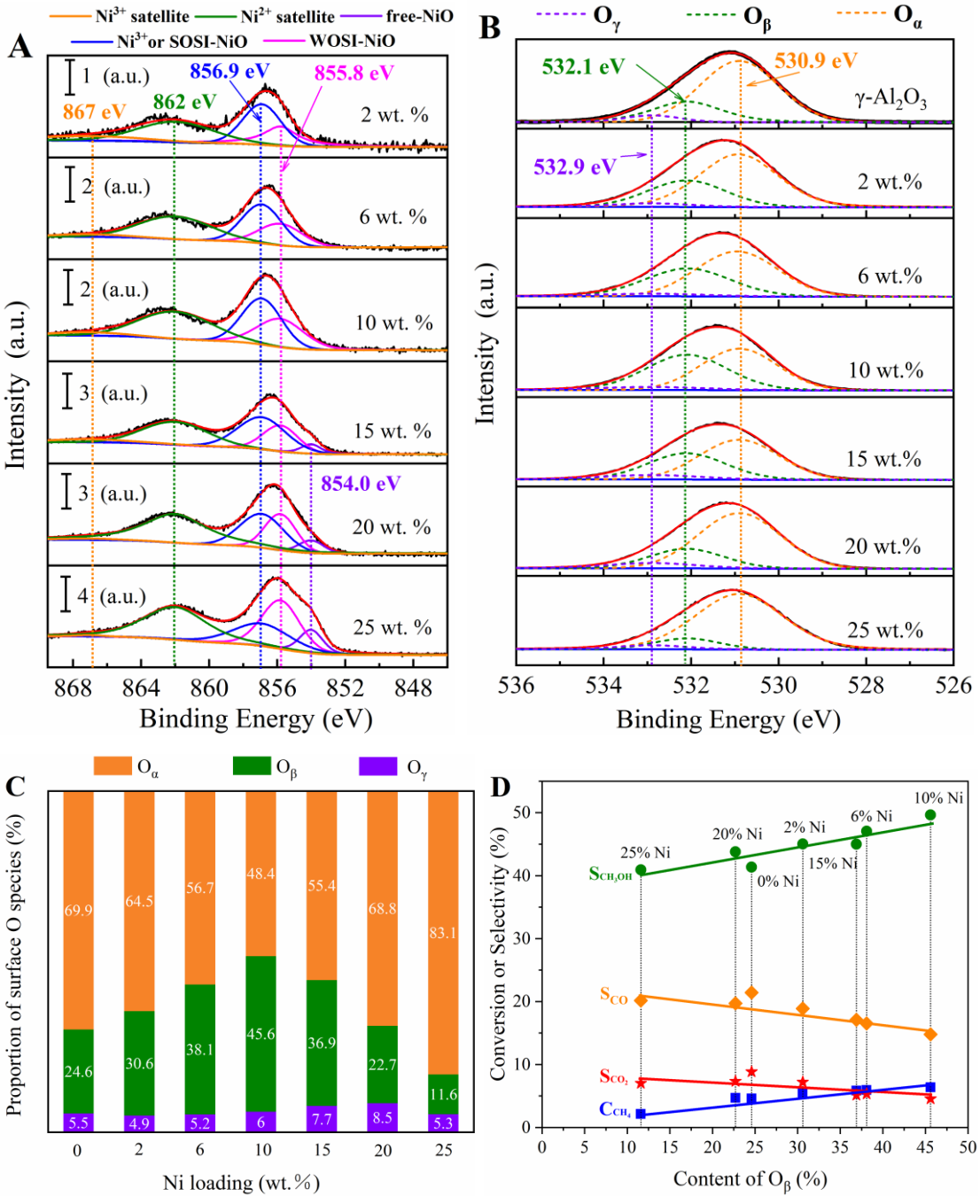


Figure 5. XPS results of the NiO/γ-Al_2O_3 catalysts with varying loadings. (A) Ni 2p region; (B) O 1s region; (C) Proportion of oxygen species for varied loading of Ni on γ-Al_2O_3; (D) Linear relationship between content of chemisorbed oxygen species (O_β) and reaction performance.

Furthermore, at low loading (2, 6 and 10 wt.%), Ni mainly exists as NiO species

433 with SOSI, since the peak of binding energy at 856.9 eV dominates the whole Ni 2p
434 peak. On the other hand, at higher loading (15, 20 and 25 wt.%), Ni mainly exists as
435 NiO species with WOSI and free-NiO, because the peak at 854.0 eV appears and the
436 contribution of the peak at 855.8 eV increases. The surface information obtained by
437 XPS analysis is consistent with the above XRD, TEM and H_2-TPR results.

438 The O 1s spectra of NiO/γ-Al_2O_3 catalysts presented in Figure 5 B can be fitted into
439 three peaks, corresponding to the lattice oxygen of metal oxide (O_α), chemisorbed
440 oxygen (O_β), and adsorbed water or OH species (O_λ), with binding energy at 530.9 eV,
441 532.1 eV and 532.9 eV, respectively. [47, 48]

442 As shown in Figure 5 C, upon increasing Ni loading from 2 to 10 wt.%, the
443 proportion of O_β species on the catalyst surface rises, and reaches the highest value
444 (45.6%) at 10 wt.% loading, and then it decreases. Interestingly, the variation trend of
445 Ni 2p peak of SOSI NiO (Figure 5 A) is synchronous with O 1s of O_β species, which
446 means that the chemisorbed oxygen, i.e., O_β species, mainly comes from the SOSI NiO.
447 Lattice oxygen, i.e., O_α species, are undoubtedly from crystals, i.e., γ-Al_2O_3 support,
448 free-NiO particles, and big NiO particles with WOSI. Upon increasing Ni loading, the
449 proportion of O_α species, however, firstly decreases and then increases, and the lowest
450 proportion was found at 10 wt.% loading, which means that the defects on the surface
451 of 10 wt.% NiO/γ-Al_2O_3 catalysts is much more than those of the other catalysts. The
452 defects have been created by SOSI, and usually, the created defects on metal oxide are
453 not stable. In an oxidizing atmosphere, they tend to combine with oxygen to form
454 chemisorbed oxygen, i.e., O_β species. That is, NiO with SOSI leads to surface

chemisorbed oxygen species.

Figure 5 D presents the reaction performance (CH_4 conversion, CH_3OH selectivity, CO and CO_2 selectivity) as a function of O_β content on the catalyst surface. Interestingly, with increasing O_β species content, both CH_4 conversion and CH_3OH selectivity rise linearly, while both CO and CO_2 selectivity decrease linearly. Therefore, it can be reasonably inferred that chemisorbed oxygen, i.e., O_β species, are the real active sites for CH_4 to CH_3OH conversion in this study. In contrast, lattice oxygen species, i.e., O_α, may be the sites leading to deep oxidation to produce CO and CO_2 (Figure S20).

TG-MS results (Figure S21) shows very limited carbon deposition. In addition, the fresh and spent NiO/γ-Al_2O_3 (10 wt.%) catalysts were compared by XRD (Figure S22), H_2-TPR (Figure S23) and XPS (Figure S24), and no evident changes were observed. These results demonstrate the excellent catalytic stability of NiO/γ-Al_2O_3 catalyst in CH_4/O_2 NTP for CH_3OH production. Some other information of the NiO/γ-Al_2O_3 catalysts, i.e., the real loading, surface area and porosity, is shown in Table S6.

3.4 NTP diagnostics and reaction mechanism

OES diagnostics were employed to reveal some of the important plasma species playing a role in CH_4/O_2 NTP for CH_3OH synthesis. As shown in Figure 6 and Figure S25, CH (431.4 nm), H (656.3nm) and O (777.4 nm and 844.7 nm) were directly identified, demonstrating the existence of CH, H and O species in the plasma. However, also other reactive species are present in the plasma, which cannot be observed by OES.

Morgan and Erwin stated that CH_4 can be decomposed into CH_3, CH_2 and CH neutral

fragments. [49, 50] Based on a 1D fluid model, De Bie et al. predicted a probability of producing CH_3, CH_2 and CH radicals in CH_4 DBD plasma of 79 %, 15 % and 5 %, respectively.[51] A similar trend was predicted in a CH_4/O_2 DBD plasma, again by a 1D fluid model. [52] Therefore, we can assume that CH_3 is more abundant than CH_2 and CH in the CH_4/O_2 NTP. The reason why CH_3 was not detected by OES is because its emission lines appear in the infrared region, which is out of the wavelength range of our OES measurements. For the oxidative species, the lines at 777.4 nm and 844.7 nm were detected by OES, attributed to deexcitation of O ($3p^5P$) and O ($3p^3P$) atoms, respectively.[53] However, the pathways for activation of O_2 through inelastic collisions with energetic electrons, as listed in Figure S26, indicate that the generation of O (^1D) is easier than the generation of O ($3p^5P$) and O ($3p^3P$). [54, 55] The reason why we did not detect O (^1D) by OES is that it is a metastable species with long lifetime, which dissipates its internal energy by chemical reactions, instead of deexcitation. Therefore, there will be abundant CH_3 radicals and O (^1D) atoms in the CH_4/O_2 NTP, which confirms the reaction pathway in Scheme 1, triggered by O (^1D) and CH_3. The above OES results show that, in CH_4/O_2 plasma, there are abundant CH_3, O (^1D) and H radical species.

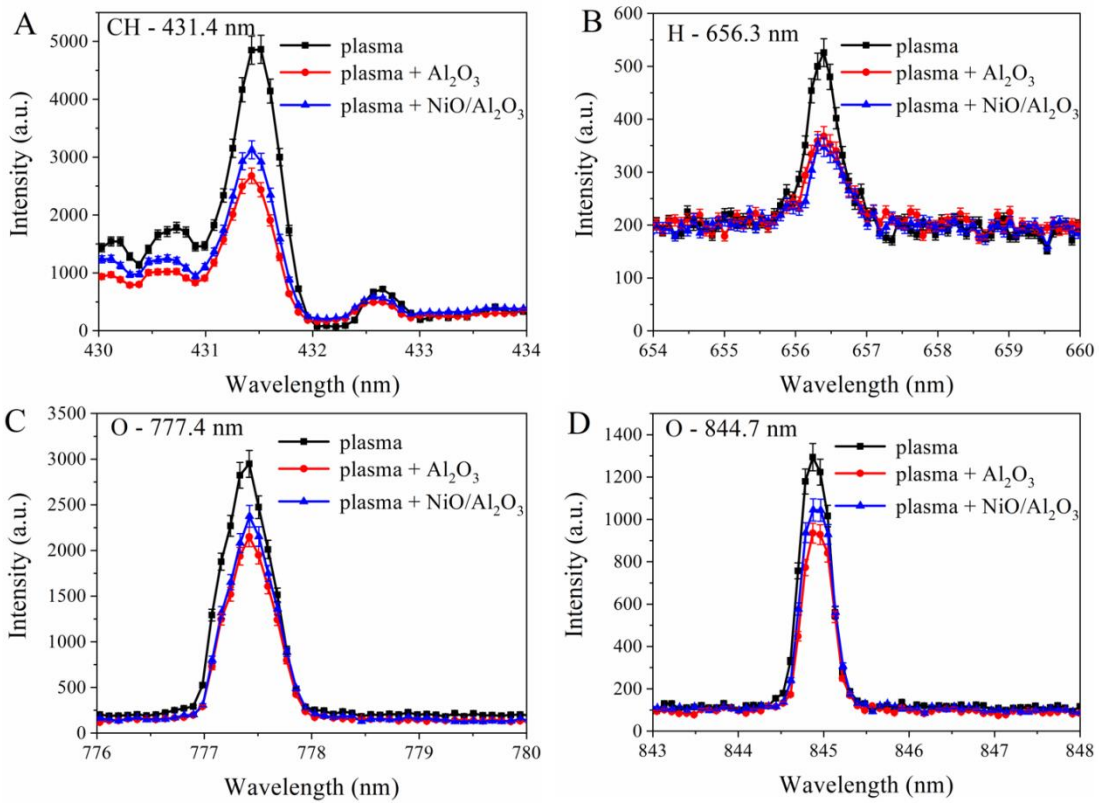


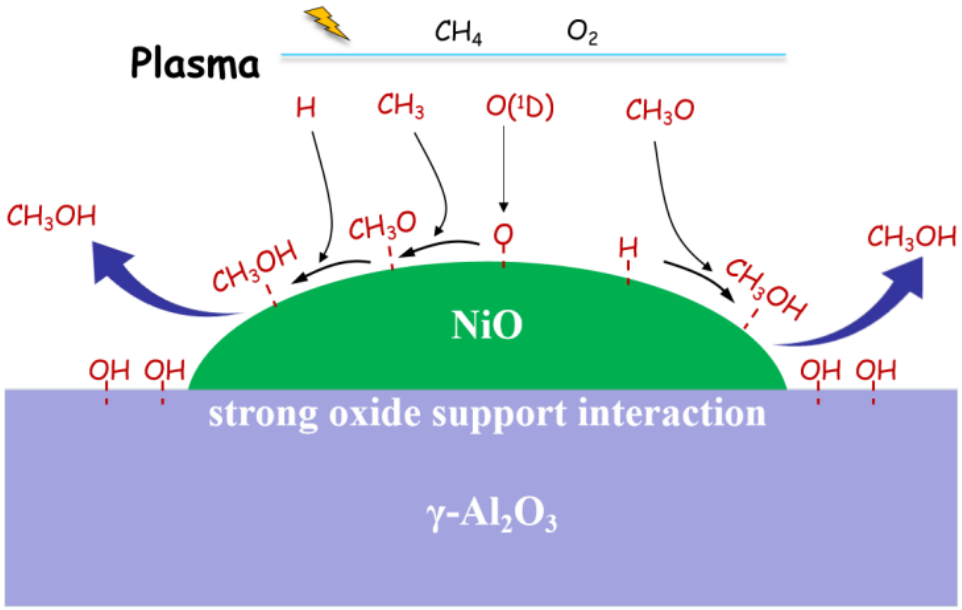
Figure 6. OES intensities of (A) CH (431.4 nm), (B) H (656.3 nm), (C) O (777.4 nm) and (D) O (844.7 nm), in the case of plasma alone, plasma + γ-Al_2O_3 beads, and plasma +(10 wt%) NiO/γ-Al_2O_3 catalyst, for the same conditions as in Figure 1.

Tang et al. predicted that CH_3OH synthesis usually proceeds through the Langmuir-Hinshelwood (L-H) mechanism in thermal catalysis.[56] In plasma catalysis, however, CH_3OH might be formed by both Eley-Rideal (E-R) and L-H mechanisms. [32, 57, 58] On the NiO/γ-Al_2O_3 (10 wt.%) catalyst surface, chemisorbed oxygen is abundant, which has been demonstrated by our XPS results. On the other hand, in the gas-phase, CH_3 and O radicals are also abundant, as proven by our OES results. Therefore, it can be reasonably assumed that CH_3O species can be formed, not only through radical reactions in gas-phase (proven by our modelling results in Scheme 1), i.e., $CH_3O_{(g)}$, but also through reaction between CH_3 in gas phase and chemisorbed

oxygen on the catalyst surface, i.e., $CH_3O_{(ad)}$. That is, due to the reactivity of the CH_3 radicals caused by their internal energy, the formation of CH_3O species through E-R reaction between CH_3 radicals and chemisorbed oxygen will be very fast. Subsequently, the formed CH_3O species may result in the generation of CH_3OH through recombination with a H atom generated by CH_4/O_2 plasma (E-R reaction) [32]. Therefore, the reason why the NiO/γ-Al_2O_3 (10 wt.%) catalyst shows the best CH_4 conversion may be that it contains the highest content of chemisorbed oxygen. In the case of plasma-catalytic CH_4 to CH_3OH conversion, the formation and desorption of one CH_3OH molecule will consume one O_β species (as O_β is the real active site). In conventional heterogeneous catalysis, this may lead to a continuous decrease of the O_β content at the catalyst surface, and thus the reaction performance would decline since the catalytic cycle cannot be completed. However, in the case of plasma catalysis, O_2 is activated by the plasma into O atoms (either in ground or excited states, e.g., ^1D), which are very reactive, and easily interact with the catalyst surface. So, we believe that these O atoms are capable of interacting with the catalyst surface to rapidly form O_β species, which compensates for the consumption of O_β species producing CH_3OH. In other words, the plasma-generated reactive oxygen species enable the fast catalytic cycle for CH_4 oxidation to CH_3OH.

The produced CH_3OH molecule usually strongly adsorbs on the catalyst surface, making desorption difficult and resulting in deep oxidation, which is the key factor inhibiting the CH_3OH selectivity, and it is the issue many researchers are concerning. As reported by Lustemberg, water molecules can be activated by Ni/CeO_2 catalyst with

strong metal-support interactions, and then the activated H_2O molecule can promote CH_3OH desorption.[37] In addition, Water molecular can act as a site blocker, which can preferentially occupy the active Ce sites at the CeO_2-Cu_2O catalyst interface and hinder methane overoxidation to CO and CO_2, meanwhile, it can also act as an active center where the active *OH was produced at interfacial Ce sites to promote methanol synthesis.[15] In the stepwise process using copper-exchanged zeolites, H_2O molecule also plays an essential role in promoting CH_3OH formation and desorption.[59, 60] Chemical kinetics modeling result (Figure S13) shows that H_2O molecules are abundant in the CH_4/O_2 NTP. The measured products selectivity based on hydrogen (Figure S9) shows that the selectivity of H_2O reached 29.1 %, demonstrating that H_2O molecules are abundant in CH_4/O_2 NTP. As demonstrated by our XPS results (Figure 5), caused by SOSI, the defects are also abundant at the interface between NiO particles and γ-Al_2O_3 support, especially for the NiO/γ-Al_2O_3 catalyst with 10 wt.% loading. Therefore, we believe that the H_2O molecule produced by CH_4/O_2 plasma can also be activated by NiO/γ-Al_2O_3 catalyst with SOSI, and the activated H_2O molecule may promote desorption of CH_3OH, which may be the reason why the NiO/γ-Al_2O_3 (10 wt.%) catalyst shows the best CH_3OH selectivity. The role of plasma and Ni-based catalyst in SOMTM has been summarized in Scheme 2.



Scheme 2. Suggested reaction pathways of CH_3OH formation in CH_4/O_2 plasma promoted by $NiO/\gamma\text{-}Al_2O_3$ catalyst with SOSI (see text)

4. Conclusion

We demonstrated the selective oxidation of methane to methanol (SOMTM) in CH_4/O_2 plasma, promoted by Ni-based catalysts, with excellent catalytic stability. 76 % liquid oxygenates selectivity with 42 % CH_3OH selectivity are achieved in plasma alone, and the selectivities are further enhanced to 81 % and 50 %, respectively, when adding $NiO/\gamma\text{-}Al_2O_3$ catalyst with 10 wt.% loading. The energy efficiency by plasma catalysis is improved with 84 % comparing to plasma alone (from 0.76 to 1.4 mol/kWh).

In addition, chemical kinetics modelling shows that within the plasma, CH_3OH is mainly produced through radical reactions, i.e., $CH_4 + O(^1D) \rightarrow CH_3O + H$, followed by $CH_3O + H + M \rightarrow CH_3OH + M$ and $CH_3O + HCO \rightarrow CH_3OH + CO$. The catalyst characterization shows that the further improvement in CH_3OH production by plasma

566 catalysis is attributed to the highly dispersed NiO phase with SOSI. This causes an
567 improvement of chemisorbed oxygen species, which catch CH_3 radicals from the
568 plasma to form CH_3O_{ad} species. The latter can form CH_3OH through the ER reaction
569 with H atoms from the plasma. Furthermore, H_2O molecules produced by CH_4/O_2
570 plasma may also be activated by NiO/γ-Al_2O_3 catalyst with SOSI, and the activated
571 H_2O molecules may promote desorption of CH_3OH. The highest content of
572 chemisorbed oxygen species can explain why the NiO/γ-Al_2O_3 catalyst with 10 wt.%
573 loading shows both the best CH_4 conversion and the best CH_3OH selectivity.

574 Further work will be focused on enhancing the plasma-catalyst synergy through
575 modifying the NiO/γ-Al_2O_3 catalyst by electronic promoters (multi-component
576 catalysts), which should allow to enhance the adsorption capacity towards reaction
577 intermediates (CH_3O, etc.) and the desorption of favorable target products, aiming to
578 further improve the CH_4 conversion and CH_3OH selectivity.

579 ## ASSOCIATED CONTENT

580 **Supporting Information**. The supporting information is available free of charge via
581 the Internet at XX.

582 Thermodynamic equilibrium of CH_4/O_2 conversion (Figure S1), preparation of
583 catalysts (Scheme S1), experimental details for activity test (Scheme S2), results of
584 qualitative analysis (Figure S2, Table S1), results of control experiments (Figure S3-
585 S9), plasma diagnostics (Figure S10-S11), energy efficiency (Figure S12), details of
586 chemical kinetic modeling (Table S2-S5, Figure S13), results of catalyst
587 characterization (Table S6-S7, Figure S14-S24), OES diagnostic of CH_4/O_2 plasma

(Figure S25-S26).

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Author Contributions

The manuscript was written through contributions of all authors. All authors have given approval to the final version of the manuscript.

Notes

The authors declare no competing financial interest.

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